

NTNU

Innovation and Creativity

Near-Optimal Output Feedback Control of Dynamic Processes

Håkon Dahl-Olsen, Sridharakumar Narasimhan
and Sigurd Skogestad

Optimal operation

- Two paradigms for implementation
 - i. on-line optimization using measurements for model or state estimate updates (RTO, MPC)
 - ii. inherent optimal operation by exploiting off-line information in control structure design

Off-line optimization

- Lower computational load
 - Still a significant problem for dynamic real-time optimization
- Less sensitive to modeling errors

Dynamic optimization

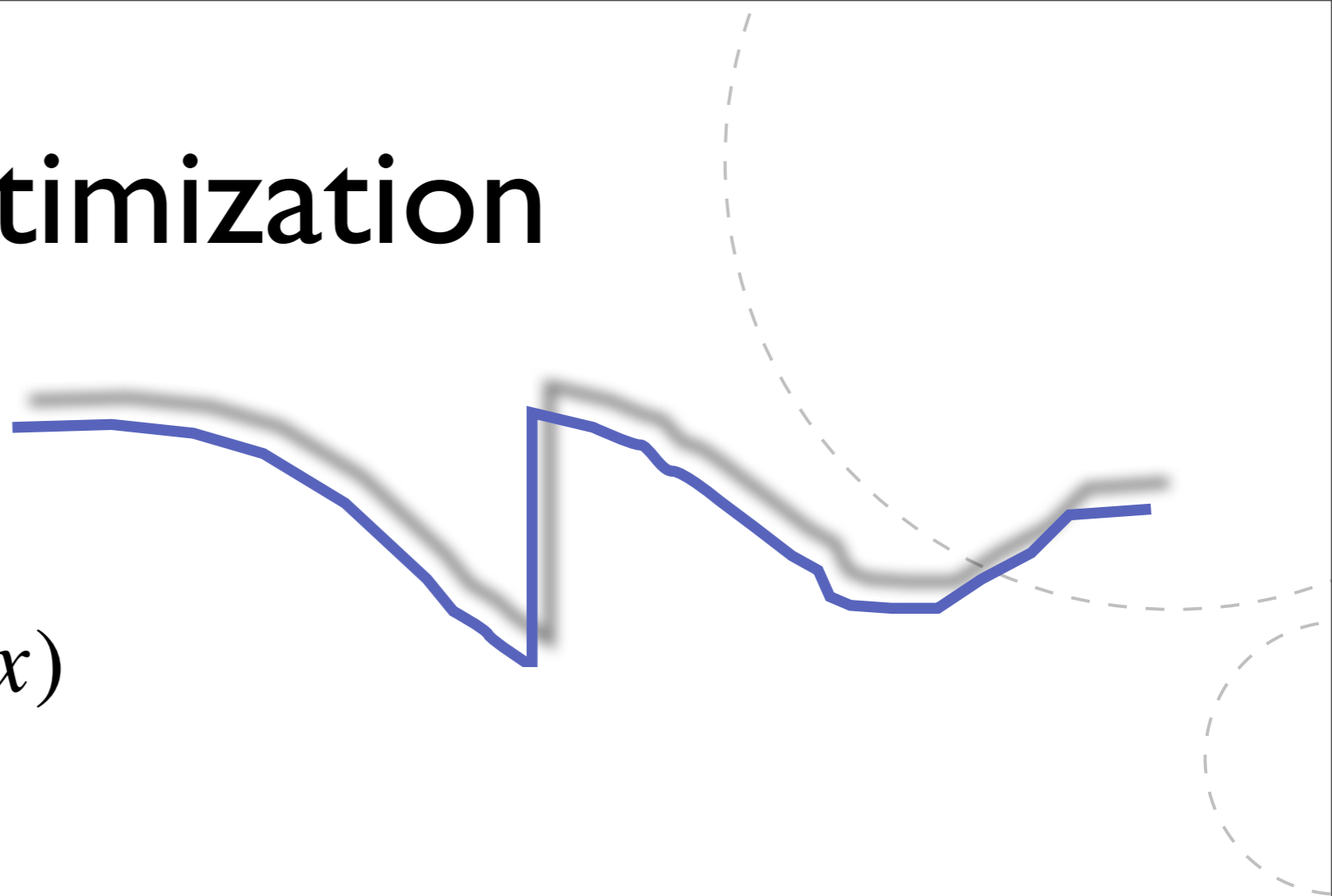
$$\min_{u(t), t_f} J(x(t_f))$$

$$\dot{x} = f(x, u) \quad y = h(x)$$

$$c(x, u) \leq 0$$

$$u(t) \in U[0, T]$$

$$x(t_f) \in X$$



$$H(t) = \lambda^T f(x, u) + \mu^T c(x, u)$$

$$\dot{\lambda}_i = -\frac{\partial H}{\partial x_i}$$

Hamiltonian

- takes minimum along optimal path
- has a constant value along the optimal path for problems not depending explicitly on time
- can be used to define a loss in sub-optimal operation:

$$L(t) = H(t) - H_{\text{opt}}(t)$$

Loss related to outputs

$$L(t) = \underbrace{H_u}_{0} \delta u + \frac{1}{2} \delta u^T H_{uu} \delta u$$

Need to relate variations in inputs
to variations in outputs

$$\delta y = \frac{\partial h}{\partial x^T} \frac{\partial x}{\partial u^T} \delta u = G \delta u$$

$$L(t) = \frac{1}{2} \delta y^T G^{-T} H_{uu} G^{-1} \delta y$$



NTNU

Innovation and Creativity

Maximum gain rule for dynamic optimization

- Assume the model is scaled such that $\delta y_{\max} \approx 1$

Select y 's to minimize the following expression along the nominal trajectory

$$\min \left(\int_{t_0}^{t_f} \left\| G^{-T} H_{uu} G^{-1} \right\|_2^2 dt \right)^{1/2}$$

How to obtain G

- How does variations in inputs map to the states?
- Neighboring optimal control gives $u=Kx$
- We estimate G by

$$G \approx \frac{\partial h}{\partial x^T} K^+$$

Example



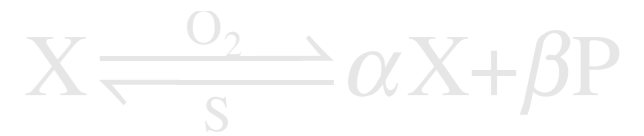
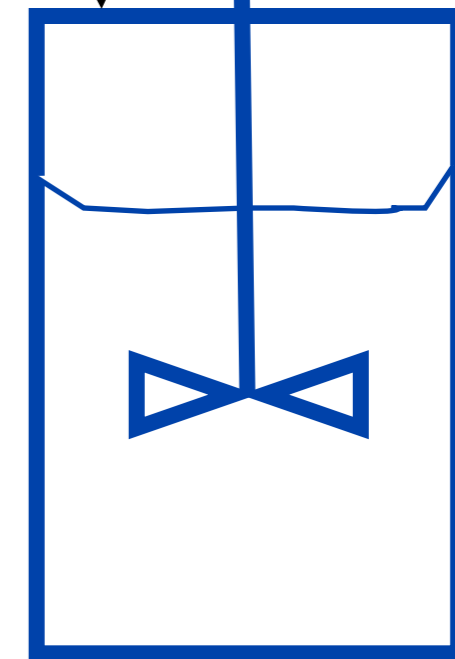
Bioreactor

- Maximize production of product P in a fed-batch bioreactor with fixed final time of 150 hours
- Reaction is driven by the presence of a substrate S, which is consumed in the biomass generation
- The biomass concentration is constrained

Example

$X < 3.7$	Biomass concentration
S	Substrate concentration
P	Product concentration
V	Volume
$u < 1$	Substrate feedrate

u [L/h]
 $S_{in} = 200$ g/L



Bioreactor

Example

$X < 3.7$	Biomass concentration
S	Substrate concentration
P	Product concentration
V	Volume
$u < 1$	Substrate feedrate



Bioreactor

$$\dot{X} = \mu(S)X - \frac{u}{V}X$$

$$\dot{S} = -\frac{\mu(S)X}{Y_X} - \frac{vX}{Y_P} + \frac{u}{V}(S_{in} - S)$$

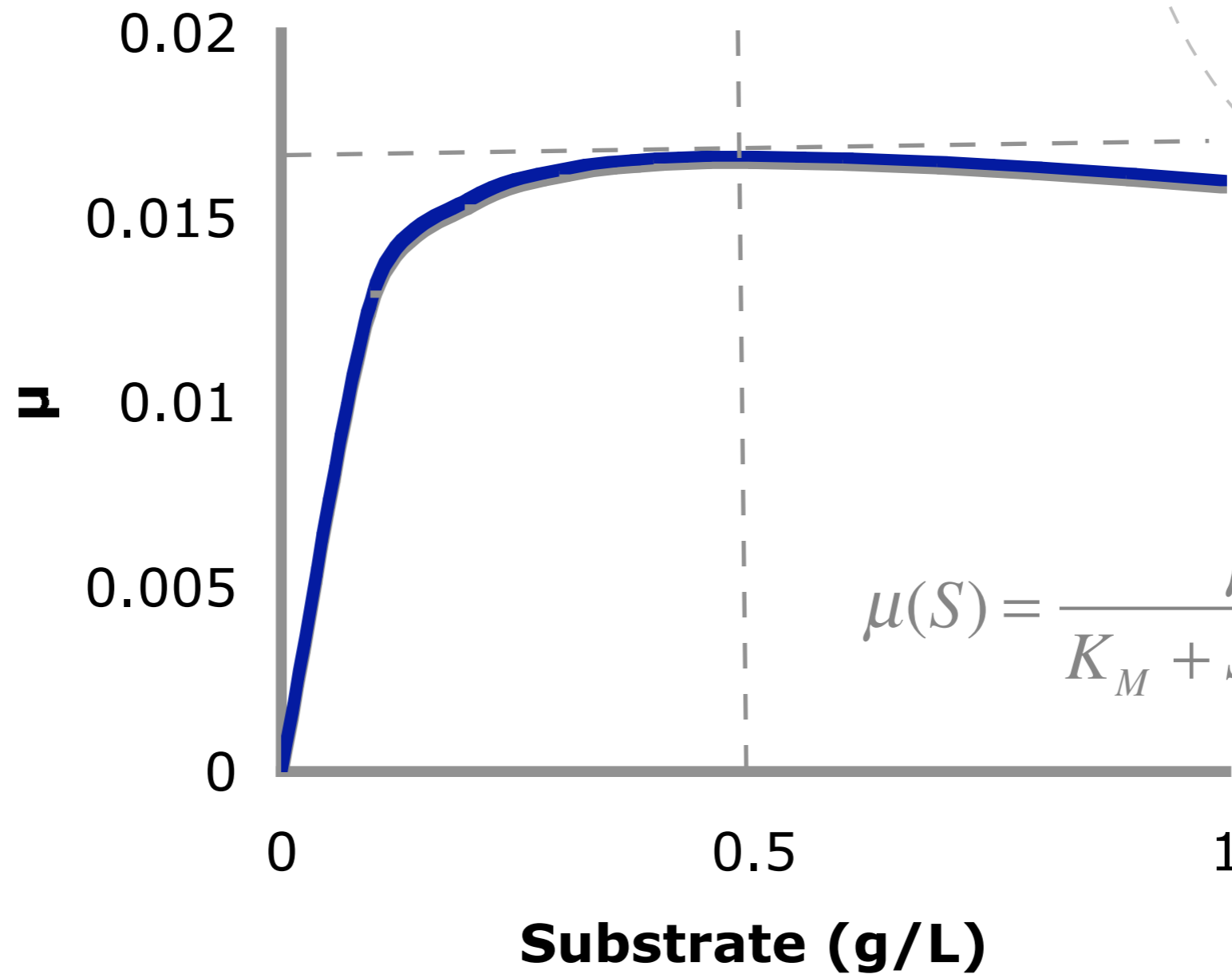
$$\dot{P} = vX - \frac{u}{V}P$$

$$\dot{V} = u$$

Biomass growth rate



Bioreactor



Consider gain magnitude



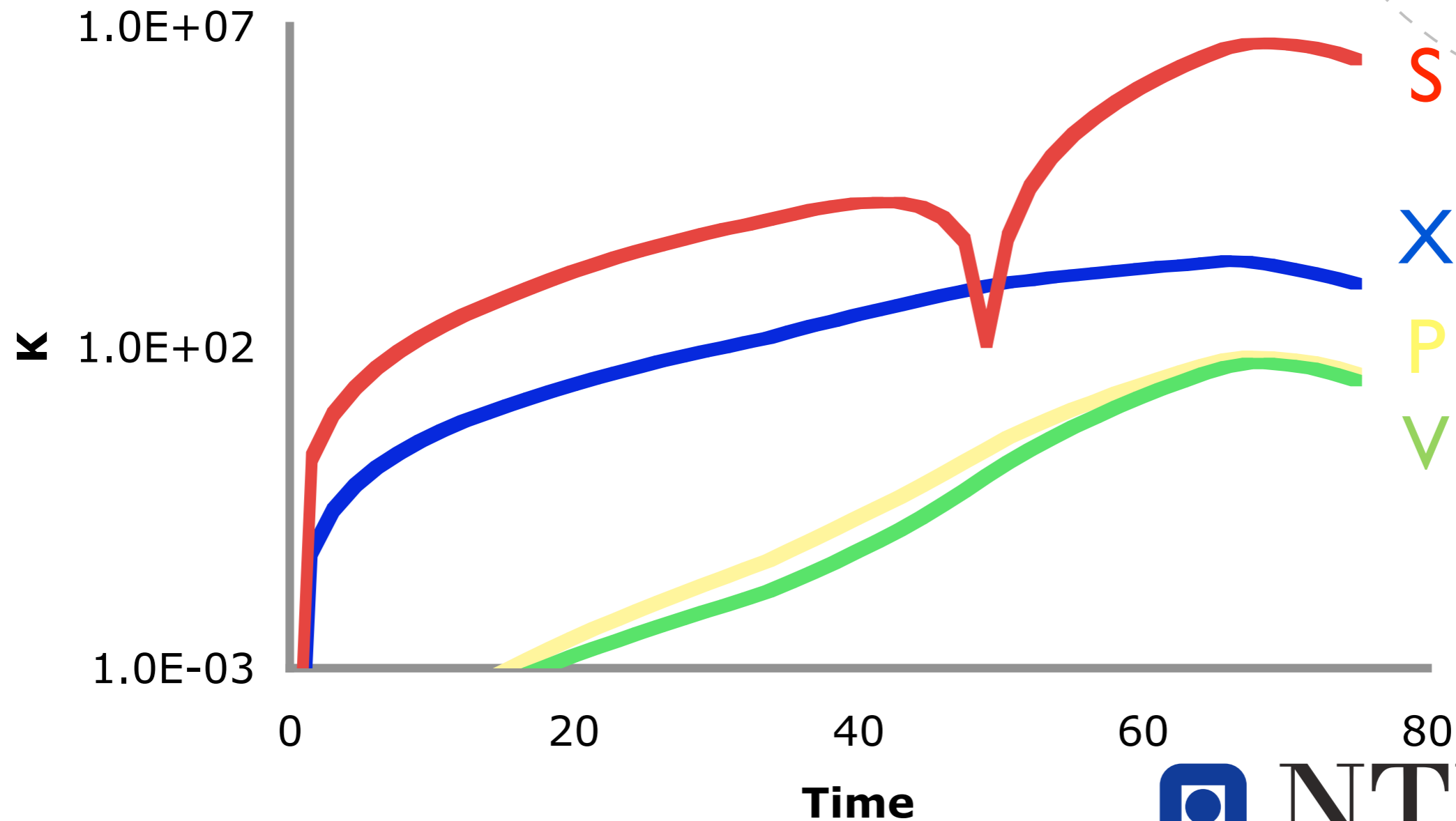
Bioreactor

- Transformation of input: $\xi = \sqrt{u}$
- $H_{\xi\xi}$ is constant
- Minimizing of $1/K^2$ corresponds to maximizing K^2

Comparison of gains



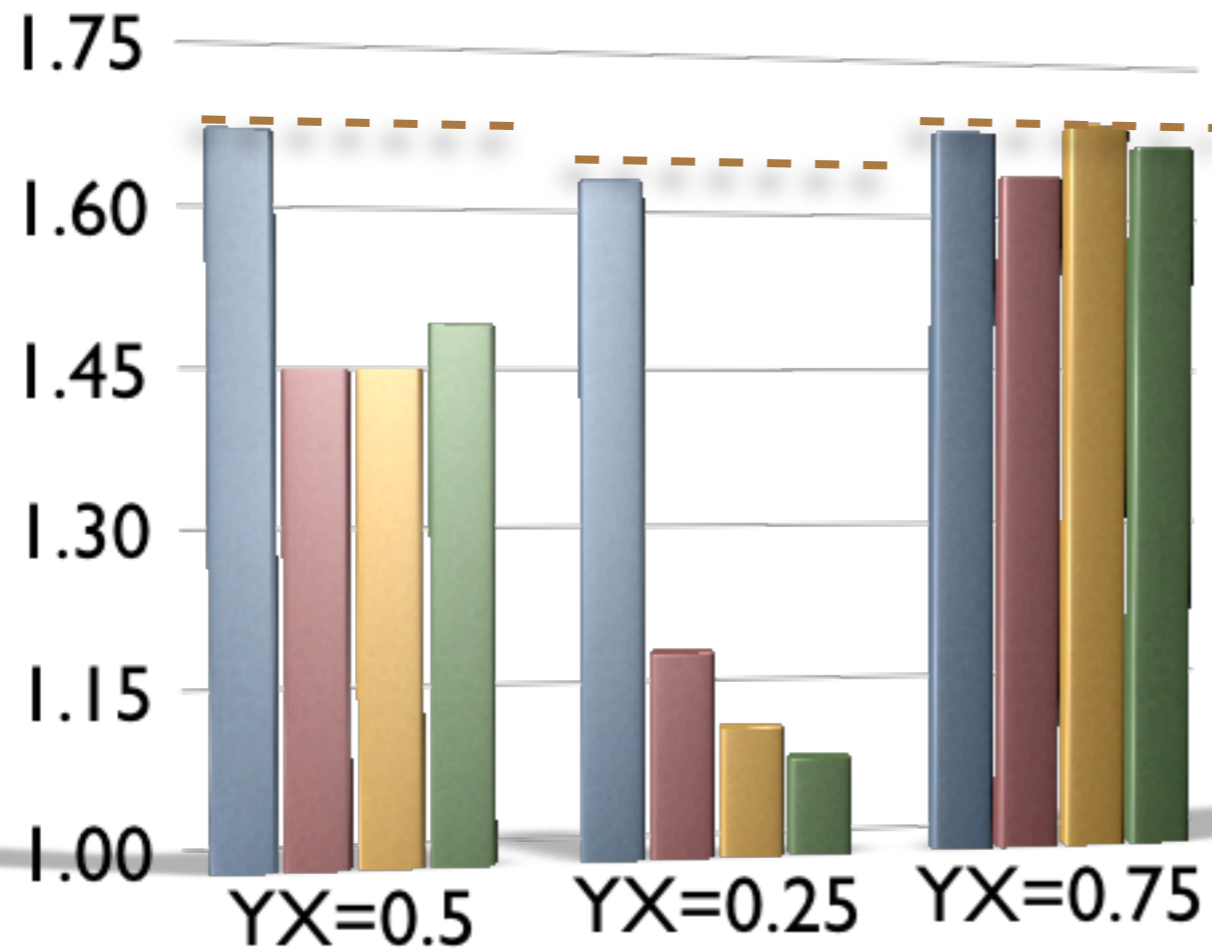
Bioreactor



NTNU

Innovation and Creativity

Simulation results



- Control of S
- X-step
- Open loop
- Control of P

Summary

- The maximum gain rule can be extended to unsteady-state problems
- Using the solution of the time-varying LQR problem, it is possible to get a good estimate of the time-varying gain needed to use the maximum gain rule