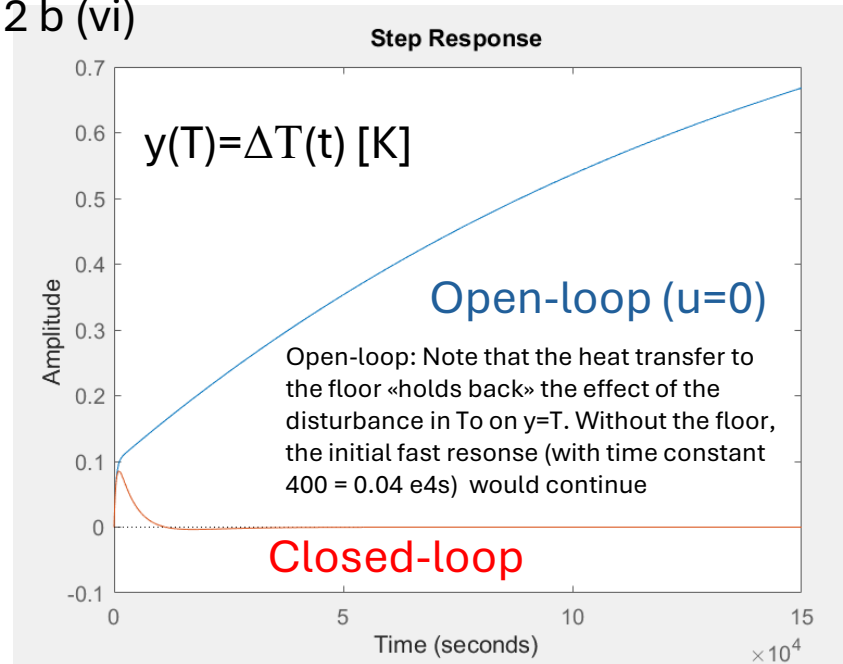


Exam 2024

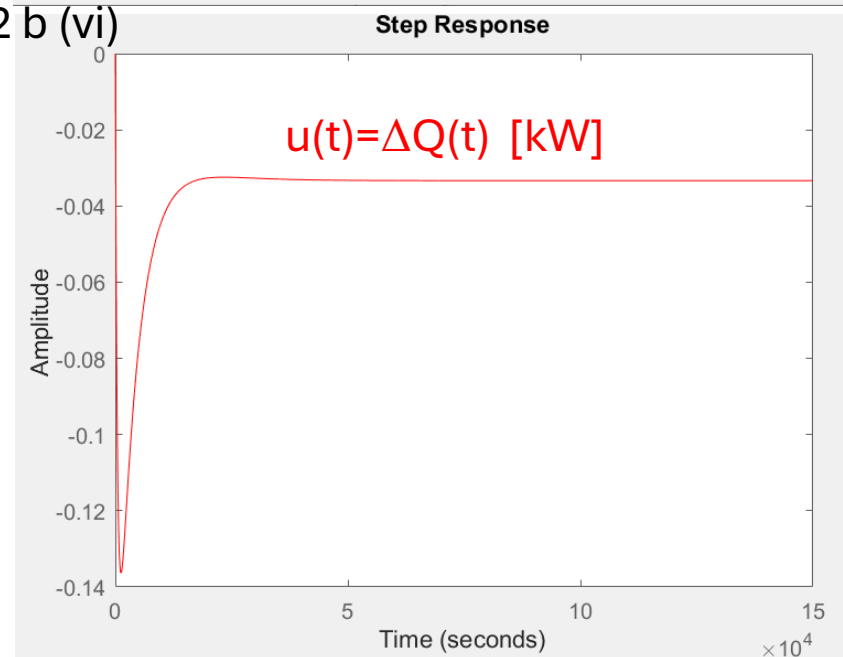
Process control

Problem 2b

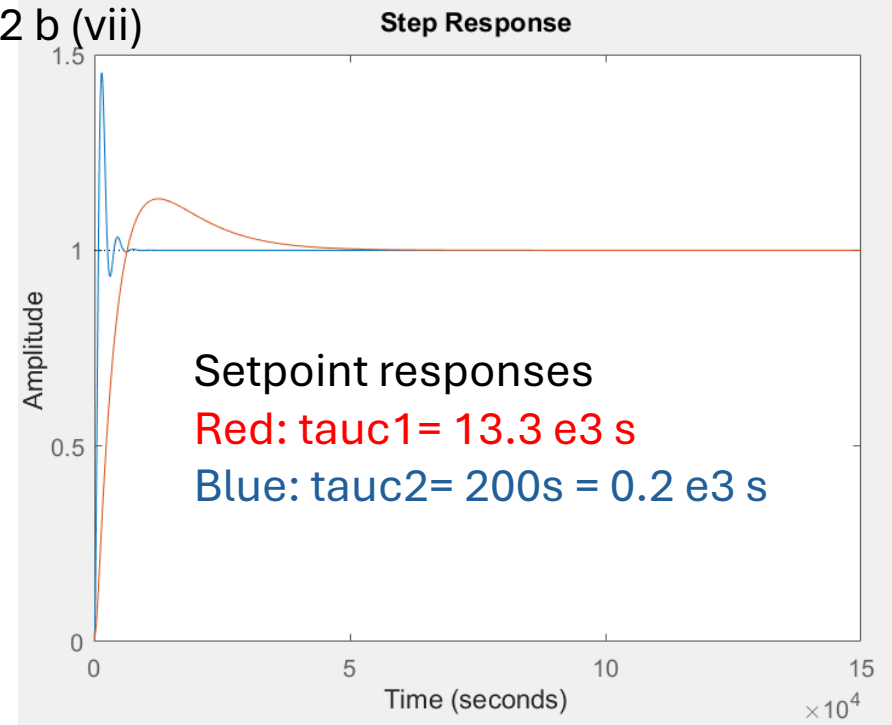
2 b (vi)



2 b (vi)



2 b (vii)



%Exam 2024

 $s=\text{tf}('s');$ $G_b = 30/((15\text{e}4*s+1)*(400*s+1))$ $G_{db} = (1.5\text{e}4*s+1)/((15\text{e}4*s+1)*(400*s+1))$ $C = 1.5*(1 + 1/(13351*s))$ $S = 1/(1+G_b*C)$ $T_d = S*G_{db}$ $KSG_d = -C*T_d$ figure(1), step($G_{db}, T_d, 150\text{e}3$) % disturbancefigure(2), step($KSG_d, 150\text{e}3, 'red'$) % disturbance $T = 1-S$ $C_2 = 12.5*(1+1/(1600*s))$ $S_2 = 1/(1+G_b*C_2); T_2=1-S_2;$ figure(4), step($T_2, T, 150\text{e}3$) % setpoints

2 b (vii)

Discussion: (a) There is not much point in reducing tauc to tauc_2 because the response with tauc_1 is already good enough, even for setpoint changes. Actually the 50% overshoot for $y=T$ with tauc_2 is not desirable. (b) Cascade control (based on $y_2=T_f$) is not helpful because (i) there are no disturbances that directly effect T_f . (ii) there is no nonlinearity.