

## Estimation of Unmeasured Oil and Water Purities for a Continuous Subsea Gravity Separator

*Tamal Das and Johannes Jäschke*

---

Controlling the quality of outlet streams in subsea oil-water gravity separators is currently difficult, because existing subsea sensors for oil and water purity are not sufficiently accurate. We address this issue by developing a dynamic model for a gravity separator that is used to predict and estimate the concentration of outgoing streams. We consider that the fluids inside the separator separate into layers of water, emulsion and oil, where the emulsion layer consists of two sections: sedimentation layer and dense-packed layer. The separator includes a weir that prevents the emulsion and the water from flowing over the weir leaving only oil to flow over the weir to the oil outlet section. The removal of the water takes place from the bottom of the separator from the water outlet.

Frising reviewed batch gravity separation models reported in the literature in [1] and classified them into sedimentation-based models and coalescence-based models. Sedimentation based models [2-6] are based on interfacial coalescence between droplets and interface, and sedimentation of droplets; whereas the coalescence based models [7,8] focus on binary as well as interfacial coalescence of the droplets of the dispersed phase. Sayda *et al.* [9] developed a model for a continuous gravity separation, however, their model ignores coalescence effects. A model for a horizontal pipe separator for continuous oil-water separation described in [10], combines principles from a sedimentation based model [11] and a coalescence-based model by Henschke [8]. Pipe separators, however, differ from gravity separators as gravity separators are not completely filled with liquids and often are designed with a weir.

Our model predicts oil content in outgoing oil and water streams based on lumped total and partial mass balances for each layer, including principles from sedimentation based models and Henschke's model for inter-layer mass transfer terms. It captures the effect of total inlet flow rate, inlet oil cut, and inlet droplet size on purities of outlet streams and thickness of each layer. We use the model in a Kalman-based non-linear estimator for estimating unmeasured variables, such as oil and water purities using level and density measurements.

[1] Frising, T., Noik, C. and Dalmazzone, C., 2006. The liquid/liquid sedimentation process: from droplet coalescence to technologically enhanced water/oil emulsion gravity separators: a review. *Journal of Dispersion Science and Technology*, 27(7), pp.1035-1057.

[2] Jeelani, S.A.K. and Hartland, S., 1986. Prediction of dispersion height in liquid-liquid gravity settlers from batch settling data. *Chemical engineering research & design*, 64(6), pp.450-460.

[3] Jeelani, S.A.K., Pandit, A. and Hartland, S., 1990. Factors affecting the decay of batch liquid-liquid dispersions. *The Canadian Journal of Chemical Engineering*, 68(6), pp.924-931.

- [4] Jeelani, S.A.K. and Hartland, S., 1993. The continuous separation of liquid/liquid dispersions. *Chemical engineering science*, 48(2), pp.239-254.
- [5] Jeelani, S.A.K., Panoussopoulos, K. and Hartland, S., 1999. Effect of turbulence on the separation of liquid-liquid dispersions in batch settlers of different geometries. *Industrial & engineering chemistry research*, 38(2), pp.493-501.
- [6] Jeelani, S.A.K., Hosig, R. and Windhab, E.J., 2005. Kinetics of low Reynolds number creaming and coalescence in droplet dispersions. *AIChE journal*, 51(1), pp.149-161.
- [7] Lobo, L., Ivanov, I. and Wasan, D., 1993. Dispersion coalescence: Kinetic stability of creamed dispersions. *AIChE journal*, 39(2), pp.322-334.
- [8] Henschke, M., Schlieper, L.H. and Pfennig, A., 2002. Determination of a coalescence parameter from batch-settling experiments. *Chemical Engineering Journal*, 85(2), pp.369-378.
- [9] Sayda, A.F. and Taylor, J.H., 2007, July. Modeling and Control of Three-Phase Gravity Separators in Oil Production Facilities. In *American Control Conference, 2007. ACC'07* (pp. 4847-4853). IEEE.
- [10] Pereyra, E., Mohan, R.S. and Shoham, O., 2013. A Simplified Mechanistic Model for an Oil/Water Horizontal Pipe Separator. *Oil and Gas Facilities*, 2(03), pp.40-46.
- [11] Hartland, S. and Jeelani, S.A.K., 1988. Prediction of sedimentation and coalescence profiles in a decaying batch dispersion. *Chemical engineering science*, 43(9), pp.2421-2429.