



# NTNU

Innovation and Creativity

## **CONTROL OF FUEL CELLS**

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# OUTLINE

INTRODUCTION

ELECTROCHEMISTRY

BUCK-BOOST CONVERTERS

MANIFOLD COMPOSITION AND PRESSURE CONTROL

STACK TEMPERATURE CONTROL

# INTRODUCTION

## Fuel cells

- Devices to convert chemicals (hydrogen, oxygen) into electricity
- No polluting emissions, scalable, efficient, no moving parts. . .
- This thesis focuses on proton-exchange-membrane fuel cells

## Motivation for control of fuel cells

- Any fuel cell outside a lab needs control!
- Commercial applications require automation
- Even in the lab it would be useful: many phenomena
- Most research on the topic focuses on only one aspect at a time

## CHOICE OF CONTROL VARIABLES

- Classical stumbling block: few fuel cell researchers are trained in control theory, let alone experts
- *What* do we want to control? *With what* are we going to do it?

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  - Choosing bad combinations: manipulate inflow to control power output (not strictly impossible)
  - Considering only part of the system (this is difficult to escape)

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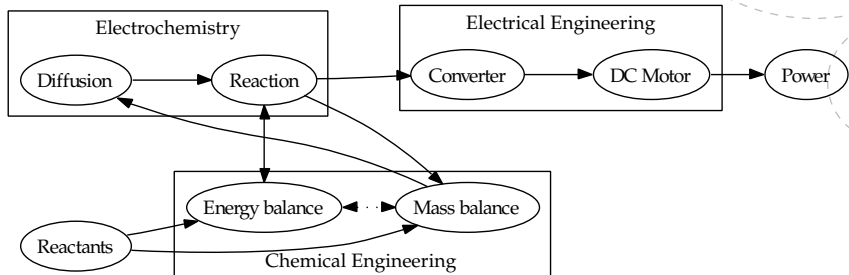
- Classical stumbling block: few fuel cell researchers are trained in control theory, let alone experts
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- Common errors:
  - Assuming current or voltage can be manipulated directly
  - Choosing bad combinations: manipulate inflow to control power output (not strictly impossible)
  - Considering only part of the system (this is difficult to escape)
- We first have to consider what the fuel cell is going to be used for, and how it will be connected
- Control insight may actually suggest design modifications to improve the system's controllability

# ADVANTAGES OF POLYBENZIMIDAZOLE MEMBRANES

- PBI works at higher temperatures (125–200 °C) than ordinary Nafion (80–90 °C):
  - We simply don't have any water management
  - Streams contain more heat: no dedicated cooling loop?
  - Increased tolerance to CO
- PBI cells look better for control, but there are some issues:
  - Not as off-the-shelf as Nafion, less reproducibility
  - Less experimental data (influence of CO?)

# FUEL-CELL DYNAMICS

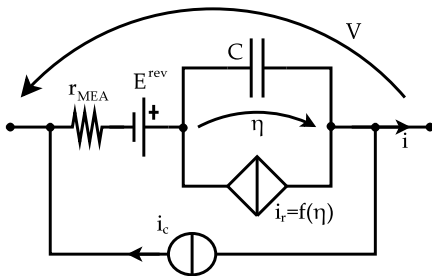
- Many assume that there is only one dynamics of fuel cells: in fact, there are many dynamic modes



- Users are really interested only in the *last part*, the rest is “under the hood”



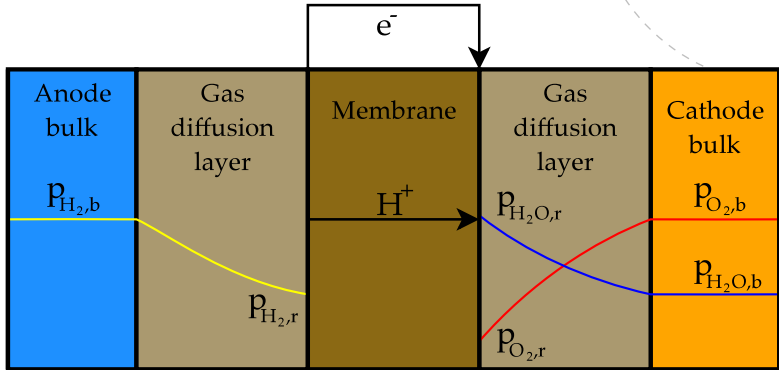
# THE ELECTROCHEMICAL MODEL



- A common model for a fuel cell, with cathode only
- It consists of generator  $E^{rev}$ , internal resistance  $R_{MEA}$ , charge double layer  $C$ , Butler-Volmer law  $f(\eta)$ , crossover current density generator  $i_c$

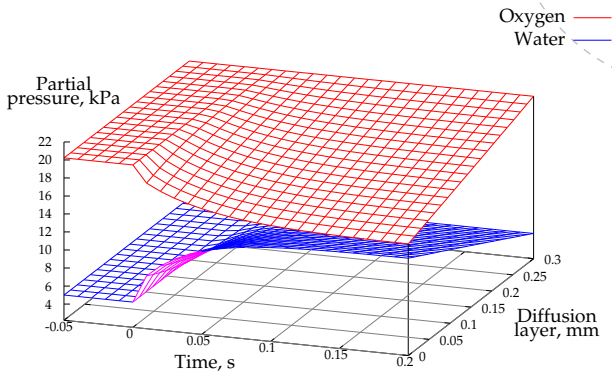
# MULTICOMPONENT DIFFUSION

Can we simplify the Stefan-Maxwell and continuity equations?



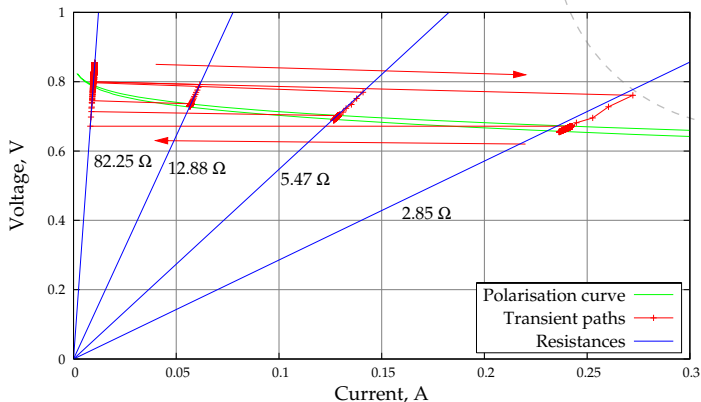
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- Transients are fast enough to be neglected, especially since these transients lag behind other ones

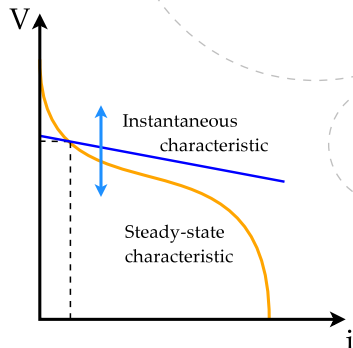
# STEPPING THE RESISTANCE LOAD



- Markers spaced by  $\approx 0.06$  s
- Notice the similar pattern for all transients!

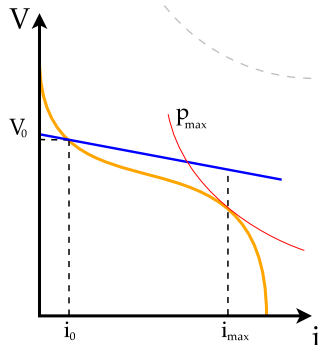
# THE INSTANTANEOUS CHARACTERISTIC

- The points in the  $i$ - $V$  plane a cell can immediately reach
- Moves up and down with values of  $\eta(i_r)$ ; inclination depends on  $r$
- The actual voltage and current depend on the load's characteristic as well



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- Moves up and down with values of  $\eta(i_r)$ ; inclination depends on  $r$
- The actual voltage and current depend on the load's characteristic as well
- It is possible to step power output instantaneously to any value



# CONTROL OF REACTION RATE

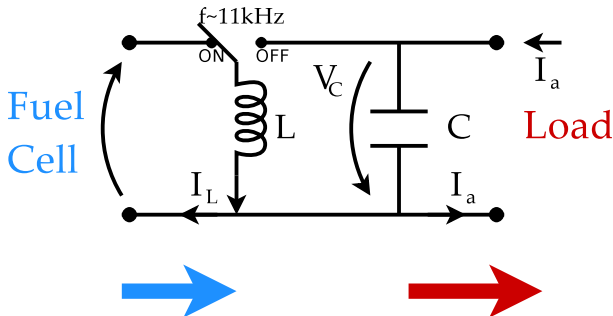
- Control of reaction rate  $i_r$  means control of the overvoltage  $\eta$

$$\eta = \frac{i + i_c - i_r}{C}$$

- The only variable we can modify (albeit indirectly) is the external current  $i$ :
- To control the reaction rate, we will manipulate the external circuit and its relation  $i(V)$
- MOSFET
  - Rheostat
  - Converter
  - ... Anything that modifies the external circuit's characteristic

# CONVERTERS

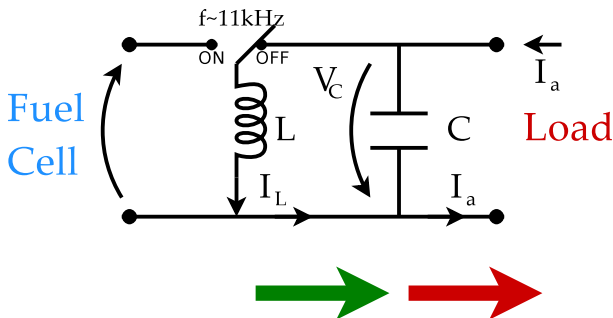
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- Buck-boost converter: can deliver higher or lower voltages
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# CONVERTER CONTROL

- Not a simple problem: no steady state
- Two strategies considered:
  - Pulse-width modulation: we use a continuous variable for the fraction of time we are in the ON mode
  - Switching rules: the switch is set ON and OFF according to some rule

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- Pulse-width modulation is better for calculations, but gives a nonlinear problem of difficult solution
- The switching rules have a better performance, but their simulation is very slow

## COMPOSITION AND PRESSURE CONTROL

- Two separate equations for cathode and anode
- Cathode side must be open-ended (water production)
- Anode side may be dead-ended if hydrogen is (reasonably) pure, possibly with periodic purging
- Reactant concentration does not determine the rate of reaction—It is *the reaction* that requires a certain concentration!

## DEAD-END FLOWS

- Typical case for an anode fed on pure hydrogen
- Fairly simple balance on a single component:

$$\frac{d n_{\text{H}_2}}{d t} = \dot{n}_{\text{H}_2}^{\text{in}} - \frac{i_r A}{2F}$$

- $\dot{n}_{\text{H}_2}^{\text{in}}$  is our manipulated variable, and we have to maintain  $n_{\text{H}_2}$  despite variations in  $i_r$
- We control anode pressure, but the system is unstable and needs feedback

CONTROL PI feedback controller with a pressure measurement with a feedforward component

## OPEN-END FLOWS

- Typical with inert components such as nitrogen, or taking up product water (air, impure hydrogen)
- Assume perfect mixing in the bulk (CSTR)
- Diffusion will occur, and with it mass-transport barriers
- Mass-transport barriers will move to higher values of current for higher reactant concentration in the bulk

# CONTROL OF OPEN-END FLOWS

— Mole fraction dynamics for a generic component  $i$ :

$$\frac{pV}{RT} \frac{dx_i}{dt} = \overbrace{\dot{n}^{\text{in}} (x_i^{\text{in}} - x_i)}^{\text{Feed}} + \frac{i_r A}{F} \left( \underbrace{\nu_i}_{\text{Reaction}} \overbrace{- x_i \sum_i \nu_i}^{\text{Dilution}} \right)$$

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CONTROL Pure feedforward

# TEMPERATURE CONTROL

— Enthalpy balance:

$$A \hat{c}_p \frac{dT}{dt} = \overbrace{\dot{H}^{\text{in}} - \dot{H}^{\text{out}}}^{\text{Usually } < 0} - \overbrace{ViA}^{\text{Electric power}} - \dot{H}^{\text{loss}}$$

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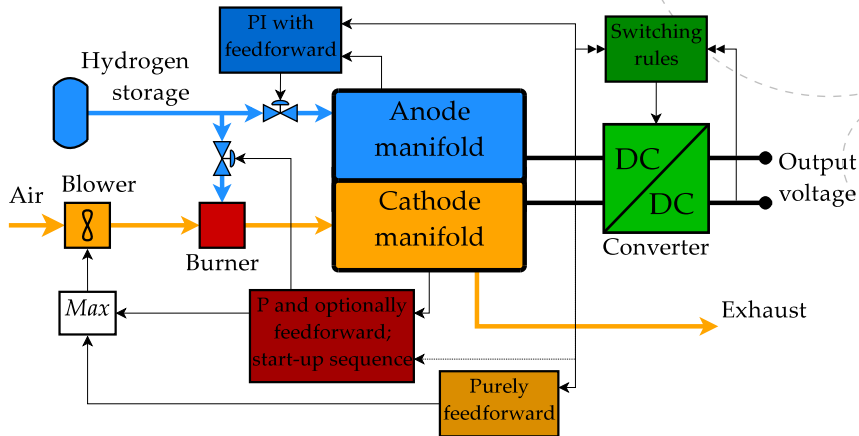
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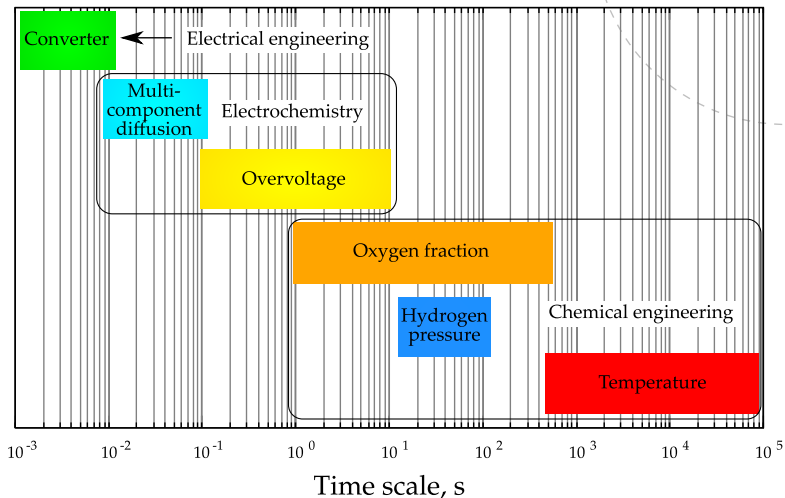
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- No additional requirement on air flow capacity

# OVERALL CONTROL STRUCTURE



# TIME SCALES OF FUEL-CELL DYNAMICS



# CONCLUSIONS

- Fuel-cell systems can deliver power very rapidly; there are slower *internal* dynamics
- The electrochemical transient's nature allows perfect control of power output from a cell
- Simple control algorithms for pressure, composition and temperature are good enough
- Converter control is somewhat less friendly, and is critical for system performance

# ACKNOWLEDGEMENTS

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*Thank you for your attention!*