

# An efficient computational strategy for dynamic real-time optimization

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## Dynamic Real-Time Optimization

### Current set-up for RTO & MPC

*Maximize profit*

#### Steady-State Optimization

↓  
*set-points*

#### Process with tracking, (non)linear MPC

Chemical Process

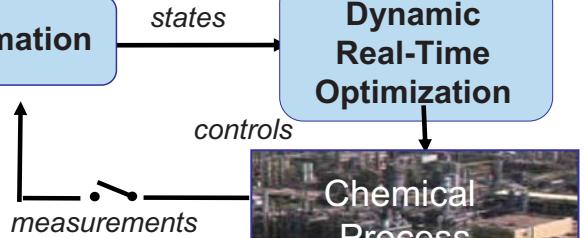
- Inconsistent objectives
- Dynamic degrees of freedom not exploited for profitable operation

### Dynamic Real-Time Optimization (DRTO):

Economically optimal operation in transient processes at any time!

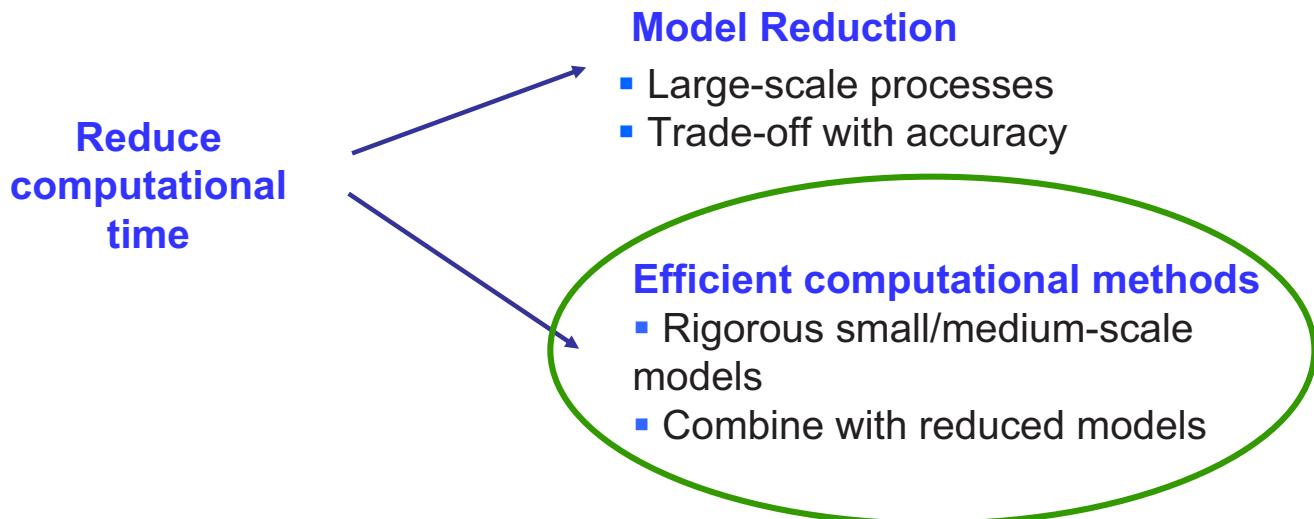
*Maximize profit*

#### Estimation



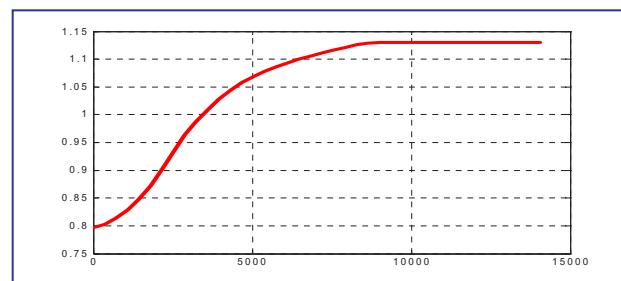
Obtain solutions of dynamic optimization problem in real-time but:

- Large-scale systems, complex models
- Different time-scales
- Severe nonlinearities e.g. reaction kinetics



## Neighboring-Extremal Updates

Objective:  
Fast updates of optimal trajectory  
under uncertainty



**Neighboring Extremal Updates:** Fast solution of related problem in the neighborhood of a nominal optimal solution

Related methods:

Indirect methods for optimal control: Neighboring extremal feedback law  
(Bryson and Ho, 1969, Pesch, 1979)

Direct methods: Diehl et al., 2002: Real-time iterations  
Kadam and Marquardt, 2004: Sensitivity-based updates  
Zavala and Biegler, 2008: Advanced-step NMPC

# Optimization problem definition

Optimization problem formulation on receding horizon:

$\min_{u^j(t)} \Phi(x(t), u_j(t), t_0, t_f)$	<i>Economic objective function</i>
s.t. $\dot{x}(t) = f(x(t), u^j(t), d^j(t), \hat{\theta}),$ $y(t) = g(x(t), u^j(t), d^j(t), \hat{\theta}),$ $x(t^j) = \hat{x}^j,$	$\left. \begin{array}{l} \text{DAE system (process model)} \\ \text{initial conditions} \end{array} \right\}$
$0 \geq h(x(t), y(t), u^j(t)),$ $0 \geq e(x(t_f)),$	<i>path constraints</i> <i>endpoint constraints</i>
$t \in [t^j, t_f^j],$ $t^j := t^{j-1} + \Delta t$	<i>time horizon</i> <i>horizon shift (index j)</i>

## Reformulation of the infinite-dimensional problem

- Control vector parameterization (single-shooting)

$$u_i(t) \approx \sum_{k \in \Lambda_i} z_{i,k} \phi_{i,k}(t)$$

- Collect different uncertainties in vector  $p$ :

- Model uncertainties  $\hat{\theta}$
- Disturbances  $d(t)$  parametrized by  $c^j$
- Estimated state variables  $\hat{x}^j$

$$p = (c^j, \hat{\theta}, \hat{x}^j) \in \mathbb{R}^{n_p}$$

- Reformulation as nonlinear parametric program problem (NLP)**

$\min_{z, t_f} \Phi(z, p)$	<i>DAE system is solved by underlying numerical integration</i>
s.t. $0 \geq g(z, p)$ $0 \geq e(x(t_f))$	

# Sensitivity-based updates

Idea: Exploit sensitivity information of offline/previosuly solved optimization problem to generate a fast approximation of the optimal update

(Fiacco, 1983)

Solve Quadratic Program online (Kadam and Marquardt, 2004)

$$\begin{aligned} \min_{\Delta z} \quad & \frac{1}{2} \Delta z^T L_{zz}(p_0) \Delta z + \Delta p^T L_{pz}(p_0) \Delta z + f_z(p_0) \Delta z \\ \text{s. t.} \quad & g(p_0) + g_z(p_0) \Delta z + g_p(p_0) \Delta p \geq 0 \end{aligned}$$

*L: Lagrange function  
g: constraints*

Parametric uncertainty:  $\Delta p = p - p_0$

Sensitivities are computed at the nominal parameter  $p_0$

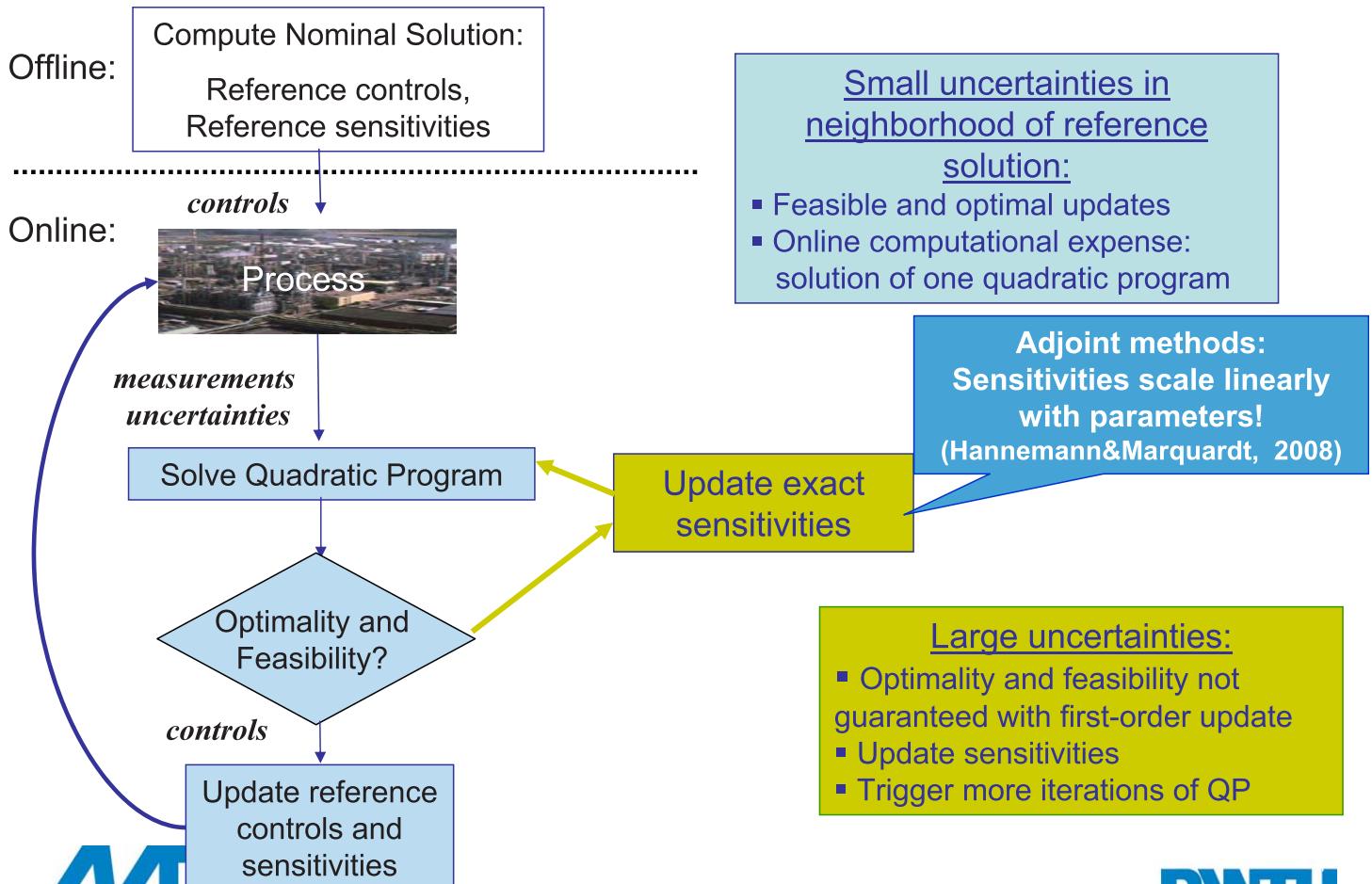
→ Fast first-order prediction of optimal controls  
& update of active constraints



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## Algorithm for online trajectory updates



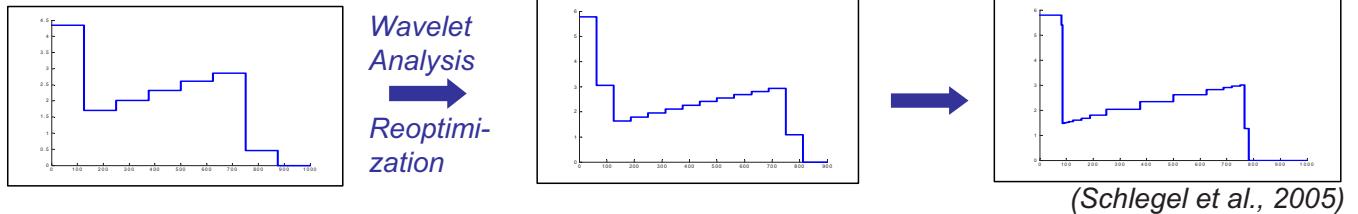
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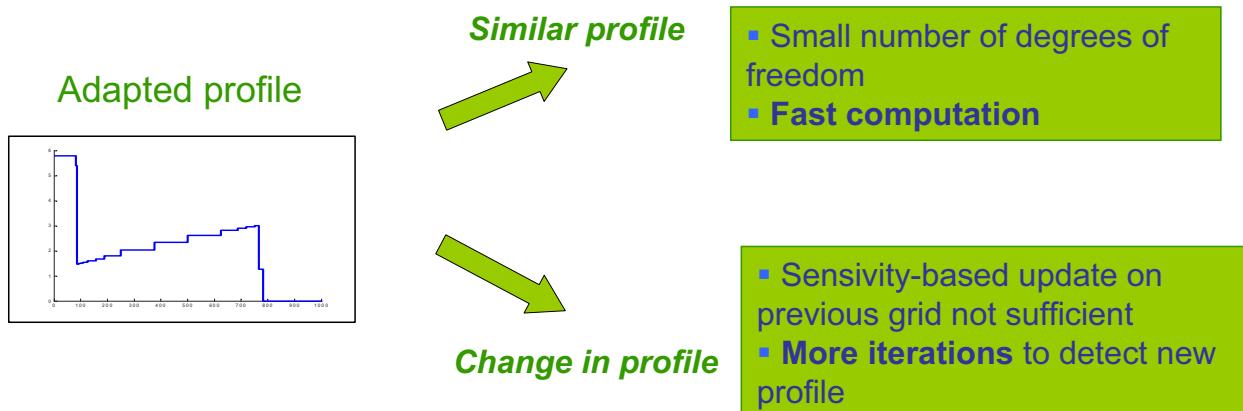
# Grid refinement strategy

- Offline adaptation



→ Reduction of degrees of freedom while maintaining solution accuracy!

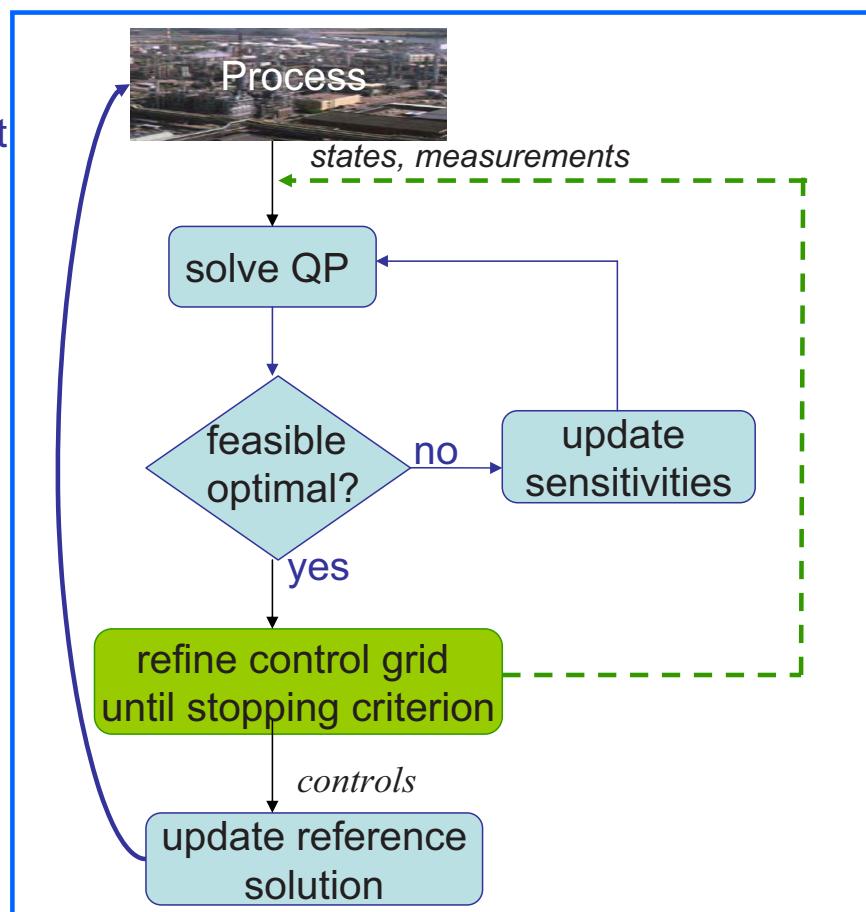
- Online adaptation under uncertainties:



## Online adaptation of control grid

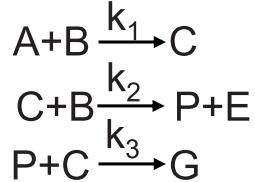
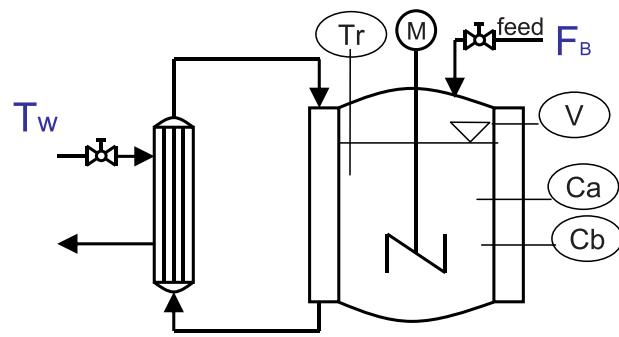
Implementation of grid refinement in the online algorithm:

Refinement of solution if time is available



# Example 1: Real-time optimization of semi-batch reactor

## Williams-Otto Benchmark Example



**Operational Objective:**  
Maximize Product P

## Optimization problem formulation

$$\max_{F_{B_{in}}(t), T_w(t)} Yield(t_f)$$

s.t. process model

$$0 \leq F_{B_{in}}(t) \leq 5.784 \frac{\text{kg}}{\text{sec}},$$

$$20 \leq T_w(t) \leq 100 \text{ }^{\circ}\text{C},$$

$$60 \leq Tr(t) \leq 90 \text{ }^{\circ}\text{C},$$

$$0 \leq V(t_f) \leq 5 \text{ m}^3.$$

## Uncertainties

$$k_i = a_i \exp\left(\frac{-b_i}{Tr + 273.15}\right), i = 1, \dots, 3$$

$$b_{1,0} = 6.6667 \text{ sec}^{-1}$$

$$T_{in} = 35 \text{ }^{\circ}\text{C}$$

$$p := [T_{in}, b_1, \hat{x}]$$



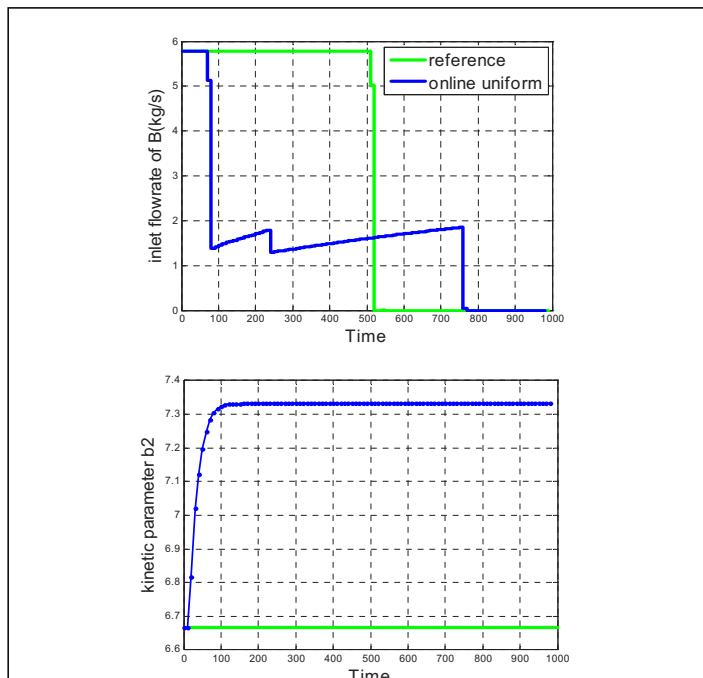
State estimation with EKF, sampling time of 10 s.



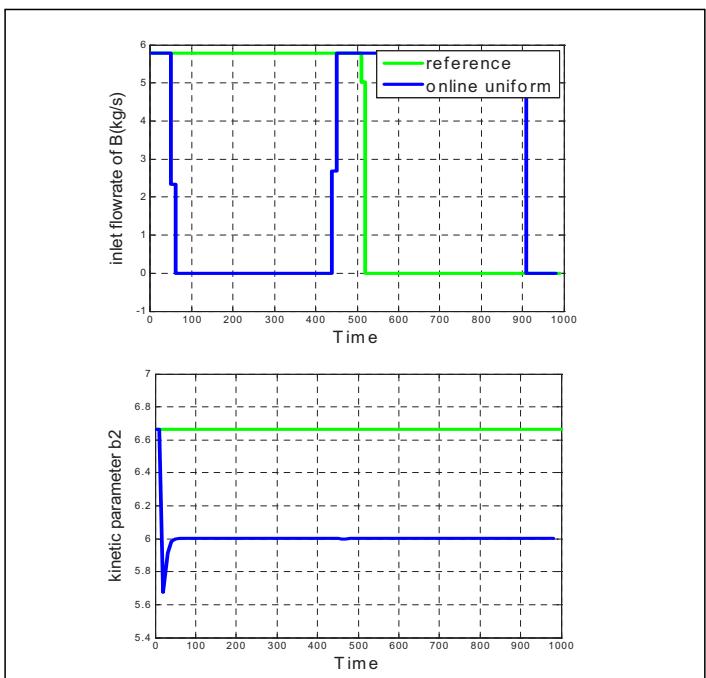
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## Real-time optimization results

Initial condition for kinetic parameter +10%



Initial condition for kinetic parameter -10%,



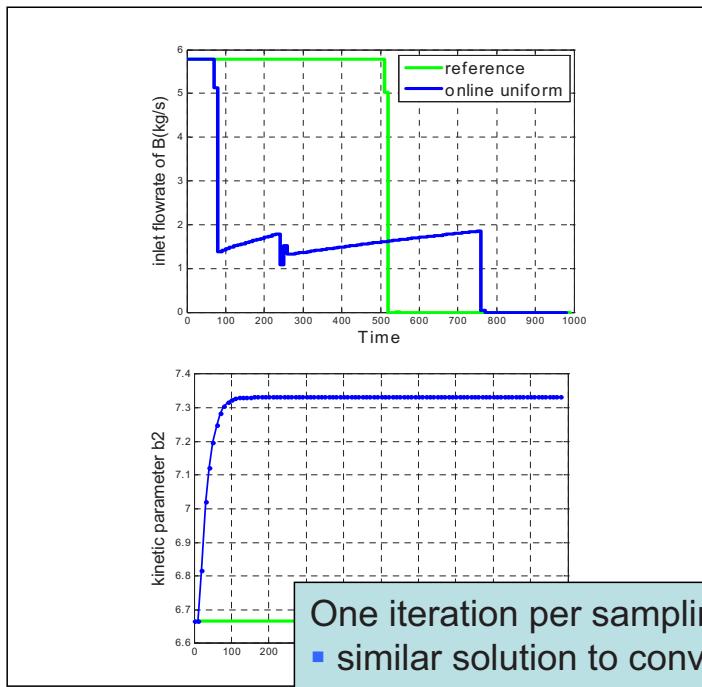
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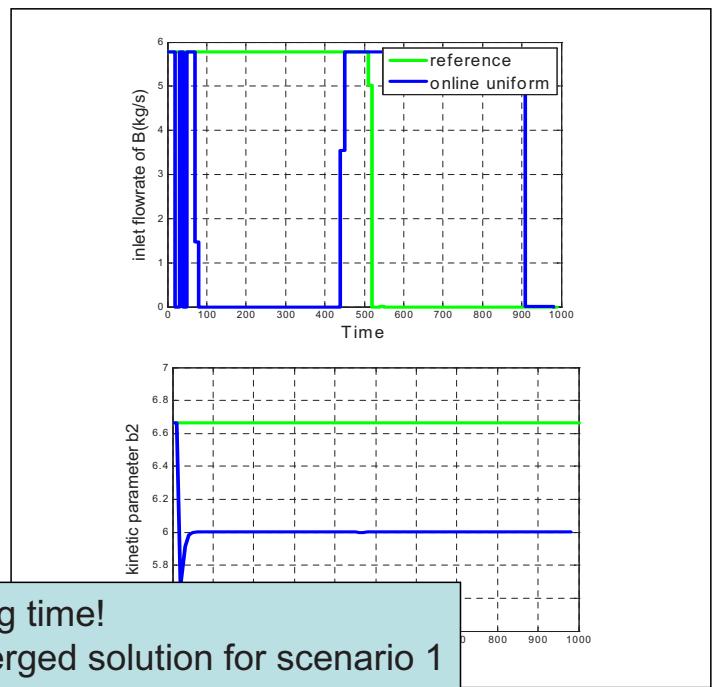


# Comparison with online iterations

Initial condition for kinetic parameter +10%



Initial condition for kinetic parameter -10%,

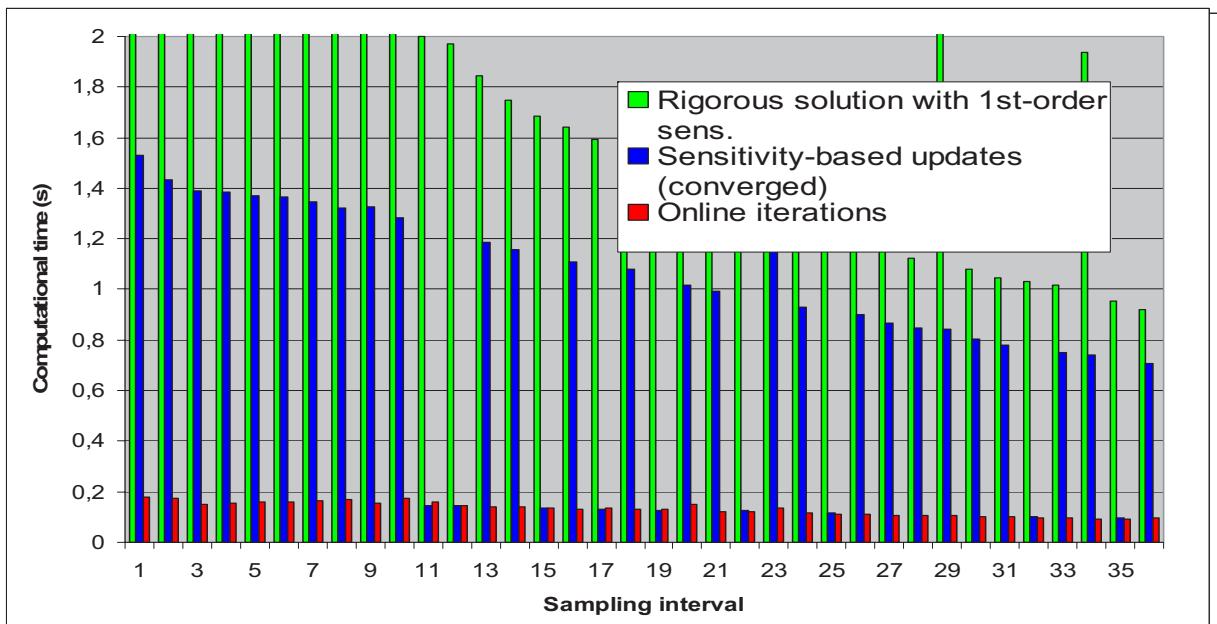


One iteration per sampling time!

- similar solution to converged solution for scenario 1
- oscillations observed for scenario 2

## Comparison of computational performance

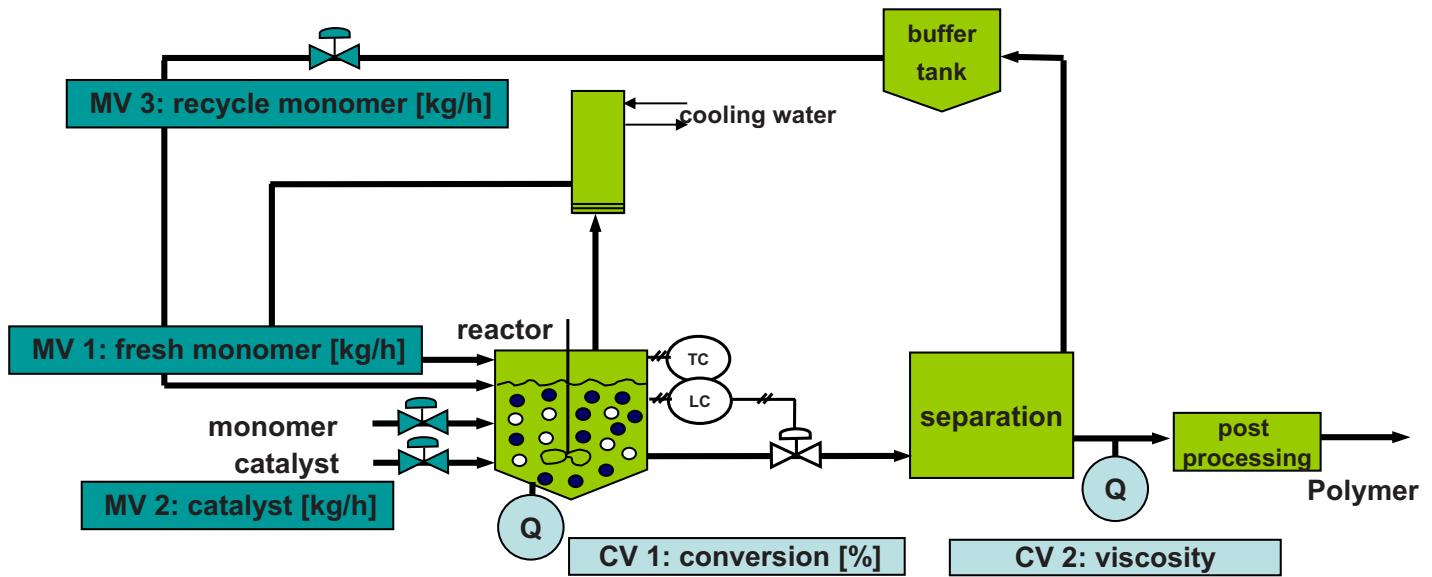
- Compared to rigorous solution with first order sensitivities
- Sensitivity-based updates with second-order exact sensitivities  
→ fast convergence
- Online iterations: computational effort very low



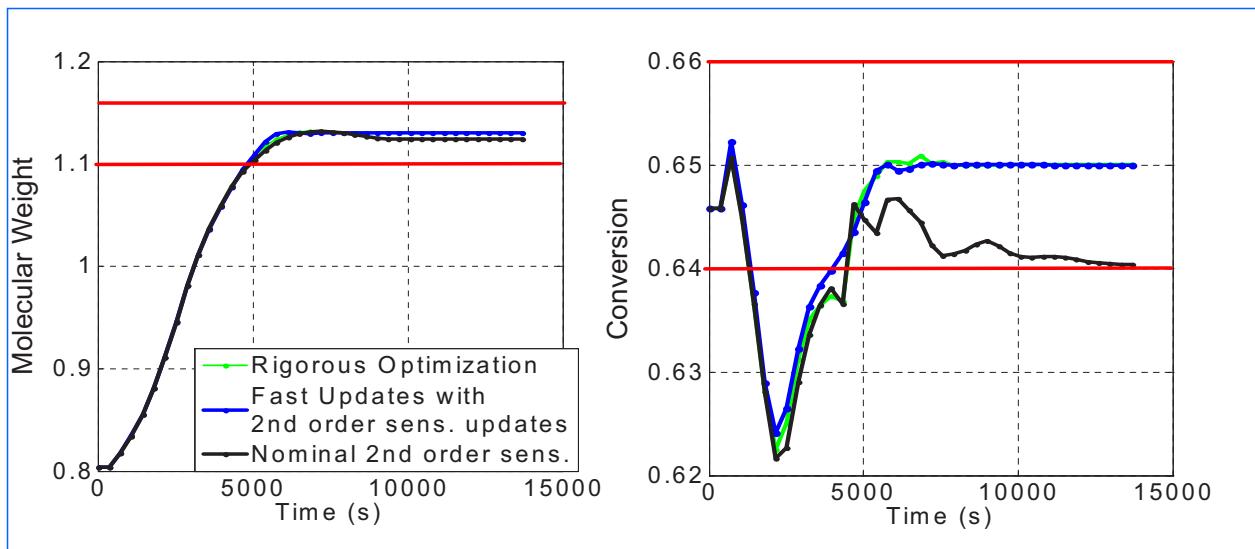
## Example 2: Copolymerization Reactor

- complex reaction mechanism
- large-scale model (~ 2000 equations)
- 3 control variables, 6 path constraints

- process operations tasks:
- optimal load change
  - optimal grade change



## Results with Fast Updates



Fast updates with online update of 2nd order sensitivities:

=> Close to rigorous optimal solution

- Method based on neighboring extremal updates was presented
  - Fast convergence
  - Solution accuracy is adjusted by a trigger
- Control performance:
  - Trade-off between computational delay and solution accuracy
  - Adjust number of iterations
- Adaptation:
  - Grid refinement allows reduction of degrees of freedom
  - Automatic structure detection => minimum number of parameters

## Acknowledgments

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