# 2. Self-optimizing control Theory

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# Outline

Skogestad procedure for control structure design:

#### I. Top Down

- <u>Step S1</u>: Define operational objective (cost) and constraints
- <u>Step S2:</u> Identify degrees of freedom and optimize operation for disturbances
- <u>Step S3</u>: Implementation of optimal operation
  - Control active constraints
  - Control self-optimizing variables for unconstrained, c=Hy
- <u>Step S4:</u> Where set the production rate? (Inventory control)
- II. Bottom Up
  - <u>Step S5</u>: Regulatory control: What more to control (secondary CV's)?
  - <u>Step S6</u>: Supervisory control
  - <u>Step S7:</u> Real-time optimization

### **Step S3: Implementation of optimal operation**

• Optimal operation for given d\*:

$$\min_{u} J(u, x, d)$$
subject to:  
Model equations:  $f(u, x, d) = 0$   
Operational constraints:  $g(u, x, d) < 0$ 
 $\rightarrow u_{opt}(d)$ 

*Problem:* Usally cannot keep  $u_{opt}$  constant because disturbances d change

How should we adjust the degrees of freedom (u)? What should we control?

# "Optimizing Control"



## "Self-Optimizing Control"



c = Hy

*H*: Nonsquare matrix

- Usually selection matrix of 0's and some 1's (measurement selection)
- Can also be full matrix (measurement combinations)

## **Self-optimizing control**

Self-optimizing control is when we can achieve an acceptable loss with constant setpoint values for the controlled variables



(b) Flat optimum: Implementation easy

(c) Sharp optimum: Sensitive to implementation erros

### **Recap: marathon runner**



- CV = heart rate is good "self-optimizing" variable
- Simple and robust implementation
- Disturbances are indirectly handled by keeping a constant heart rate
- <u>May</u> have infrequent adjustment of setpoint  $(c_s)$

## **Optimal operation**



### Unconstrained degrees of freedom The ideal "self-optimizing" variable is the gradient, $J_u$ $c = \Delta J/\Delta u = Ju$

- Keep gradient at zero for all disturbances ( $c = J_u = 0$ )
- Problem: Usually no measurement of gradient



\*I.J. Halvorsen, S. Skogestad, Indirect on-line optimization through setpoint control, in: AIChE 1997 Annual Meeting, Los Angeles; paper 194h.

\*I.J. Halvorsen, S. Skogestad, J.C. Morud, V. Alstad, Optimal selection of controlled variables, Industrial & Engineering Chemistry Research 42 (14) (2003) 3273–3284



# Unconstrained optimum: NEVER try to control a variable that reaches max or min at the optimum

- In particular, never try to control directly the cost J
- Assume we want to minimize J (e.g., J = V = energy) and we make the stupid choice os selecting CV = V = J
  - Then setting J < J<sub>min</sub>: Gives infeasible operation (cannot meet constraints)
  - and setting J > J<sub>min</sub>: Forces us to be nonoptimal (two steady states: may require strange operation)

#### **Measurements or mesurement combinations**



• Single measurements:

$$\mathbf{c} = \mathbf{H}\mathbf{y} \qquad \mathbf{H} = \begin{bmatrix} 1 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 \end{bmatrix}$$

• Combinations of measurements:

$$\mathbf{c} = \mathbf{H}\mathbf{y} \qquad \mathbf{H} = \begin{bmatrix} h_{11} & h_{12} & h_{13} & h_{14} \\ h_{21} & h_{22} & h_{23} & h_{24} \end{bmatrix}$$

### **Optimal measurement combination**

$$\Delta c = h_1 \Delta y_1 + h_2 \Delta y_2 + \dots = H \Delta y$$

• Candidate measurements (y): Include also inputs u



### **Nullspace method**

#### Theorem

Given a sufficient number of measurements ( $n_y \ge n_u + n_d$ ) and no measurement noise, select **H** such that

 $\mathbf{HF} = \mathbf{0}$ 

where

$$\mathbf{F} = rac{\partial \mathbf{y}^{opt}}{\partial \mathbf{d}}$$

- Controlling  $\mathbf{c} = \mathbf{H}\mathbf{y}$  to zero yields locally zero loss from optimal operation.

Proof: Given  $\partial y^{opt} = F \partial d$ , and c = Hy:  $\partial c^{opt} = H \partial y^{opt} = HF \partial d$ 

To make  $\partial c^{opt} = 0$  for any  $\partial d$ , we must have HF = 0.

V. Alstad, S. Skogestad, Null space method for selecting optimal measurement combinations as controlled variables, Industrial & Engineering Chemistry Research 46 (2007) 846–853.

Jäschke, J., Cao, Y., & Kariwala, V. (2017). Self-optimizing control-A survey. Annual Reviews in Control, 43, 199–223.

### Nullspace method gives J<sub>u</sub>=0

Proof:

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$$J_{u} = J_{uu} \Delta u + J_{ud} \Delta d = [J_{uu} J_{ud}] \begin{bmatrix} \Delta u \\ \Delta d \end{bmatrix}$$
$$\Delta y = \begin{bmatrix} G^{y} & G_{d}^{y} \end{bmatrix} \begin{bmatrix} \Delta u \\ \Delta d \end{bmatrix} = \tilde{G}_{y} \begin{bmatrix} \Delta u \\ \Delta d \end{bmatrix} \rightarrow \begin{bmatrix} \Delta u \\ \Delta d \end{bmatrix} = \tilde{G}_{y}^{+} \Delta y$$

Formula for *F*:

$$J_{u}^{opt} = J_{uu} \Delta u^{opt} + J_{ud} \Delta d = 0 \rightarrow \Delta u^{opt} = -J_{uu}^{-1} J_{ud} \Delta d$$
$$\Delta y^{opt} = \tilde{G}_{y} \begin{bmatrix} \Delta u^{opt} \\ \Delta d \end{bmatrix} = \tilde{G}_{y} \begin{bmatrix} -J_{uu}^{-1} J_{ud} \\ I \end{bmatrix} \Delta d$$
$$\rightarrow F = \tilde{G}_{y} \begin{bmatrix} -J_{uu}^{-1} J_{ud} \\ I \end{bmatrix}$$

Let  $H = [J_{uu} J_{ud}]\tilde{G}_y^+$ . We can verify that HF = 0. Therefore,  $J_u = [J_{uu} J_{ud}]\tilde{G}_y^+ \Delta y = H\Delta y = \Delta c$ , and thus controlling c ( $\Delta c = 0$ ) leads to  $J_u = 0$ .

Proof. Appendix B in: Jäschke and Skogestad, "NCO tracking and self-optimizing control in the context of real-time optimization", *Journal of Process Control*, 1407-1416 (2011)

### Nullspace method (HF=0) gives J<sub>u</sub>=0

Proof (constant d):

$$J_u(u,d) = \underbrace{J_u(u_{opt}(d),d)}_{=0} + J_{uu} \cdot (u - u_{opt})$$

 $u - u_{opt} = (HG^y)^{-1}(c - c_{opt})$ Here:  $c - c_{opt} = \Delta c - \Delta c_{opt}$ where we have introduced deviation variables around a nominal optimal point  $(c^*, d^*)$  (where  $c^* = c_{opt}(d^*)$ ) Assume perfect control of c (no noise):  $\Delta c = 0$ Optimal change:  $\Delta c_{opt} = H\Delta y_{opt} = HF\Delta d$ Gives:  $J_u = -J_{uu}(HG^y)^{-1}HF\Delta d$  $\Rightarrow HF = 0$  gives  $J_u = 0$  for any disturbance  $\Delta d$ 

Proof. Appendix B in: Jäschke and Skogestad, "NCO tracking and self-optimizing control in the context of real-time optimization", *Journal of Process Control*, 1407-1416 (2011)

# Example. Nullspace Method for Marathon runner

u = power, d = slope [degrees] y<sub>1</sub> = hr [beat/min], y<sub>2</sub> = v [m/s]

$$F = dy_{opt}/dd = \begin{bmatrix} 0.25 \\ -0.2 \end{bmatrix}$$
  

$$H = [h_1 \ h_2]$$
  

$$HF = 0 \rightarrow h_1 f_1 + h_2 f_2 = 0.25 h_1 - 0.2 h_2 = 0$$
  
Choose  $h_1 = 1 \rightarrow h_2 = 0.25/0.2 = 1.25$ 

Conclusion: **c** = **hr** + **1.25 v** 

Control **c** = **constant**  $\rightarrow$  hr increases when v decreases (OK uphill!)

### Marathon runner: Exact local method

$$F = \begin{bmatrix} 0.25 \\ -0.2 \end{bmatrix}, W_d = 1, W_{ny} = \begin{bmatrix} 1 & 0 \\ 0 & 1 \end{bmatrix}, G^y = \begin{bmatrix} 1 \\ 1 \end{bmatrix}$$
$$Y = \begin{bmatrix} FW_d & W_{ny} \end{bmatrix} = \begin{bmatrix} 0.25 & 1 & 0 \\ -0.2 & 0 & 1 \end{bmatrix}$$
$$H = G^{y^T} (Y Y^T)^{-1} \to H = \begin{bmatrix} 0.989 & 1.009 \end{bmatrix}$$

Normalized H1 =  $D^{*}H = [1 \ 1.02]$ Conclusion: **c** = **hr** + **1.02 v** 

- Before (nullspace method): c = hr + 1.25 v
- Note: Gives same as nullspace when  $W_{ny}$  is small

# Extension: "Exact local method" (with measurement noise)

$$\min_{H} \|J_{uu}^{1/2}(HG^{y})^{-1}H\underbrace{[FW_{d} \ W_{n^{y}}]}_{Y}\|_{F}$$

• General analytical solution ("full" H):

$$H = G^{yT}(YY^T)^{-1}$$

- No disturbances (W<sub>d</sub>= []) + same noise for all measurements (W<sub>ny</sub>= Y = I): Optimal is H=G<sup>yT</sup> ("control sensitive measurements")
  - Proof: Use analytic expression
- No noise  $(W_{nv}=0)$ : Cannot use analytic expression, but optimal is clearly
  - HF = 0 (Nullspace method)
  - Assumes enough measurements:  $\#y \ge \#u + \#d$
  - If "extra" measurements (>) then solution is not unique

V. Alstad, S. Skogestad, E.S. Hori, Optimal measurement combinations as controlled variables, Journal of Process Control 19 (1) (2009) 138–148. Jäschke, J., Cao, Y., & Kariwala, V. (2017). Self-optimizing control–A survey. Annual Reviews in Control, 43, 199–223.

Optimal self-optimizing measurement combination, H 818-23 Expected O in deviation variables d= Weld n'=wh(n") Expected magnitude" 6=0 H Ym cn=0 at steady with integral action in K Question: What to could , C= Hy. What is bead H? Steady-state: Economic loss I for given d is caused by m # Martid) L=J(u,d)-J(uoptid), d) = J (u-uopt) - 2 (u-uopt) Jun (u-upt) + L=J(u,d)-J(uoptid), d) = J (u-uopt) - 2 (u-uopt) Jun (u-upt) + higher-order higher-order higher-order higher-order higher-order Taylor expansion of loss around artimum. Here: C-lupt = H(y-Joph) = H(y'-Loph) of Jozj => (u-uor) = (464) ~ (C-lon) L= ± z z where z= Jun (under) = Jun (+ (+ (+)) - (- (q+)) 50 get L dependre on d and n' (rits =0 other wise) 1. Disturbance change wort (and you and (and ): 1. Disturbance change wort (and you and (and ): Optimul sensitivity F= Id Algert = Fd = (git = HFd = (HFWLd depictulier vier adden vier adden vier adden optimul sensitivity F= HWLL Note: HF=0 -> copt=0 (Nullspace method)  $C_{n} = 0$   $\Rightarrow$   $C_{n} = HY_{n} = H(Y + h) = 0 \Rightarrow$   $C = HY = -Hh^{Y} = +Hh^{Y} \cdot h^{Y}$   $C_{n} + c_{prod}$  attem  $(c_{h} + c_{prod}) = 0 \Rightarrow$   $C = HY = -Hh^{Y} = +Hh^{Y} \cdot h^{Y}$ 2, Noike makes (±0: change from to + because sign of nul does not 50 get Z= - Lon (16) H [FWd Wa?] Luc =  $\frac{1}{2} \overline{\sigma} (M)^2 | \overline{\sigma} = singular value$ Average loss tor Woistwee Was for is 12-norm of vector Both caree = Analytical formula for optimal H is HT=(YY)G7 special case with no noise, Wn = O get L=0 with [HF=0] mullippice molenut

# **Obtaining F**

*F* is defined as the gain matrix from the disturbances to the optimal measurements  $\rightarrow \Delta y^{opt} = F \Delta d$ 

Brute force method:

- For every disturbance  $d_i$ ,  $i = 1, ..., n_d$ :
  - Perturb the system with  $\hat{d}_i = d_i + \Delta d_i$ ,  $\Delta d_i$  small
  - Reoptimize the system  $\rightarrow$  obtain change in measurements  $\Delta y^{opt,i}$
  - Obtain *i*-th column of  $F: F_i = \Delta y^{opt,i} / \Delta d_i$
- Return F

## Linearization method for F

*F* can also be obtained through a linearized state-space model:

$$\Delta y = G^{\mathcal{Y}} \Delta u + G_d^{\mathcal{Y}} \Delta d$$

$$J_{u}(u^{*} + \Delta u, d^{*} + \Delta d) \approx J_{u}^{*} + J_{uu}\Delta u + J_{ud}\Delta d = 0$$
  
$$\Rightarrow \Delta u^{opt} = J_{uu}^{-1}J_{ud}\Delta d$$

$$\Delta y^{opt} = G^{\mathcal{Y}} \Delta u^{opt} + G^{\mathcal{Y}}_{d} \Delta d = \left(-G^{\mathcal{Y}} J^{-1}_{uu} J_{ud} + G^{\mathcal{Y}}_{d}\right) \Delta d$$

$$F = -G^{\mathcal{Y}} J_{uu}^{-1} J_{ud} + G_d^{\mathcal{Y}}$$

### Toy Example.

 $J = (u - d)^{2}$   $n_{u} = 1 \text{ unconstrained degrees of freedom}$  $u_{opt} = d$ 

Alternative measurements:

$$y_1 = 0.1(u - d)$$
  

$$y_2 = 20u$$
  

$$y_3 = 10u - 5d$$
  

$$y_4 = u$$
  
Scaled such that:  

$$|d| \le 1, |n_i| \le 1|, \text{ i.e. all } y_i\text{'s are}$$
  
Nominal operating point:

$$d = 0 \Rightarrow u_{opt} = 0, y_{opt} = 0$$
  
What variable *c* should we control?

Single measurements

$$L_{wc} = \frac{1}{2} \ \overline{\sigma} \ (M)^2$$
$$M = J_{uu}^{\frac{1}{2}} (HG^y)^{-1} H Y,$$
$$Y = [FW_d \ W_{ny}], F = -G^y J_{uu}^{-1} J_{ud} + G_d^y$$

. Exact evaluation of loss:  $L_{wc,1} = 100$   $L_{wc,2} = 1.0025$   $L_{wc,3} = 0.26$  $L_{wc,4} = 2$ 

Here:  $W_d = 1$ ,  $W_{ny} = 1$ ,  $J_{uu} = 2$ ,  $J_{ud} = -2$ , For  $y_1: HG^y = 0.1$ ,  $HG_d^y = -0.1$ , F = 0,  $HY = [0 \ 1]$ ,  $M = \sqrt{2} \cdot 10 \cdot [0 \ 1]$ ,  $L_{wc} = \frac{1}{2} \ \overline{\sigma} (M)^2 = 100$ For  $y_2: HG^y = 20$ ,  $HG_d^y = 0$ , F = 20,  $HY = [20 \ 1]$ ,  $M = \sqrt{2} \cdot \frac{1}{20} \cdot [20 \ 1]$ ,  $L_{wc} = \frac{1}{2} \ \overline{\sigma} (M)^2 = 1.0025$ For  $y_3: HG^y = 10$ ,  $HG_d^y = -5$ , F = -15,  $HY = [5 \ 1]$ ,  $M = \sqrt{2} \cdot \frac{1}{10} \cdot [5 \ 1]$ ,  $L_{wc} = \frac{1}{2} \ \overline{\sigma} (M)^2 = 0.26$ 

Reference: I. J. Halvorsen, S. Skogestad, J. Morud and V. Alstad, "Optimal selection of controlled variables", Industrial & Engineering Chemistry Research, 42 (14), 3273-3284 (2003).

 $\pm 1$ 

## Toy Example. Exact local method. Combine all measurements

 $J = (u - d)^{2}$   $n_{u} = 1 \text{ unconstrained degrees of freedom}$  $u_{opt} = d$ 

Alternative measurements:

 $\begin{array}{l} y_1 = 0.1(u-d) \\ y_2 = 20u \\ y_3 = 10u - 5d \\ y_4 = u \end{array}$ Scaled such that:  $|d| \leq 1, \ |n_i| \leq 1|, \ \text{i.e. all } y_i\text{'s are } \pm 1$ Nominal operating point:  $d = 0 \Rightarrow u_{\text{opt}} = 0, y_{\text{opt}} = 0$ 

What variable c should we control?

 $Y = [FW_d W_{ny}],$   $F = -G^y J_{uu}^{-1} J_{ud} + G_d^y$  $H = (Y Y^T)^{-1} G^y$ 

 $H = (Y Y^T)^{-1} G^y = [0.1000 - 1.1241 4.7190 - 0.0562]$ 

Normalized to have 2-norm = 1.

H = [0.0206 -0.2317 0.9725 -0.0116]

Reference: V. Alstad et al., Journal of Process Control 19 (2009) 138-148

# Toy Example: Nullspace method (not unique)

$$c = Hy = (h_1 \ h_2 \ h_3 \ h_4) \begin{pmatrix} y_1 \\ y_2 \\ y_3 \\ y_4 \end{pmatrix} = h_1y_1 + h_2y_2 + h_3y_3 + h_4y_4$$

#### **B1.** Nullspace method

Neglect measurement error (n = 0):

HF = 0

Sensitivity matrix

 $\Delta y_{\text{opt}} = F \Delta d$ ;  $F = (0 \ 20 \ 5 \ 1)^T$ To find H that satisfies HF = 0 must combine at least two measurements:

 $n_y \ge n_u + n_d = 1 + 1 = 2$ 

# Toy Example. Nullspace method with 2 measurements

#### C. Optimal combination

Need two measurements. Best combination is  $y_2$  and  $y_3$ :

$$\begin{pmatrix} y_2 \\ y_3 \end{pmatrix} = \begin{pmatrix} 20 & 0 \\ 10 & -5 \end{pmatrix} \begin{pmatrix} u \\ d \end{pmatrix}; \ \underline{\sigma} = 4.45$$

Optimal sensitivity:

$$y_{\text{opt}} = Fd; F = \begin{pmatrix} 20\\5 \end{pmatrix}$$

Optimal combination:

$$HF = 0 \Rightarrow (h_1 \quad h_2) \begin{pmatrix} 20\\5 \end{pmatrix} = 0 \Rightarrow 20h_1 + 5h_2 = 0$$

Select  $h_1 = 1$ . Get  $h_2 = -20h_1/5 = -4$ , so

$$c_{\rm opt} = y_2 - 4y_3$$

Check: 
$$c = y_2 - 4y_3 = 20u - 40u + 20d = -20(u - d)$$
  
(OK!)

### Example where nullspace method «fails»

u= reflux d=feed rate  $J = (u-d)^2$ y1 = 0.01(u-d) % temperature product (very small gain!) y2 = u-0.8d % tempereture inside column uopt = d y1opt = 0 y2opt = 0.2 d

Nullspace: H0=[1 0] % Not good! Use only y1 Exact local method: H=[1 96] % Use y2 instead  $\begin{array}{l} F = [0 \ 0.2]' \\ Wd = 1^* eye(1) \\ Wn = 1^* eye(2) \\ Gy = [0.01 \ 1]' \\ H0 = null(F'); \ H0 = H0'/H0(1) \ \% \ nullspace \ method \\ Y = [F^*Wd \ Wn], \\ H1 = Gy' * inv(Y * Y') \\ H = H1/H1(1) \ \% \ exact \ local \ method \\ \end{array}$ 

### Conclusion: GOOD "SELF-OPTIMIZING" CV = c

1. Optimal value  $c_{opt}$  is constant (independent of disturbance d):

→ Want small optimal sensitivity:  $F_c = \frac{\Delta c_{opt}}{\Delta d} = HF$ 

- 2. c is "sensitive" to input u (MV) (to reduce effect of measurement noise)
  - → Want large gain  $G = HG^y = \frac{\Delta c}{\Delta u}$ (Equivalently: Optimum should be flat!)



### New 2024: Optimal steady-state operation using gradient estimate

 $min_u J(u,d)$ s.t. g(u,d)  $\geq$  0 (constraints)

• J = economic cost [\$/s]

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• Unconstrained case: Optimal to keep gradient  $J_u = \partial J/\partial u = 0$ 



Want tight control of active constraints for economic reasons

- Active constraint:  $g_A=0$
- Tight control of g<sub>A</sub> minimizes «back-off»
- How can we identify and control active constraints?
- How can we switch constraints?
- How do find the correct gradient when the constraints change?

# **I. Primal-dual control based on KKT conditions:** Feedback solution that automatically tracks active constraints by adjusting Lagrange multipliers (= shadow prices = dual variables) $\lambda$



D. Krishnamoorthy, A distributed feedback-based online process optimization framework for optimal resource sharing, J. Process Control 97 (2021) 72–83,

• R. Dirza and S. Skogestad . Primal–dual feedback-optimizing control with override for real-time optimization. J. Process Control, Vol. 138 (2024), 103208

Primal–dual feedback-optimizing control with override for real-time optimization  $^{\circ}$  Risvan Dirza, Sigurd Skogestad  $^{\circ}$ 

### I. Region-based feedback solution with «direct» constraint control (for case with more inputs than constraints)



**KKT**:  $L_u = J_u + \lambda^T q_u = 0$ Introduce N:  $N^T g_{\mu} = 0$ Control 1. Reduced gradient  $N^T J_{\mu} = 0$  «self-optimizing variables» 2. Active constrints  $g_A = 0$ .

	Journal of Process Control 137 (2024) 103194	
	Contents lists available at ScienceDirect	*
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ELSEVIER	journal homepage: www.elsevier.com/locate/jprocont	

- Jaschke and Skogestad, «Optimal controlled variables for" polynomial systems». S., J. Process Control, 2012
- D. Krishnamoorthy and S. Skogestad, «Online Process Optimization with Active Constraint Set Changes using Simple Control Structure», I&EC Res., 2019
- Bernardino and Skogestad, Decentralized control using selectors for optimal steady-state operation with changing active constraints, J. Process Control, Vol. 137, 2024

Decentralized control using selectors for optimal steady-state operation w changing active constraints

### Static gradient estimation: Very simple and works well!



From «exact local method» of self-optimizing control:



	Computers and Chemical Engineering 189 (2024) 108815	
	Contents lists available at ScienceDirect	Computers
	Computers and Chemical Engineering	Engineering
ELSEVIER	journal homepage: www.elsevier.com/locate/cace	

Optimal measurement-based cost gradient estimate for feedback real-time

Bernardino and Skogestad, Optimal measurement-based cost gradient estimate for real-time optimization, Comp. Chem. Engng., 2024
 Compare Structure S



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#### III. Region-based MPC with switching of cost function (for general case)

Standard MPC with fixed CVs: Not optimal



Figure 1: Typical hierarchical control structure with standard setpoint-tracking MPC in the supervisory layer. The cost function for the RTO layer is  $J^{ec}$  and the cost function for the MPC layer is  $J^{MPC}$ . With no RTO layer (and thus constant setpoints  $CV^{sp}$ ), this structure is not economically optimal when there are changes in the active constraints. For smaller applications, the state estimator may be used also as the RTO estimator.

$$J^{MPC} = \sum_{k=1}^{N} \|CV_k - CV^{sp}\|_Q^2 + \|\Delta u_k\|_R^2$$



Figure 2: Proposed region-based MPC structure with active set detection and change in controlled variables. The possible updates from an upper RTO layer  $(y^*, J_u^* \text{ etc.})$  are not considered in the present work. Even with no RTO layer (and thus with constant setpoints  $CV_{\mathcal{A}}^{sp}$ , see [14] and [15], in each active constraint region), this structure is potentially economically optimal when there are changes in the active constraints.

$$I_{\mathcal{A}}^{MPC} = \sum_{k=1}^{N} \|CV_{\mathcal{A}} - CV_{\mathcal{A}}^{sp}\|_{\mathcal{Q}_{\mathcal{A}}}^{2} + \|\Delta u_{k}\|_{\mathcal{R}_{\mathcal{A}}}^{2} \qquad CV_{\mathcal{A}} = \begin{bmatrix} g_{\mathcal{A}} \\ c_{\mathcal{A}} \end{bmatrix} = \begin{bmatrix} g_{\mathcal{A}} \\ N_{\mathcal{A}}^{T}H_{0}y \end{bmatrix} \qquad (14)$$

$$H_{0} = \begin{bmatrix} J_{uu} & J_{ud} \end{bmatrix} \begin{bmatrix} G^{y} & G_{y}^{y} \end{bmatrix}^{\dagger}$$

$$H_{0} = \begin{bmatrix} J_{uu} & J_{ud} \end{bmatrix} \begin{bmatrix} G^{y} & G_{y}^{y} \end{bmatrix}^{\dagger}$$

$$(14)$$

Bernardino and Skogestad, Optimal switching of MPC cost function for changing active constraints. J. Proc. Control, 2024

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