

The German “Energiewende” – a Systems & Control Perspective

Wolfgang Marquardt

Chairman of the Board of Directors of
Forschungszentrum Jülich GmbH, Jülich, Germany,
on leave from RWTH Aachen University, Germany

Award Lecture, Nordic Process Control Workshop, Sigtunastiftelsen, August 25, 2016

Content

- **Where do I work?**
- The German “Energiewende”: objectives and challenges
- Stabilizing the grid by design: Managing storage and demand side
- “Intelligent” grid management: Demonstrator and research infrastructure
- Control methods and tools: Hierarchical and distributed architectures
- Take away messages



Major Professional Experiences, since 1992



Forschungszentrum Jülich
 Chairman of the Board
 of Directors & Scientific
 Director, since 2014
 Research Management



RWTH Aachen University

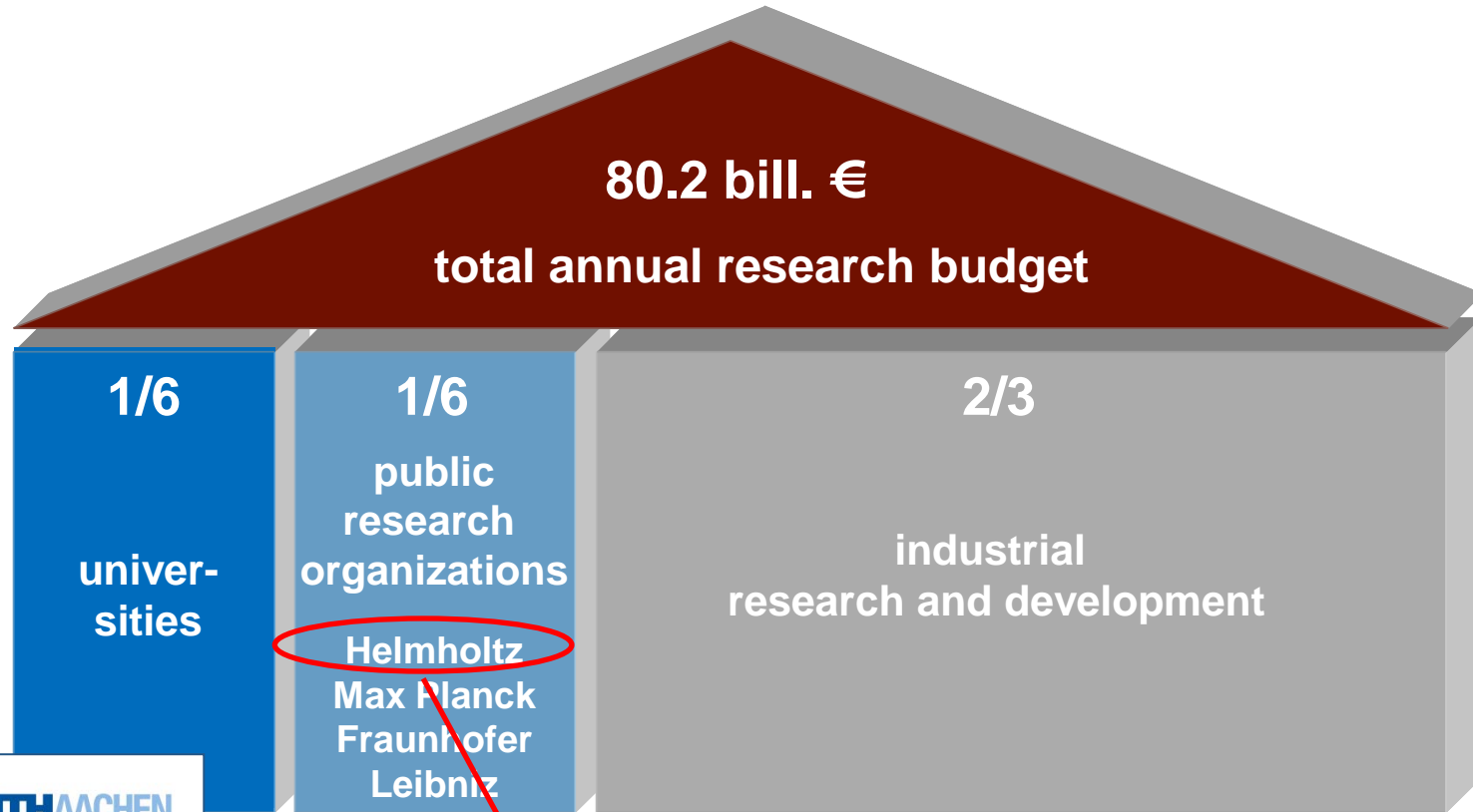
Professor, Process Systems Engineering, 1992-2014
 (Co-)Director, DFG CRC 476 & 540, 1998-2008
 Co-Director, AICES & Fuel Design Center, 2008-2011
 RWTH Strategy Board, 2007-2011, since 2014
 Research, Teaching, Collaborative Research Centers



**German Council of
 Science & Humanities**
 Member & Chairman
 2010-2014,
 Advisor to the State and
 Federal Governments on
 Science Policy



The Big Picture: German Research System

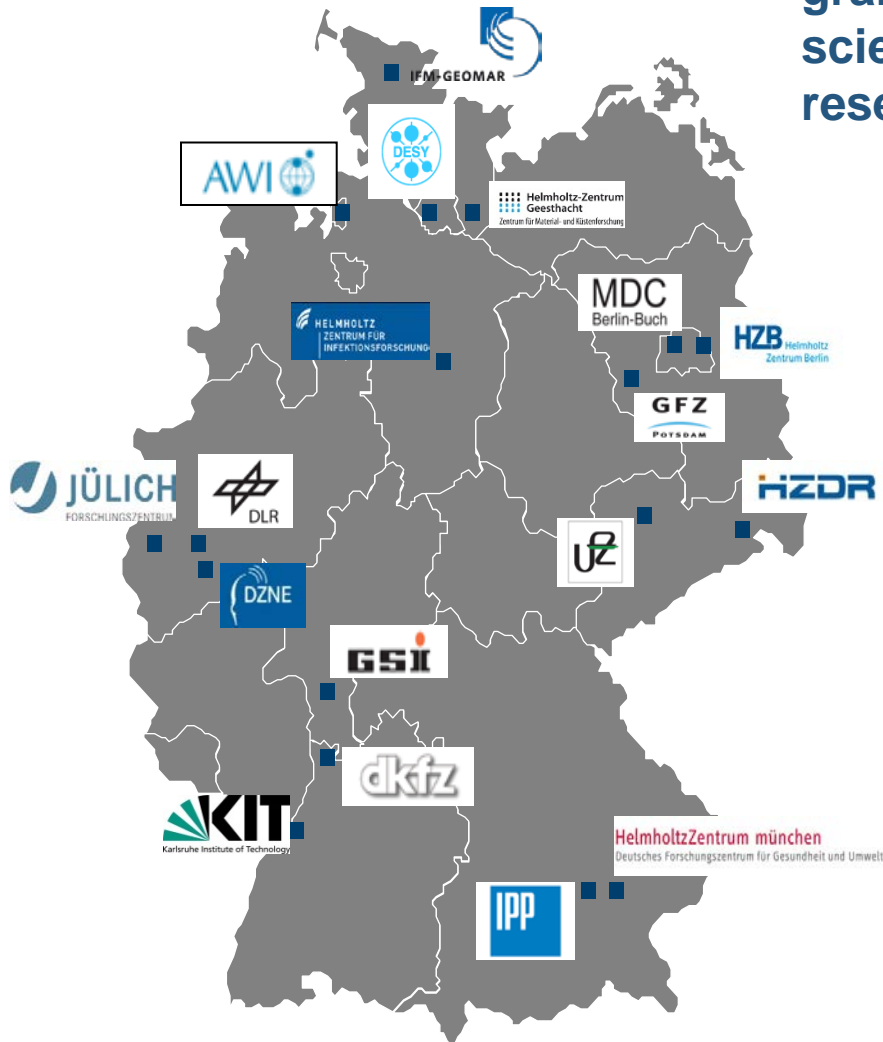





18 centres, 4.24 bill. €
38036 staff
14734 scientists
7446 doctoral students
7476 visiting scientists

Helmholtz Association

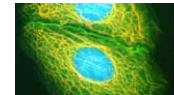
We contribute scientifically to address the grand challenges which face society, science and industry by performing research in strategic programs in



Energy



Earth & Environment



Health



Key Technologies

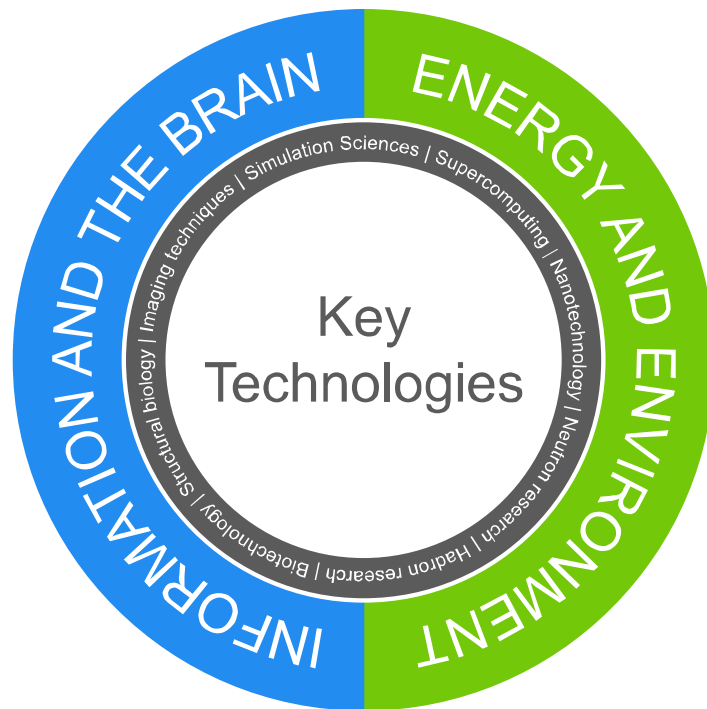


Matter



Aeronautics, Space and Mobility

Forschungszentrum Jülich – Facts and Figures



Research on **next generation**
 enabling key technologies

Staff (2015): ~ **5700** employees

Budget (2015): **558 Mio. €**

- Institutional funding: **320 Mio. €**
- Third party funding: **238 Mio. €**

Project administration: **1.6 Billion €**

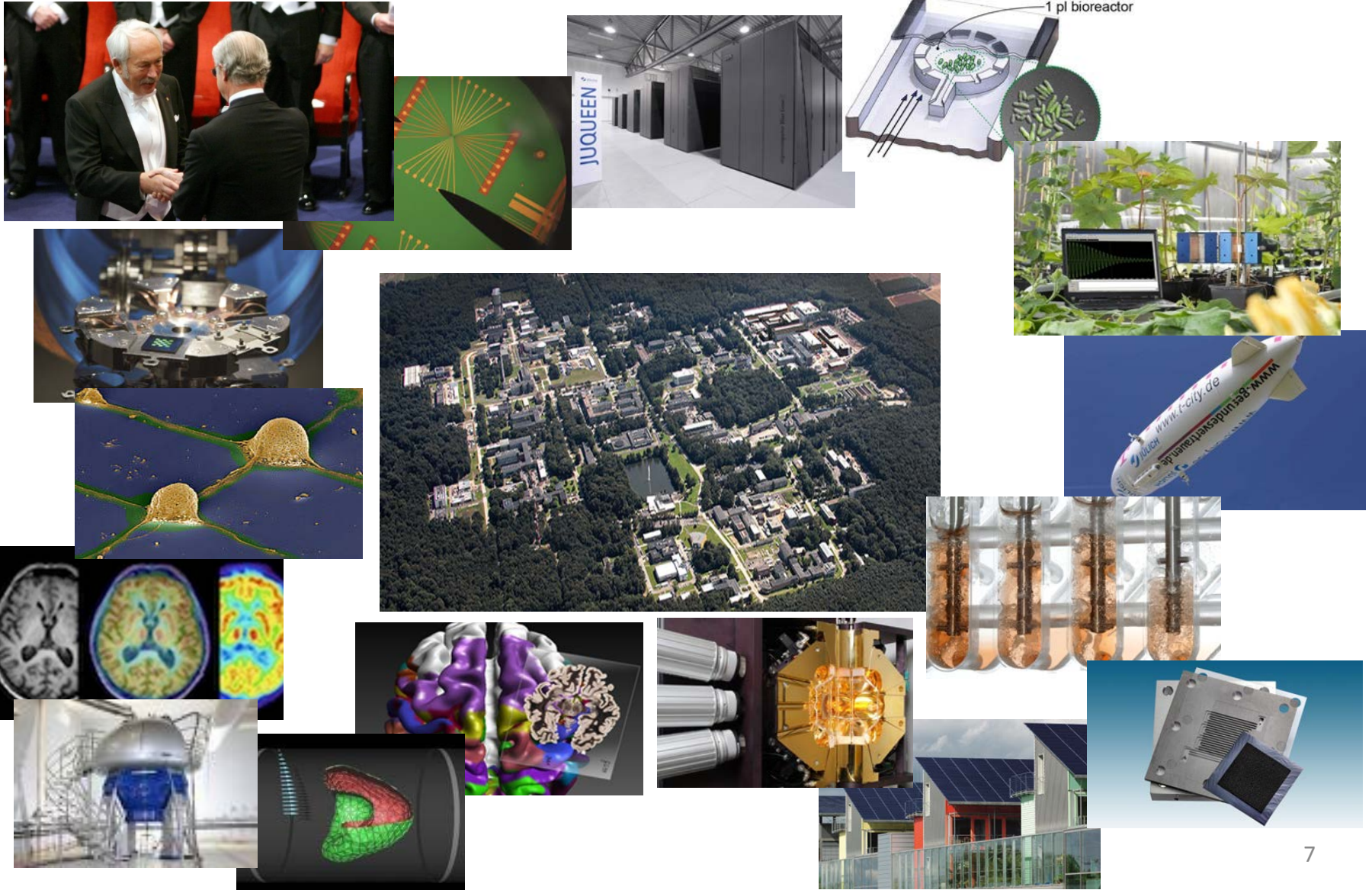
Education:

- ~ 900 Phd students
- ~ 350 Trainees

JARA collaboration

- 6 JARA Sections, 4 JARA Institutes
- ~ 200 PIs involved

Forschungszentrum Jülich – Impressions



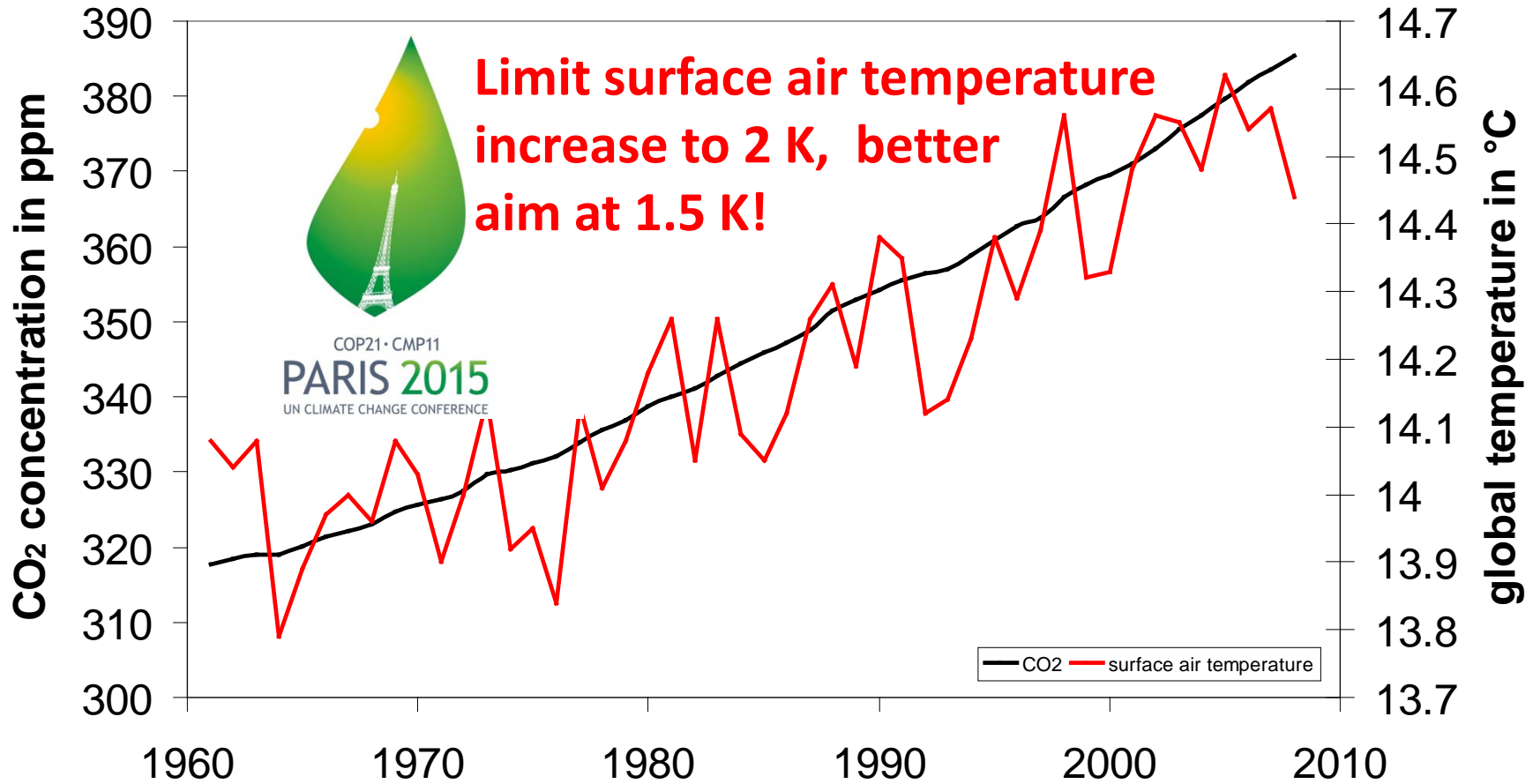
Content

- Where do I work?
- **The German “Energiewende”:
objectives and challenges**
- Stabilizing the grid by design:
Managing storage and demand
side
- “Intelligent” grid management:
Demonstrator and research infrastructure
- Control methods and tools:
Hierarchical and distributed architectures
- Take away messages



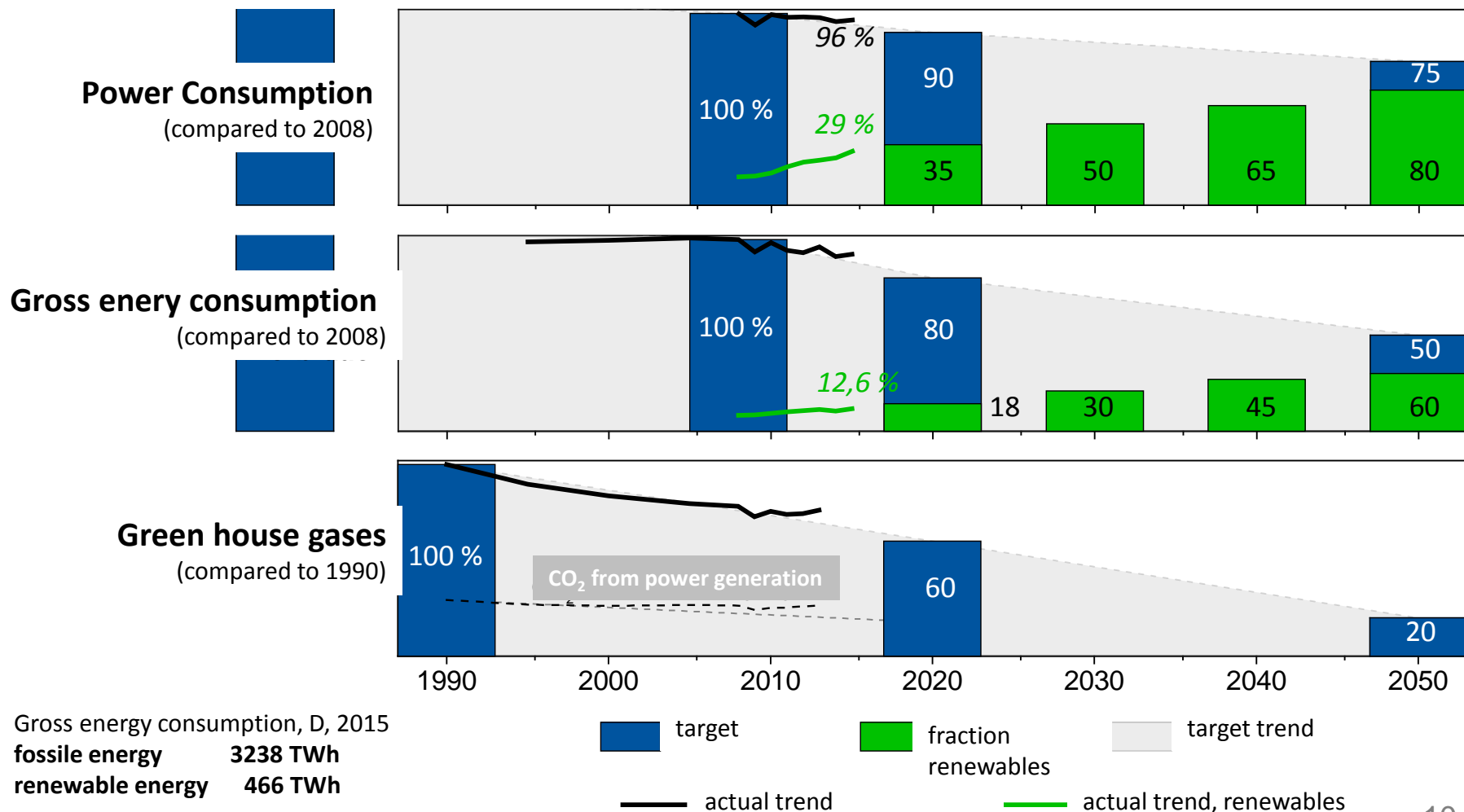
Source: Siemens Energie-Puzzle

We Face Climate Change!



Targets for the German Energy System 2050

... defined by the German Federal Government



The Current Energy Mix in Germany

Nuclear energy (~14%)

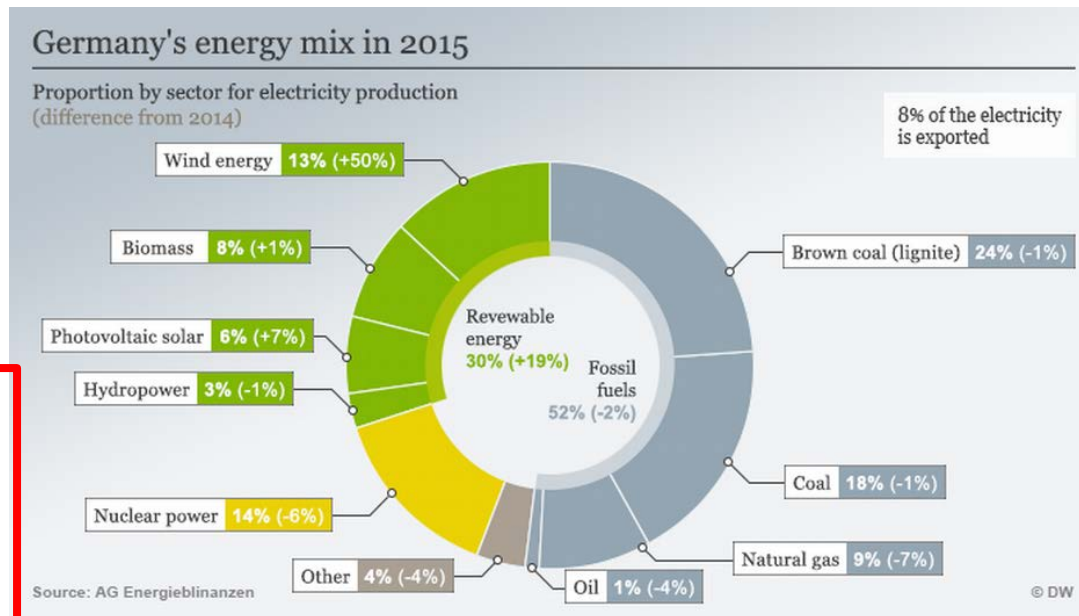
- strong anti-nuclear movement in Germany since 1970s
- Government decision after Fukushima event in 2012: shutdown of all nuclear power plants by 2022

Clean fossil-fired power plants (~52%)

- societal opposition toward carbon capture and storage
- shutdown of all coal-fired power plants by 2040 under discussion

Renewable energies (~30%)

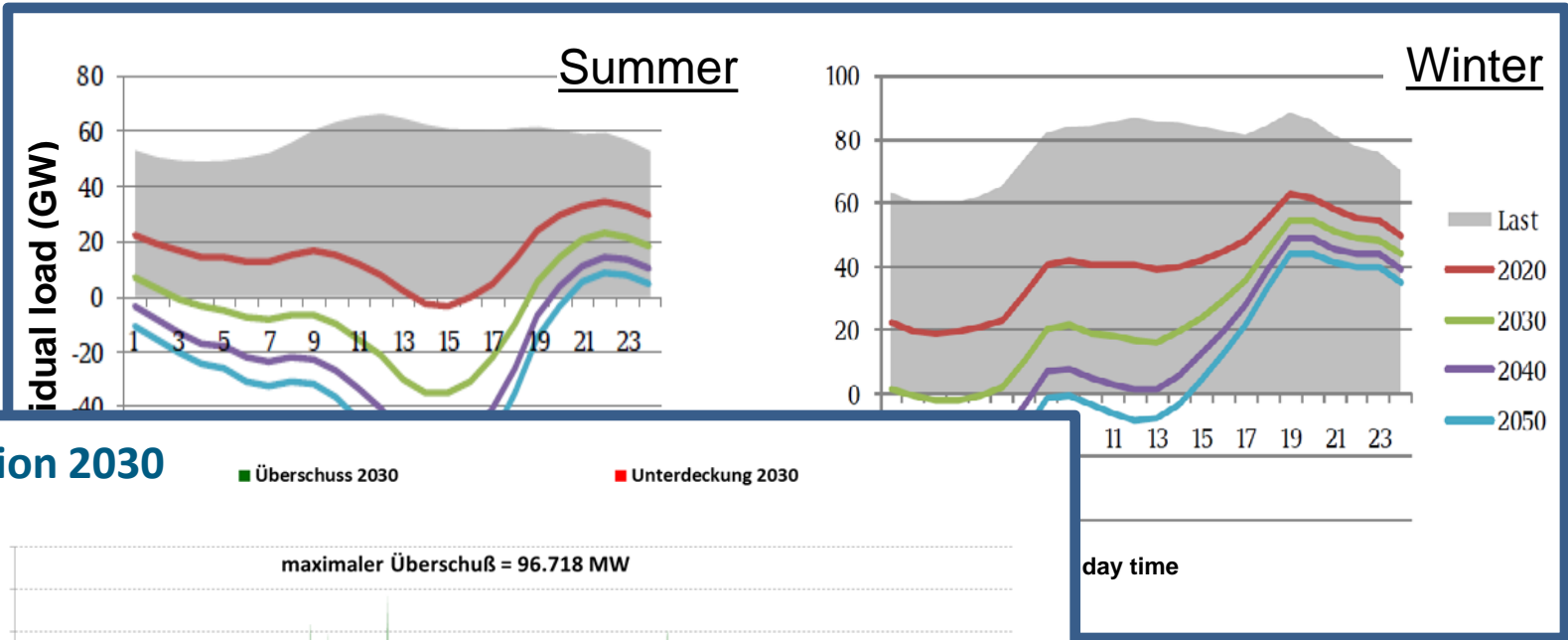
- on-shore and off-shore wind power
- biomass-to-gas
- solar (heat and) power
- hydropower



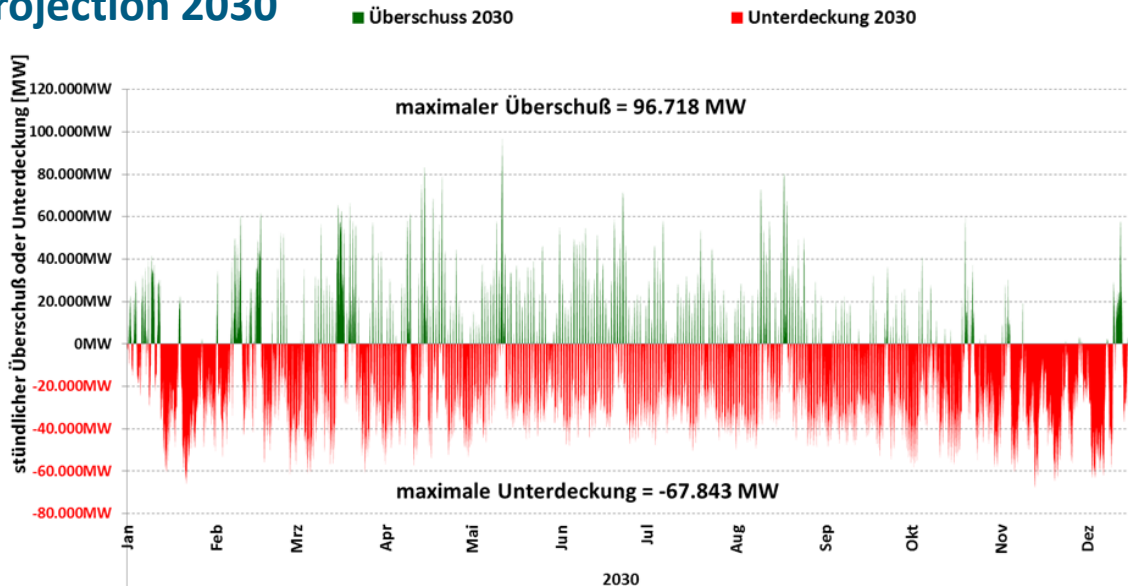
Energy mix (electricity generation) in Germany (2015)

Source: AG Energiebilanzen

The Challenge: Volatile and Decentralized Generation



projection 2030



Datenquelle: EEX-Leipzig / Entsoe.net

Auflösung: Stundenwerte

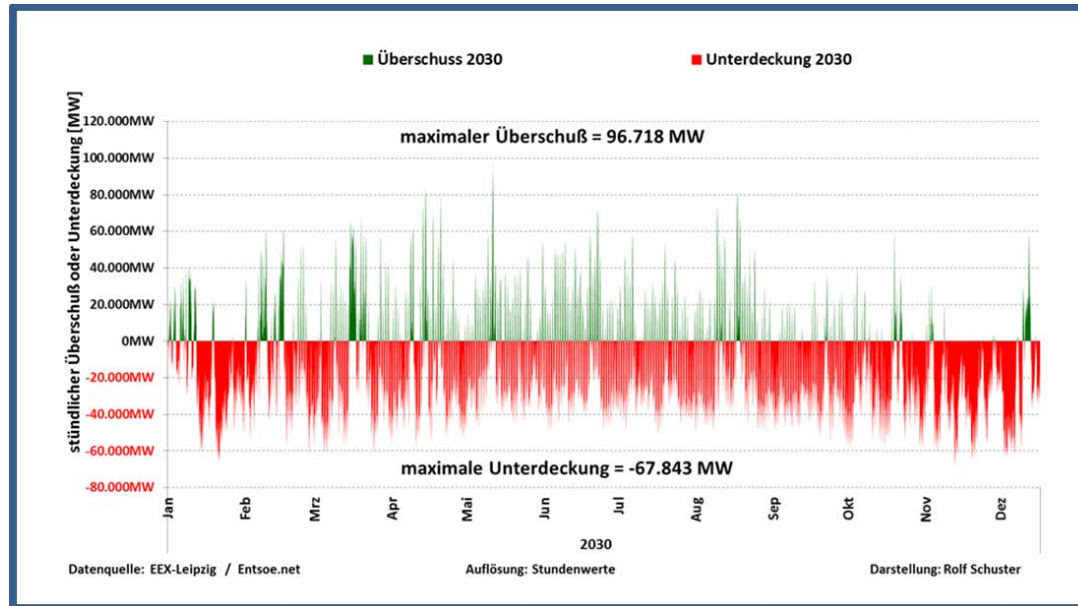
Darstellung: Rolf Schuster

day time

Electricity prices, D, 2015
 Spot market: 25 €/MWh
 Household: 295 €/MWh
 Industry: 149 €/MWh

<https://www.energy-charts.de/price.htm>

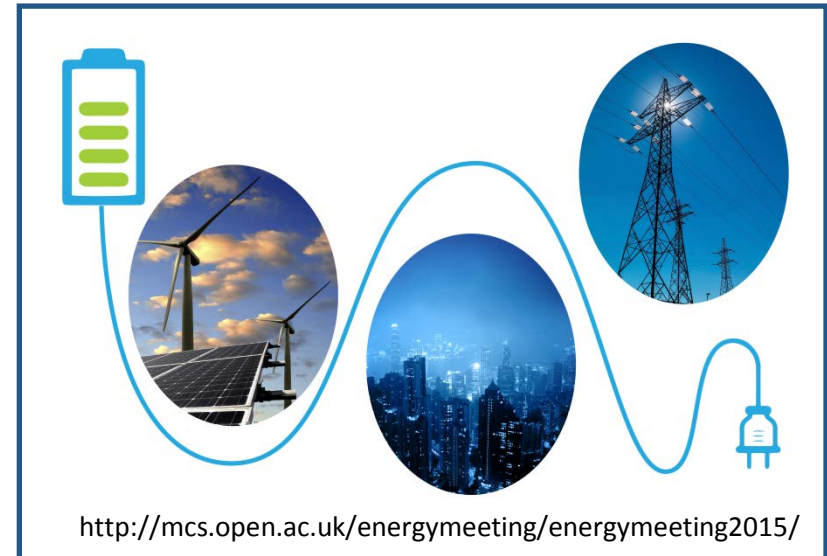
The Challenge: Volatile and Decentralized Generation



- new production and distribution technologies and services
- wide-area overhead power grid
- local “capacity reserves” on different scales: power plants vs. storage systems
- flexibilisation and use of overcapacity: supply-driven rather than demand-driven consumption (households, industrial production, ...)
- „intelligent“ (i.e., optimal) real-time planning, scheduling / trajectory planning and control of energy supply, storage, and demand
- “smart data“ and „smart models“ for „smart grid solutions“: data-driven and model-based grid management technologies

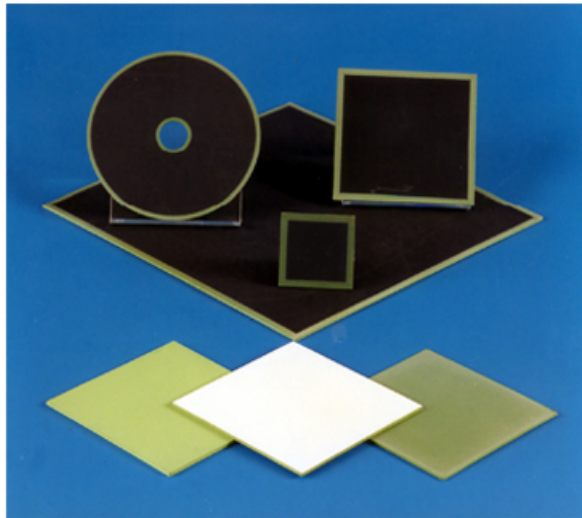
Content

- Where do I work?
- The German “Energiewende”: objectives and challenges
- **Stabilizing the grid by design: Managing storage and demand side**
- “Intelligent” grid management: Demonstrator and research infrastructure
- Control methods and tools: Hierarchical and distributed architectures
- Take away message

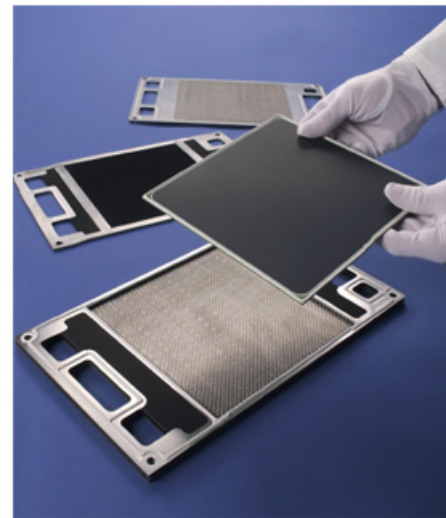


Key Technology: Reversible Solid-Oxide Fuel Cell

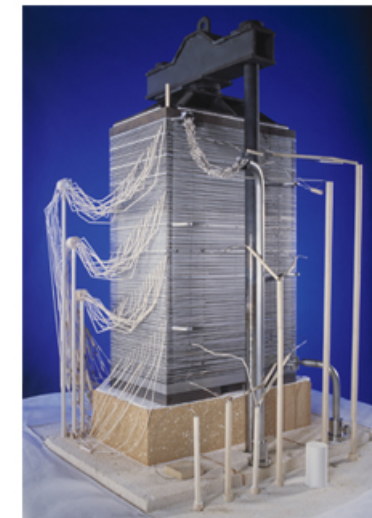
Research@FZJ: Eichel, Guillon, Singheiser, Stolten et al.



Materials design, synthesis,
and processing

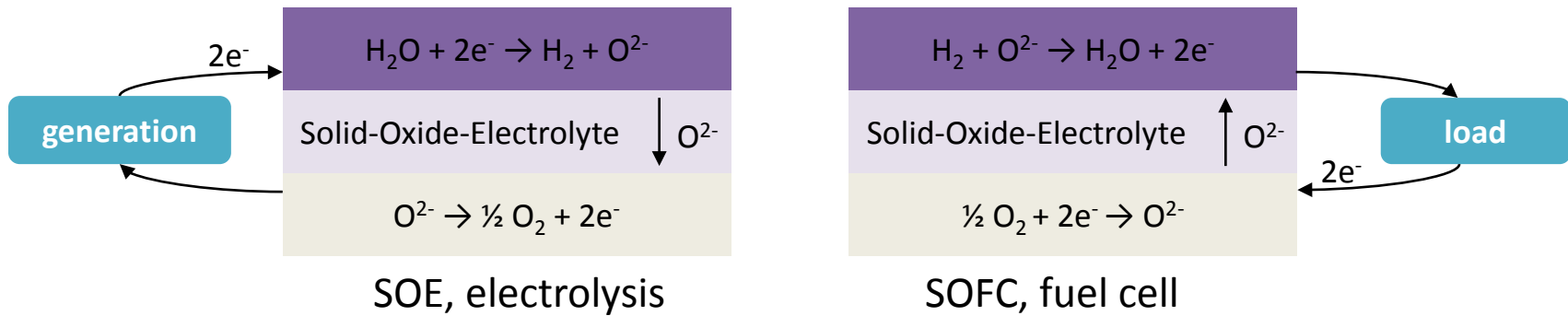


Cell and stack design

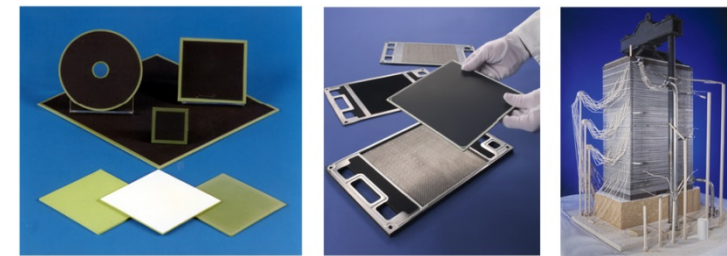
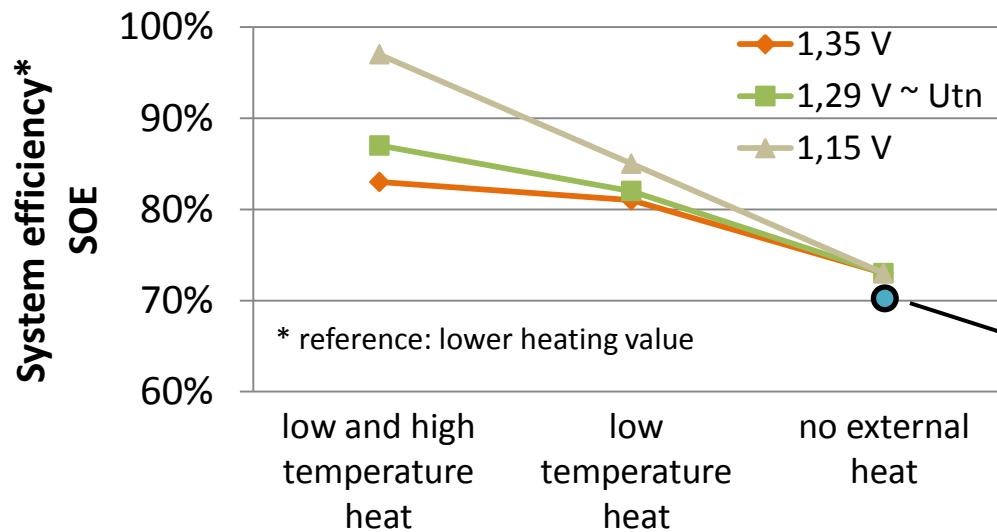


Systems design
and testing
(<100 kW)

Key Technology: Reversible Solid-Oxide Fuel Cell



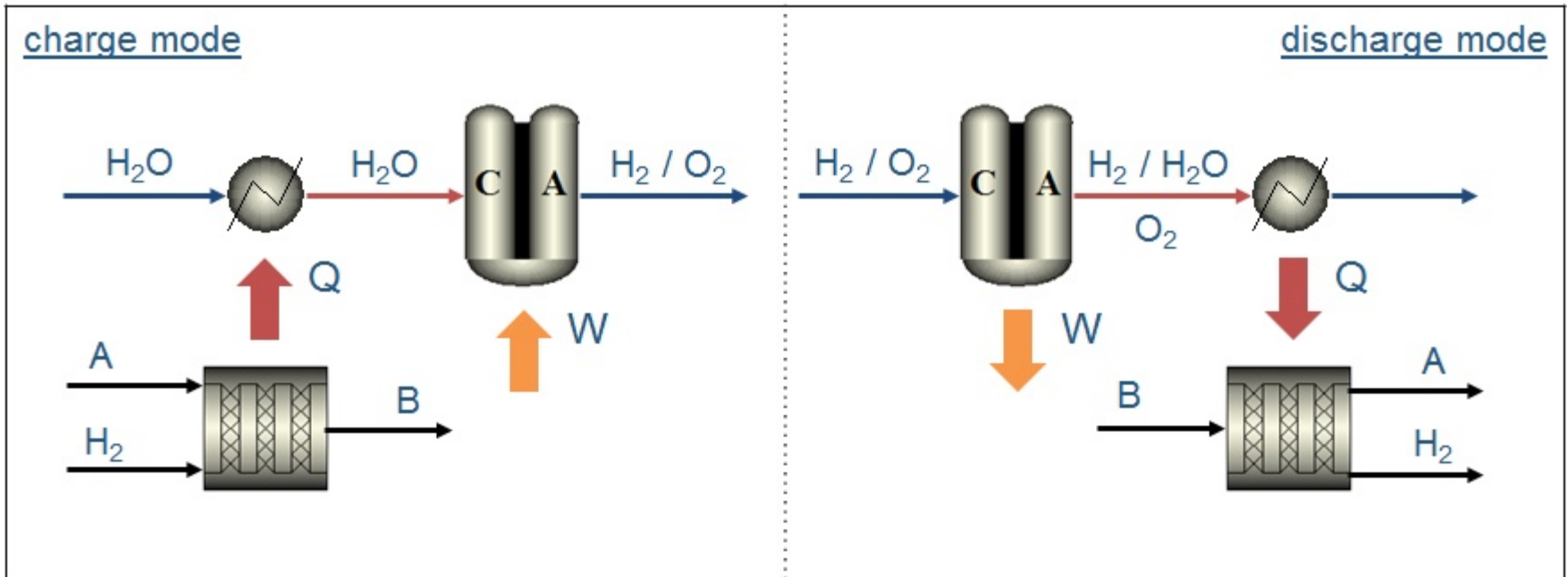
High temperature SO electrolysis



target for low temperature electrolysis

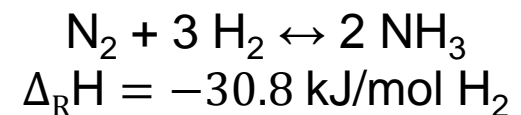
A Novel Concept for Power-to-Chemicals-to-Power

RSOFC integrated with a chemical reaction

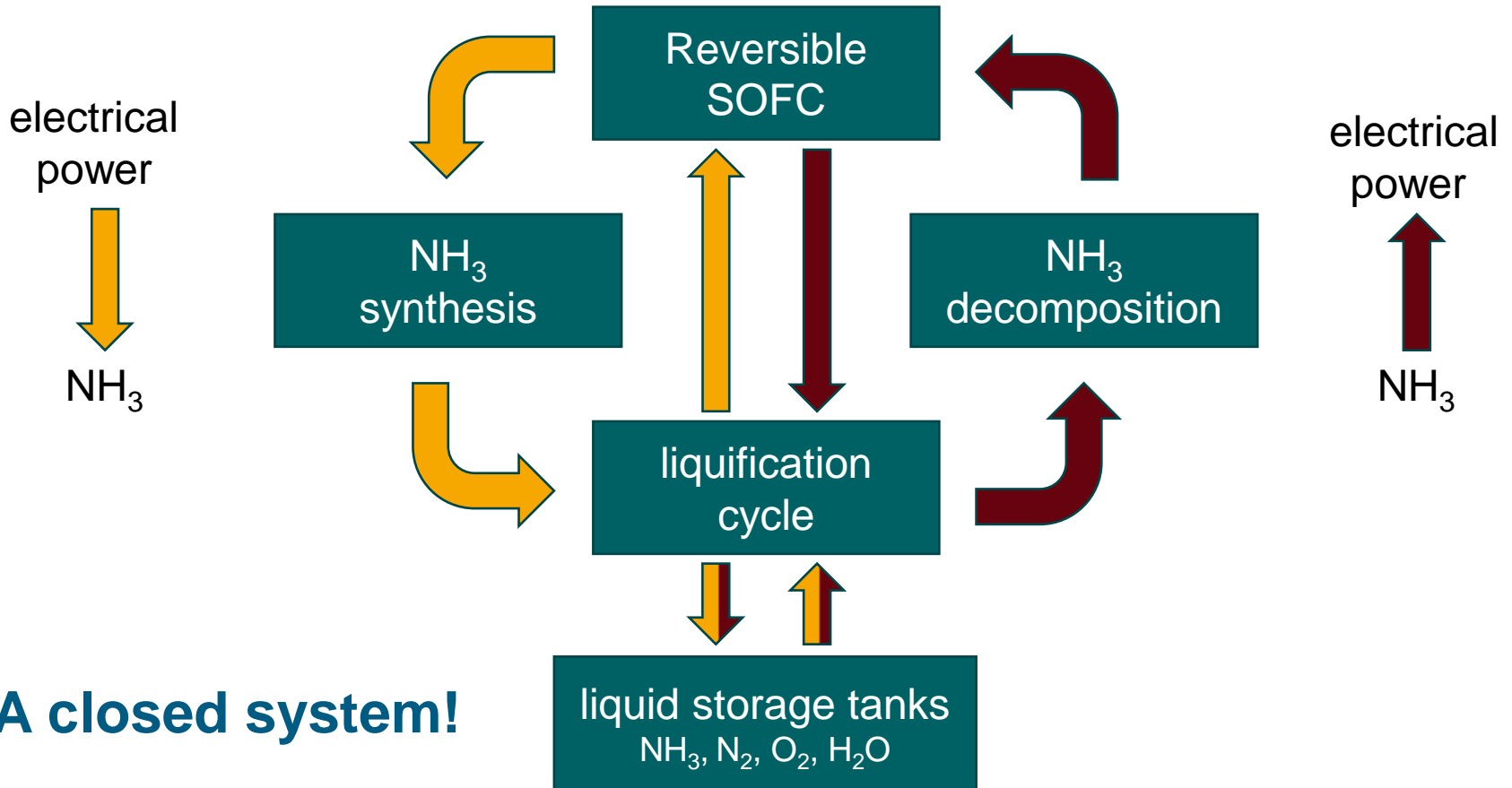


Ammonia – a promising candidate

- storage in large volume, easy to handle
- substrates are water and air (nitrogen)
- no side-products, simple separations



Ammonia-Based Energy Storage System



Ammonia-Based Energy Storage System

Performance for nominal steady-state operation

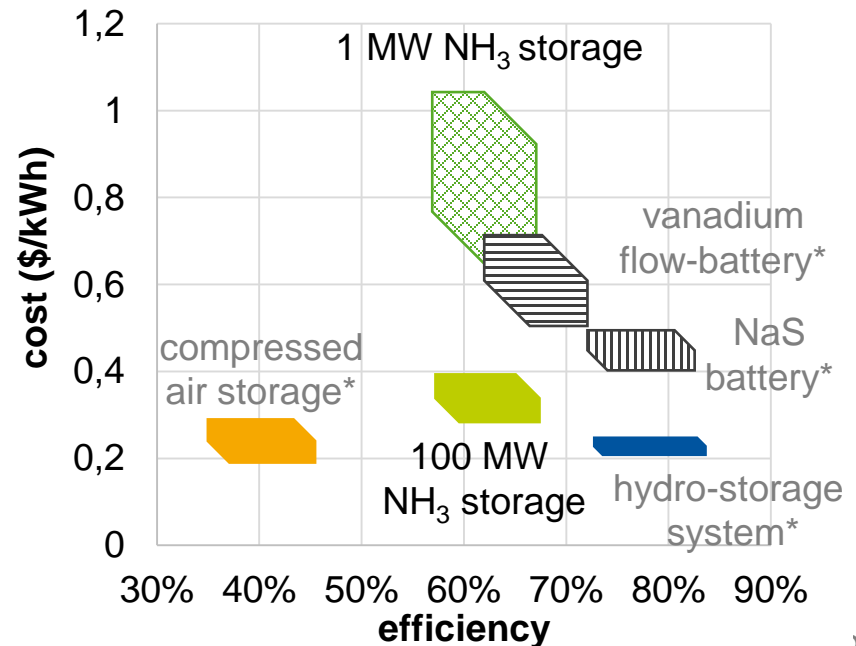
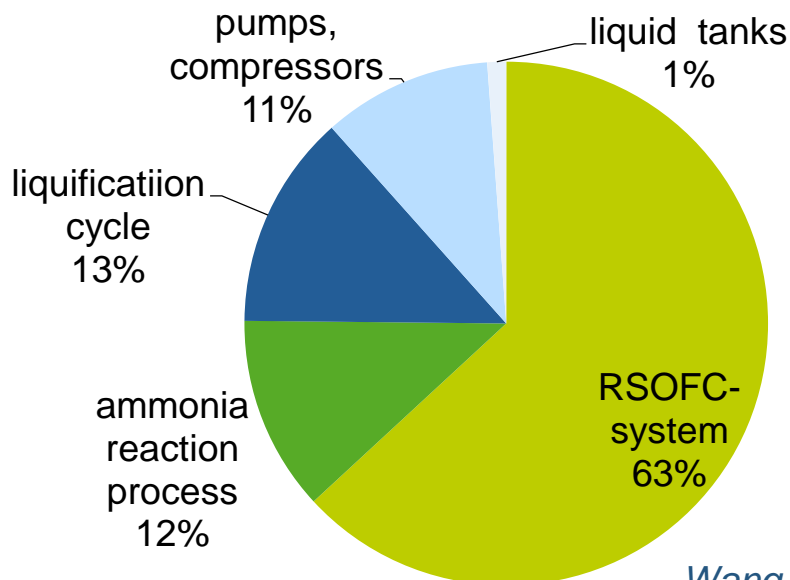
Scenario

- 100 MW capacity
- 10 h/d charge/discharge time, 4 h/d storage time

Optimization model

- 29.796 vars, 7 decisions

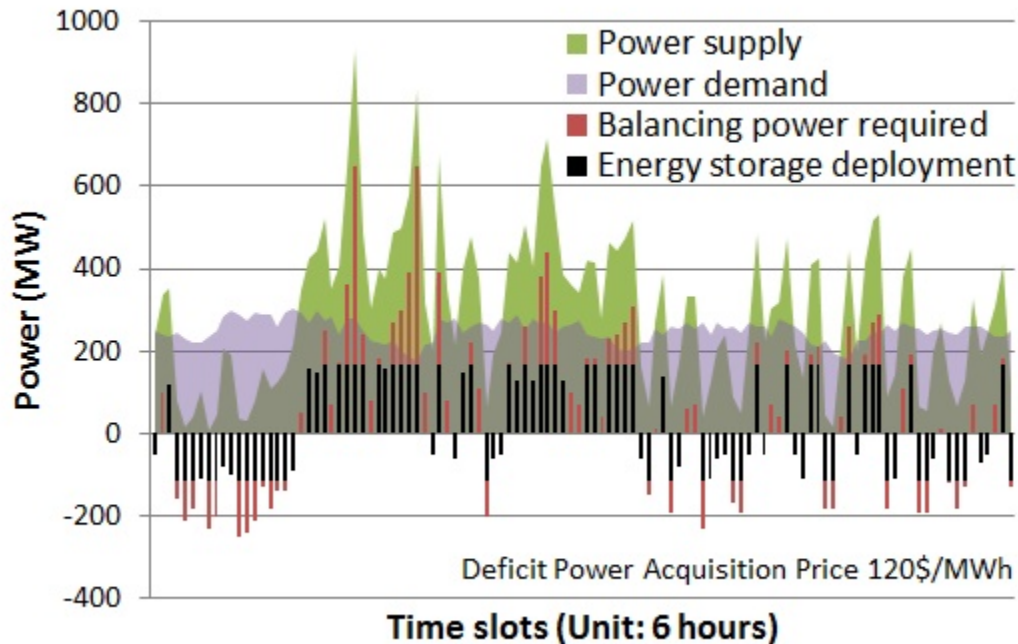
	max. efficiency	min. cost
efficiency (%)	72	64
storage cost (\$/kWh)	0,35	0,24



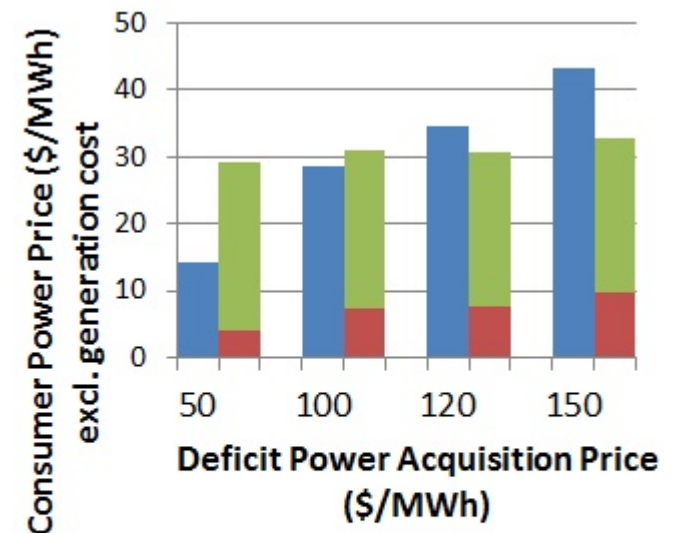
Wang, Mitsos, M. (sub.)

Ammonia-Based Energy Storage System

Performance under transient operation



- Total round-trip efficiency 62% for typical scenario, February, Southern Germany



Comparison of consumer power prices:

- 100% external power acquisition
- using ammonia-based energy storage system

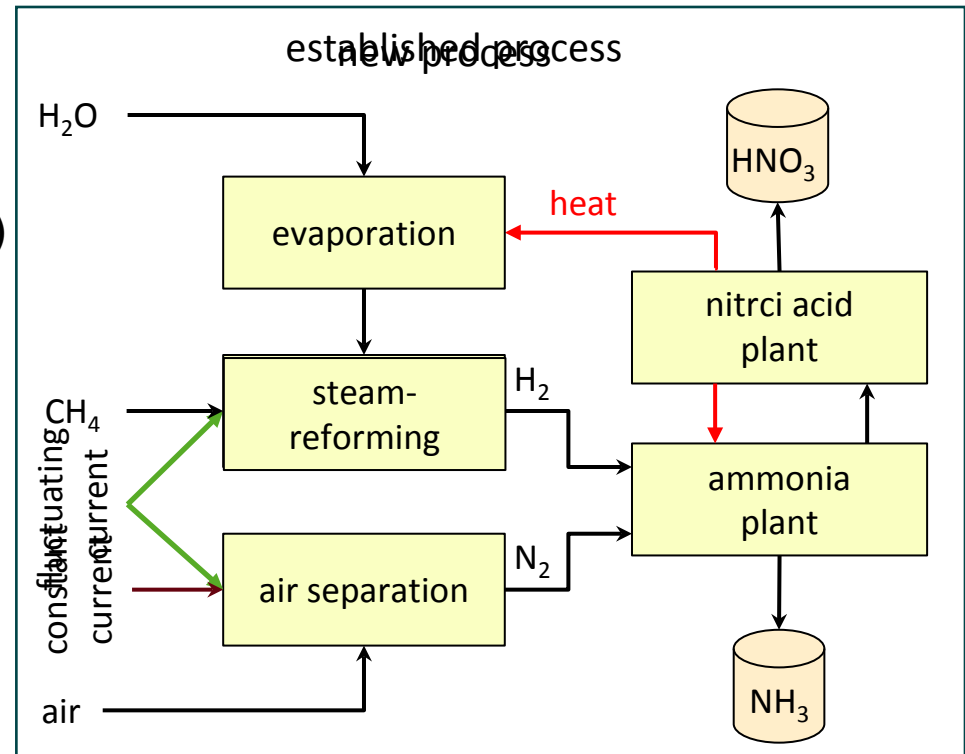
Demand-Side Management – NH₃/HNO₃ Complex

Established ammonia process

- steady-state operation
- H₂ from steam reforming
- high emissions (1,7 t CO₂/t NH₃)

Novel NH₃/HNO₃ complex

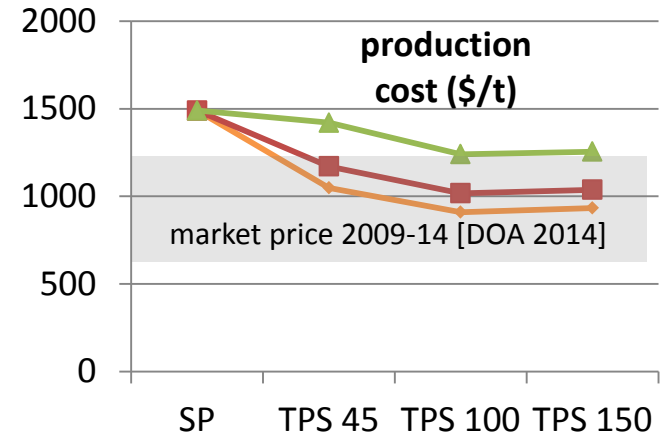
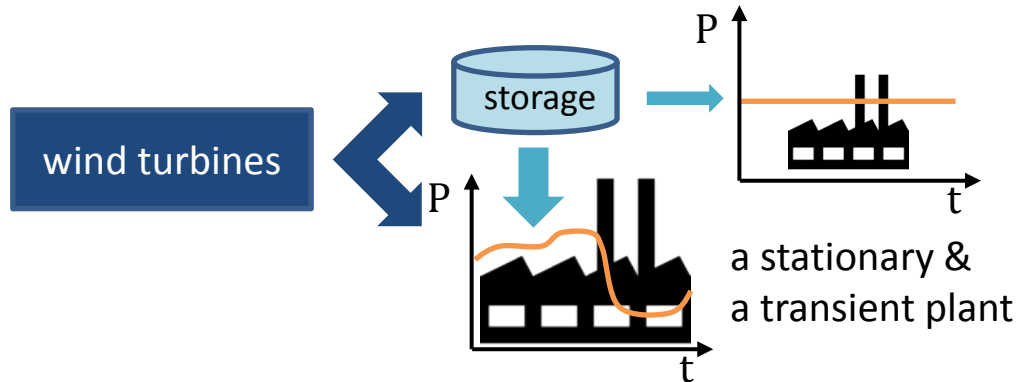
- transient operation
- H₂ from electrolysis
- zero CO₂ emission
- heat integration with nitric acid
- highly energy-efficient (7.0 MWh_{el} / t NH₃)



Process design, control and optimization for demand-side management

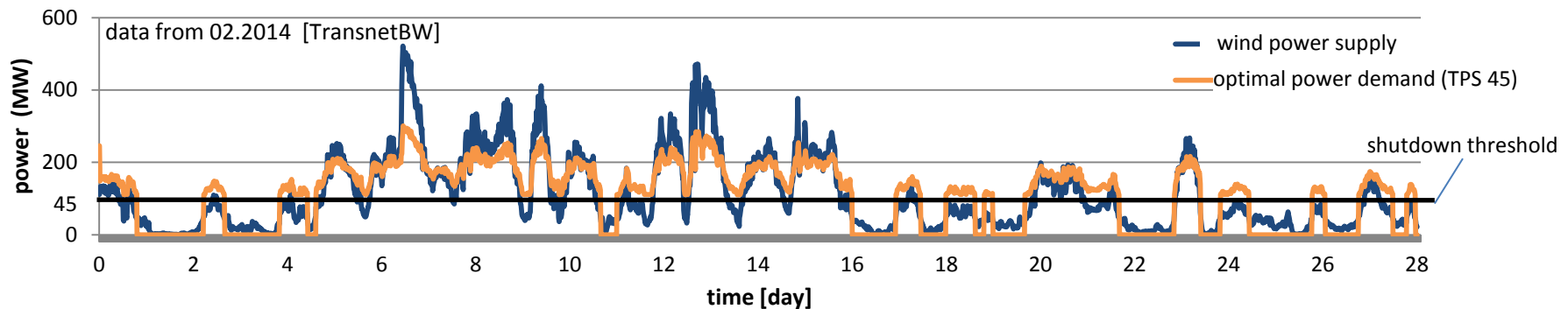
- economically optimal design for nominal case (stationary operation)
- base layer control (levels, temperatures, product quality)
- dynamic real-time optimization for transient load

Demand-side Management: Results



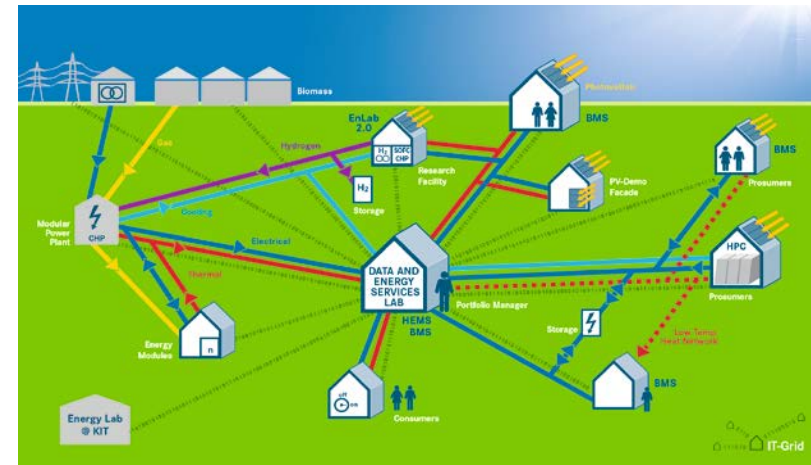
- Lifetime of a transient production system, 20 years
- 10 years
- 5 years

- real power generation scenario
- cost-optimal design
- design variables
 - capacities (storage, both plants)
 - reference load trajectories



Content

- Where do I work?
- The German “Energiewende”: objectives and challenges
- Stabilizing the grid by design: Managing storage and demand side
- **“Intelligent” grid management: Demonstrator and research infrastructure**
- Control methods and tools: Hierarchical and distributed architectures
- Take away messages

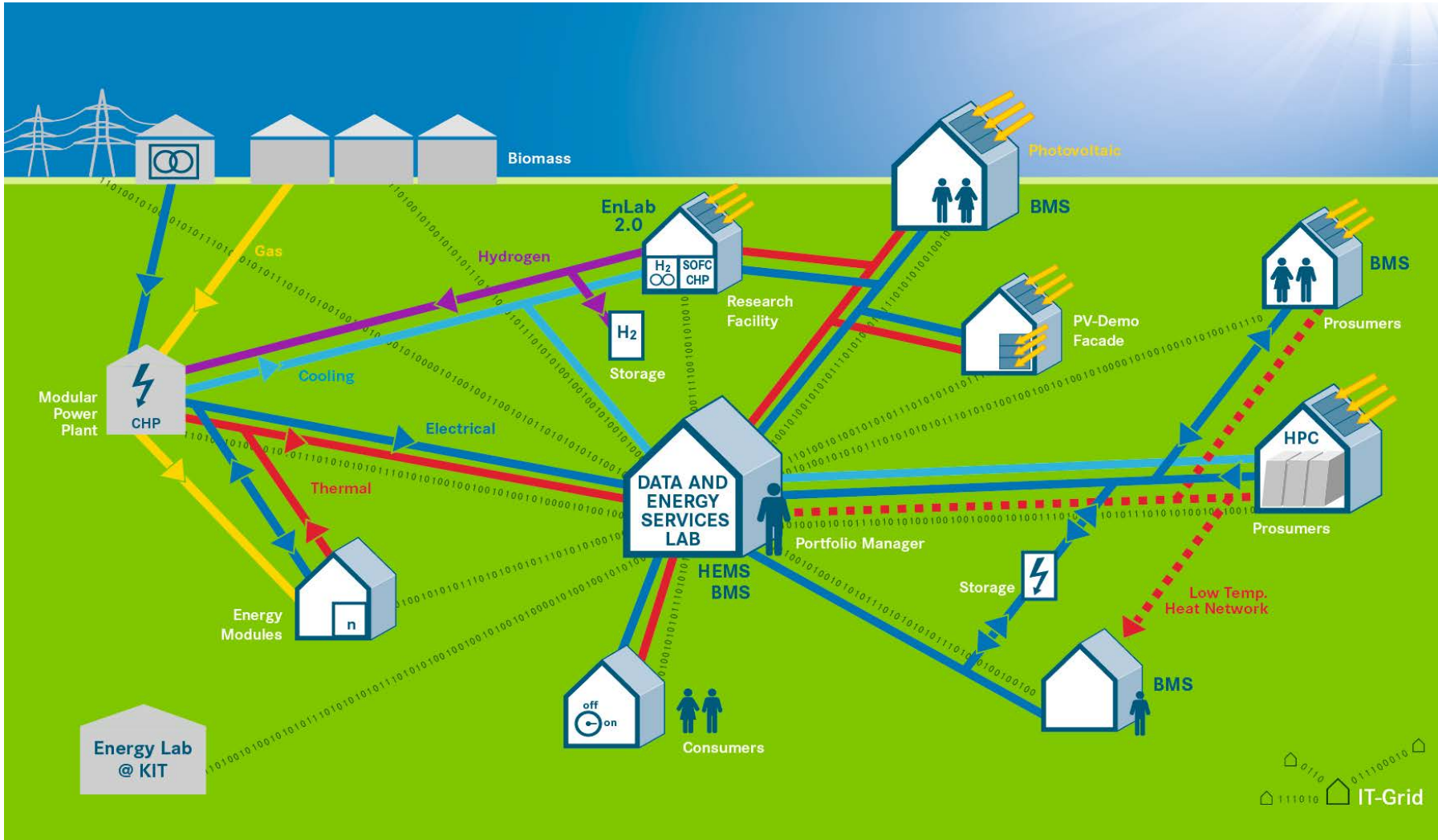


Research for Energy – Energy for Research



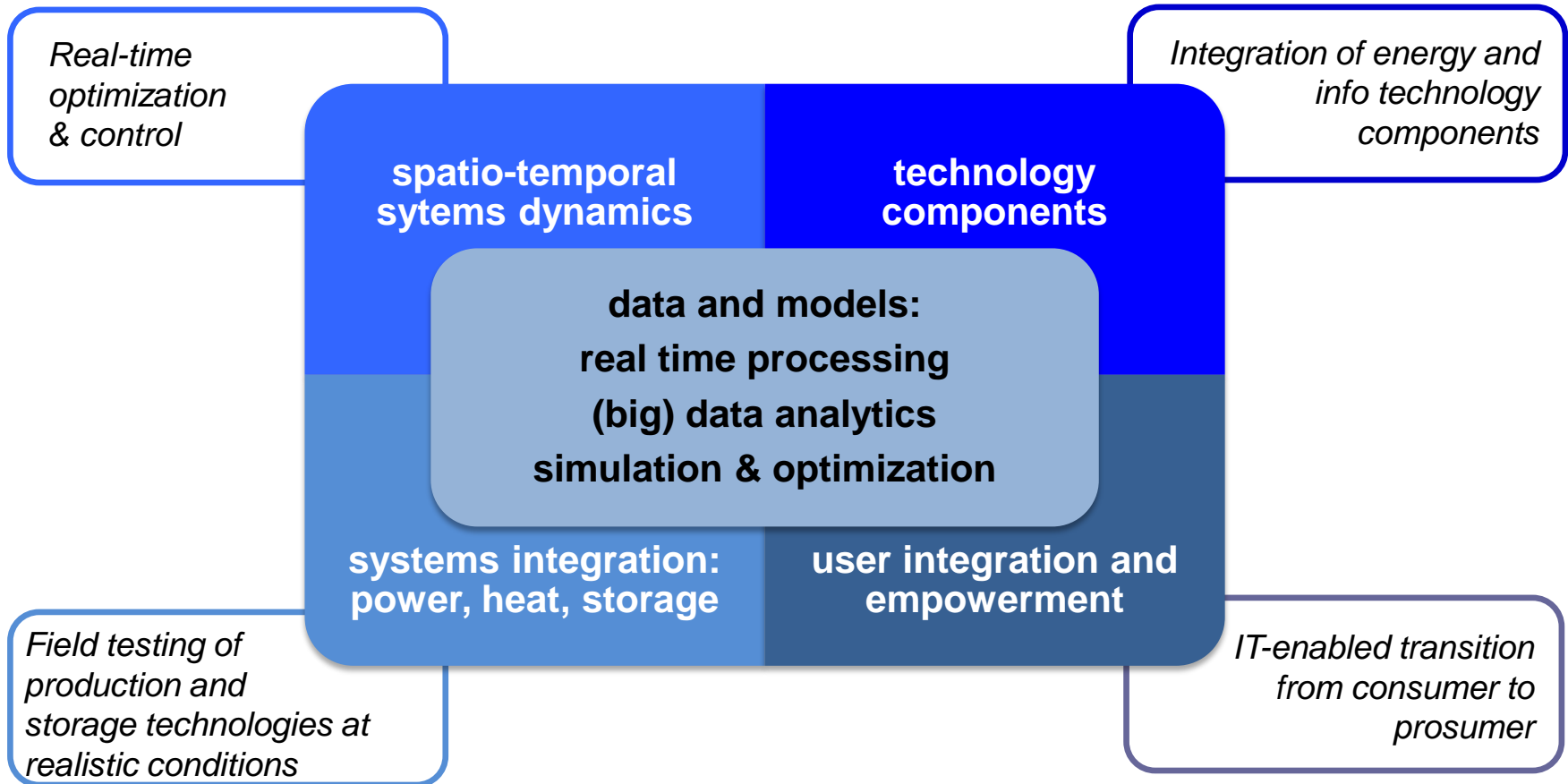
**Develop the FZJ Campus into a node
of the national energy grid dominated
by renewables:
A large-scale demonstrator and
research infrastructure**

Living Lab Energy Campus – a Node in a Smart Grid



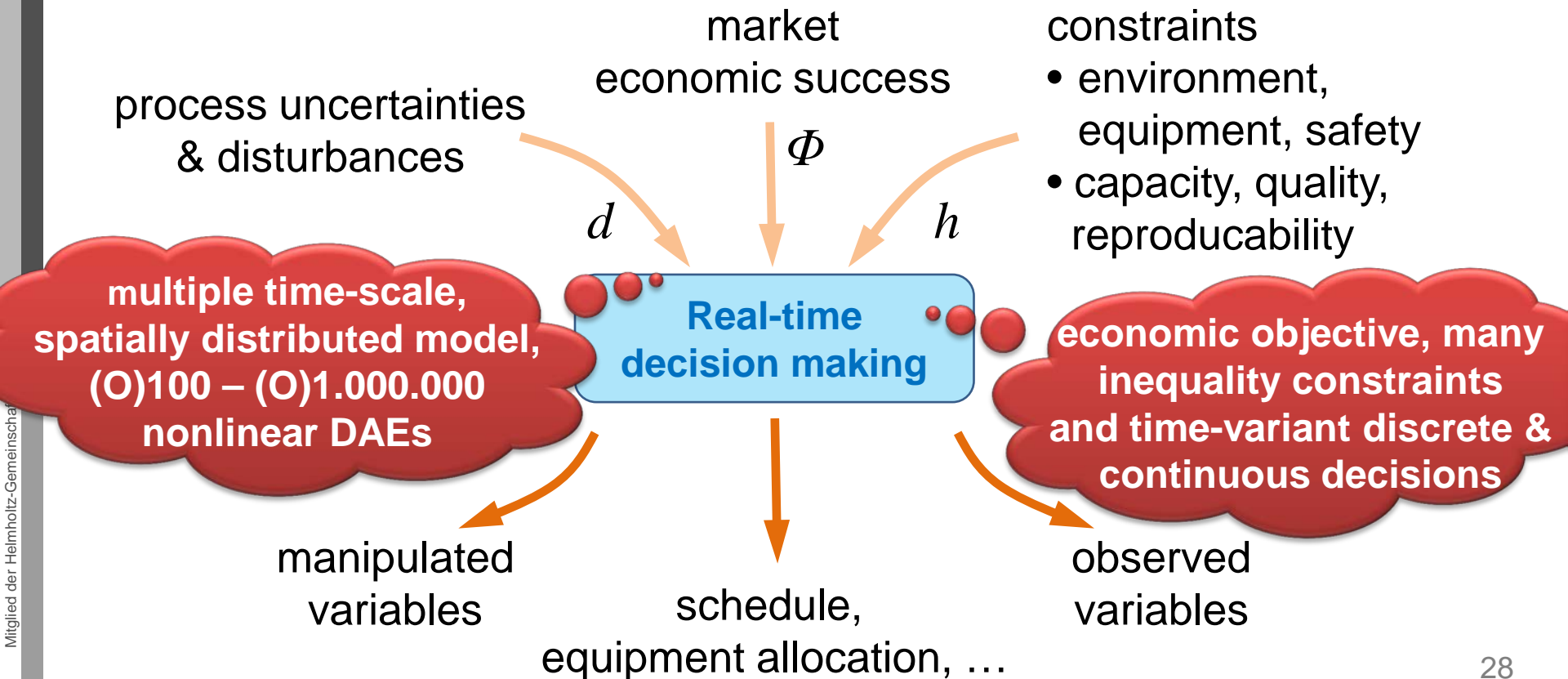
Living Lab Energy Campus: Overview

Integrated research infrastructure for decentralised urban energy systems



The Objective of Operations and Control

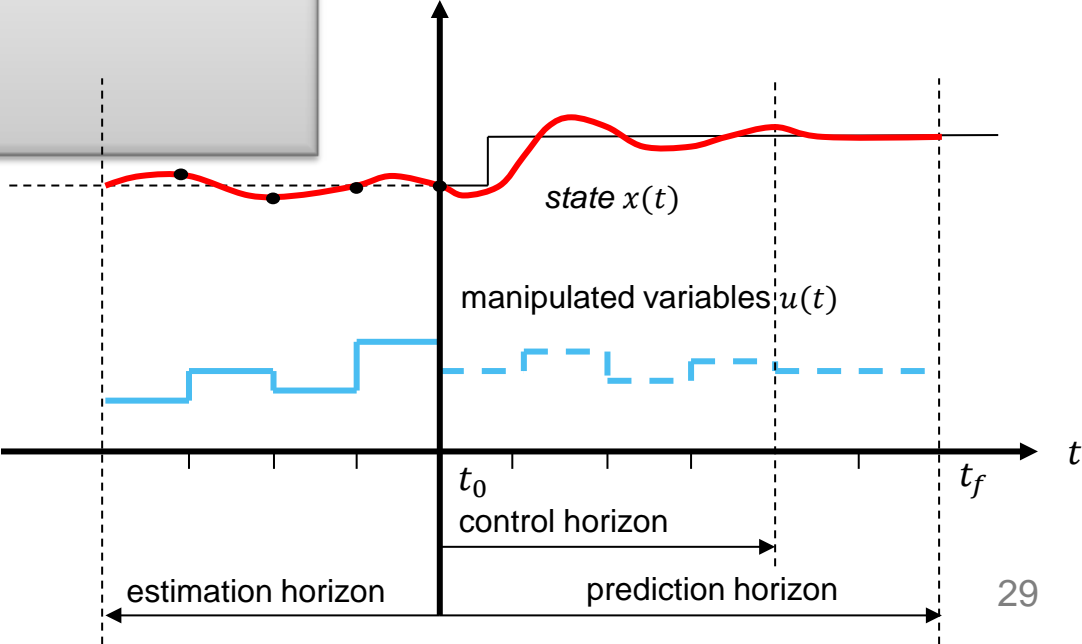
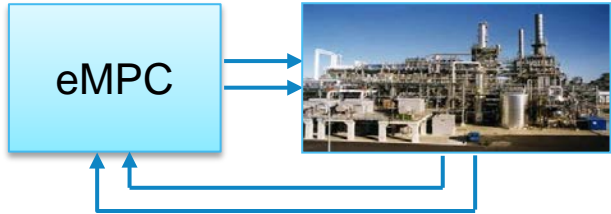
Economically optimal operation of transient processes anytime !



Economic Model-Predictive Control – The Concept

Continuous-time state feedback, moving horizon, no discrete decisions

$$\begin{aligned}
 & \min_{x,u} \Phi(x,u) \quad s.t. \\
 & \Phi(x,u) = \|x(t_f)\|_P^2 + \int_{t_0}^{t_f} \|x(t)\|_Q^2 + \|u(t)\|_R^2 dt, \\
 & \dot{x}(t) = f[x(t), u(t)], \quad t \in [t_0, t_f], \\
 & x(t_0) = \hat{x}_0, \\
 & x(t) \in X, \quad t \in [t_0, t_f], \\
 & u(t) \in U, \quad t \in [t_0, t_f], \\
 & x(t_f) \in X_f
 \end{aligned}$$



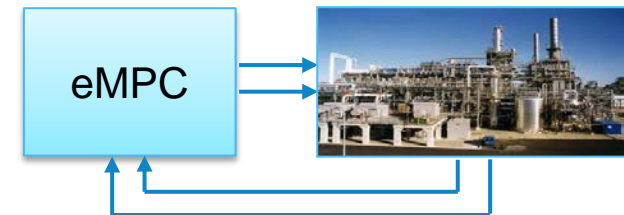
Discretization of manipulated variables:

$$u(t) = \sum_{l=1}^L c_l \psi_l(t)$$

Economic Model-Predictive Control – The Concept

Continuous-time state feedback, moving horizon, no discrete decisions

$$\begin{aligned} & \min_{x,u} \Phi(x,u) \quad s.t. \\ & \Phi(x,u) = \|x(t_f)\|_P^2 + \int_{t_0}^{t_f} \|x(t)\|_Q^2 + \|u(t)\|_R^2 dt, \\ & \dot{x}(t) = f[x(t), u(t)], \quad t \in [t_0, t_f], \\ & x(t_0) = \hat{x}_0, \\ & x(t) \in X, \quad t \in [t_0, t_f], \\ & u(t) \in U, \quad t \in [t_0, t_f], \\ & x(t_f) \in X_f \end{aligned}$$



Discretization of manipulated variables:

$$u(t) = \sum_{l=1}^L c_l \psi_l(t)$$

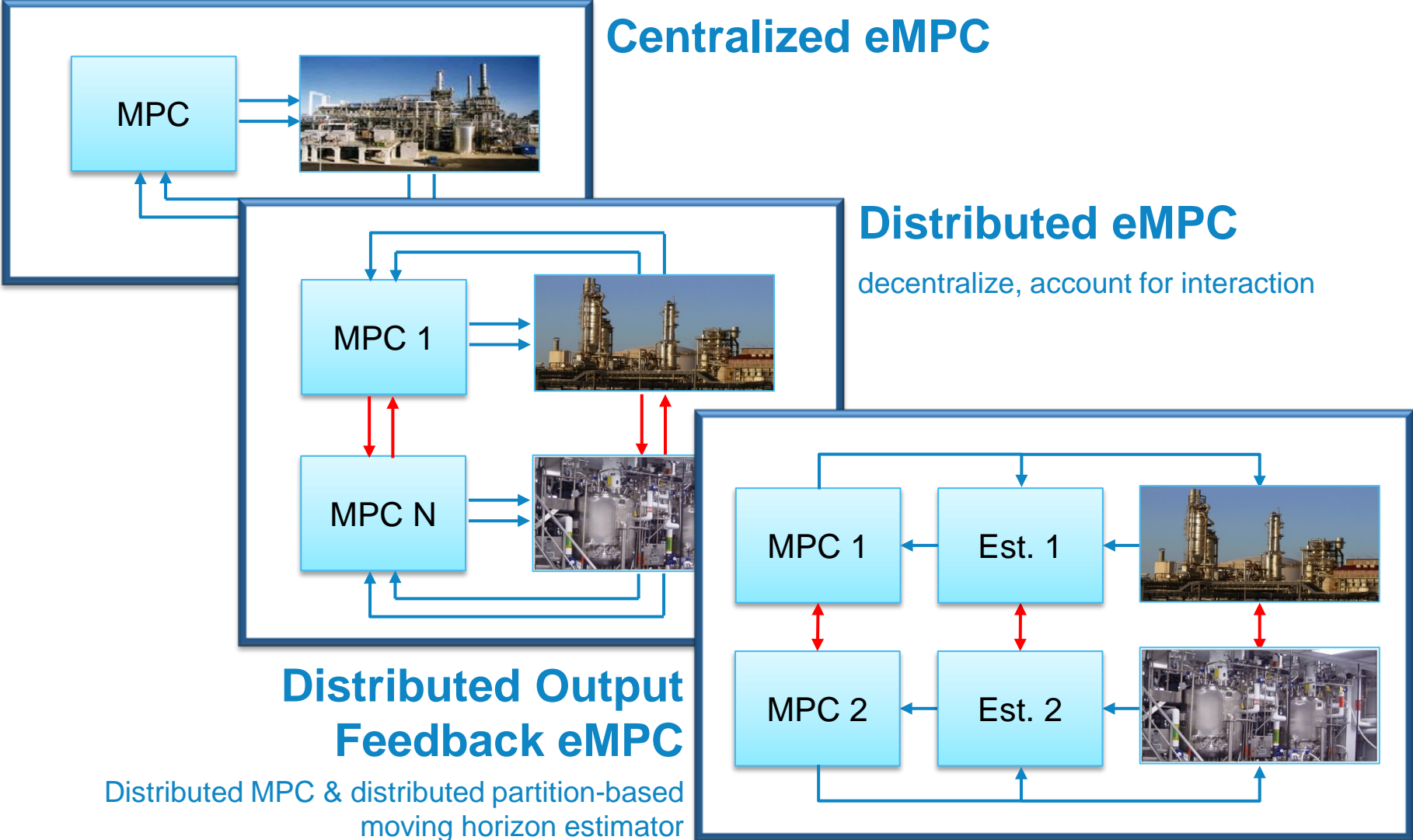
Dynamic Real-Time Optimization (DRTO):

Gouvea and Odloak (1998), Backx, Bosgra and M. (2000), Helbig, Abel and M. (2000), Kadam et al. (2003), Engell (2007), Kadam, Würth and M. (2007), Würth, Hannemann and M. (2009, 2011), ...

Economic Nonlinear Model-Predictive Control

(eMPC): Adetola and Guay (2010), Amrit et al. (2011), Diehl et al. (2011), Huang et al. (2012), Grüne (2013), Ellis et al. (2014) ...

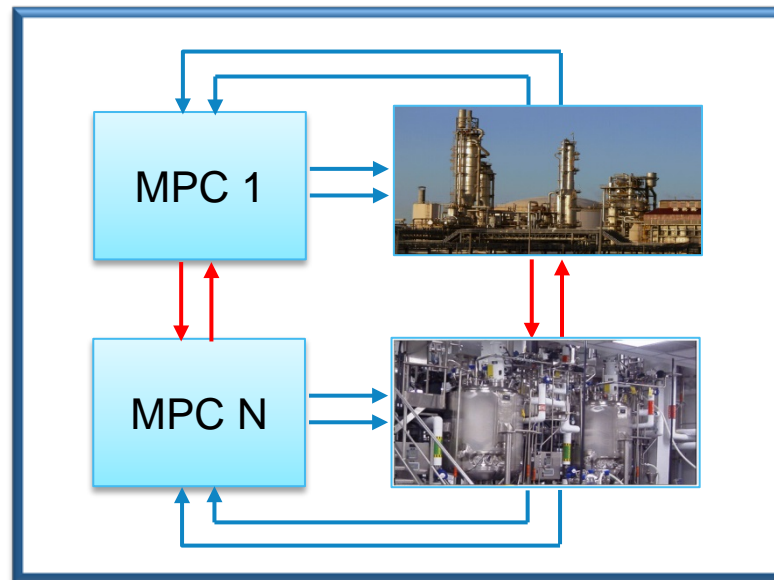
Decentralization and Distribution



Distributed Model-Predictive Control – DMPC

Review on architectures: Scattolini, 2009, Farina et al., 2010

Classic approach – Dual decomposition: Lasdon, 1970, Negenborn et al., 2008, ...



Distributed MPC

decentralize, account for interaction

Challenges

- broad applicability
- optimality
- convergence
- stability
- efficiency

Recent approach – Sensitivity-driven S-DMPC: Mesarovic et.al, 1970, Scheu & M., 2011

Benchmarking of S-DMPC: Alavarado et al., 2011, Maestre et al. 2015

Sensitivity-based Decomposition – DMPC

Continuous-time OCP

$$\begin{aligned} \min_{x,u} & \frac{1}{2} \int_{t_0}^{t_f} (\|x(t)\|_Q^2 + \|u(t)\|_R^2) dt, \\ \text{s.t. } & \dot{x}(t) = Ax(t) + Bu(t), \quad t \in (t_0, t_f], \\ & x(t_0) = x_0, \\ & x \in X, \quad u \in U \end{aligned}$$

Transcription



QP

$$\begin{aligned} \min_z & = \sum_{i=1}^N \Phi_i(z) = \sum_{i=1}^N \frac{1}{2} z' H_i z + f_i' z \\ \text{s.t. } & 0 \leq c_i(z) = A_i z + b_i, \forall i \end{aligned}$$

Parallel iterative solution using decomposed subproblems



$$\begin{aligned} \min_{z_i} & \Phi_i^*(z) \\ \Phi_i^*(z) & = \Phi_i(z) + \left[\sum_{j=1, j \neq i}^N \frac{d\Phi_j}{dz_i} \Big|_{z^{[k]}} - \lambda_j^{[k]T} \frac{dc_j}{dz_i} \Big|_{z^{[k]}} \right] (z_i - z_i^{[k]}) \\ \text{s.t. } & c_i(z) \geq 0, \end{aligned}$$

S-DMPC

- optimality ✓
- convergence ✓
- stability 
- efficiency ✓

Theory for **linear** systems, benchmarking with **(simple)** nonlinear plants:
Scheu & M., 2011; Alavarado et al., 2011, Maestre et al. 2015

Distributed State Estimation

Classic approaches to state estimation

Centralized eMPC

- **Kalman Filter** (Kalman, 1960, Hassan et al., 1978, Venkat et al., 2006, Roshany-Yamchi et al. 2013)
- **Luenberger Observer** (Luenberger, 1964, Venkat et al. 2005, Farina & Scattolini, 2011, Giselsson, 2013)

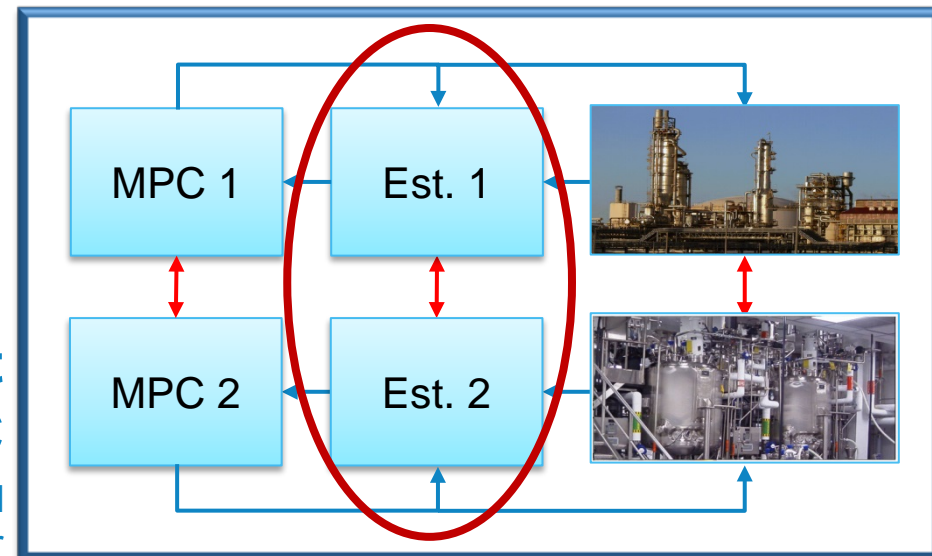
More recent approach

- **Moving horizon estimation** (Grizzle & Moraal, 1990, Michalska & Mayne, 1992)
- **Partition-based estimation** (Farina et al., 2011, Schneider et al. 2013, 2014, 2015, 2016)

iterative & inherently parallel algorithm with optimal performance of centralized estimator

Distributed Output Feedback eMPC

Distributed MPC & distributed partition-based moving horizon estimator



Sensitivity-based Decomposition – PMHE

Discrete-time moving horizon estimation problem

$$\min_{\Delta x(k^0), \{x\}, \{w\}, \{v\}} \frac{1}{2} \left(\|\Delta x(k^0)\|_{\bar{P}}^2 + \sum_{k=k^0}^{k'-1} \|w(k)\|_{\bar{Q}}^2 + \sum_{k=k^0}^{k'} \|v(k)\|_{\bar{R}}^2 \right)$$

$$\text{s.t. } x(k^0) = \bar{x}(k^0) + \Delta x(k^0),$$

$$x(k+1) = Ax(k) + w(k),$$

$$y(k) = Cx(k) + v(k)$$

QP

$$\min_z \sum_{i=1}^N \Phi_i(z),$$

$$\text{s.t. } c_i(z) \geq 0, \quad \forall i$$

Parallel iterative solution using decomposed subproblems



$$\min_{z_i} \Phi_i^*(z)$$

$$\Phi_i^*(z) = \Phi_i(z) + \left[\sum_{j=1, j \neq i}^N \frac{d\Phi_j}{dz_i} \Big|_{z^{[k]}} - \lambda_j^{[k]T} \frac{dc_j}{dz_i} \Big|_{z^{[k]}} \right] (z_i - z_i^{[k]})$$

$$\text{s.t. } c_i(z) \geq 0,$$

R-PMHE

- optimality 
- convergence 
- stability 
- efficiency 

Theory for **linear** systems, various formulations with different and theoretical properties, benchmarking with (non-)linear plants: Schneider et al. 2013, 2014, 2015, 2016

Distributed Output Feedback MPC

Established approaches

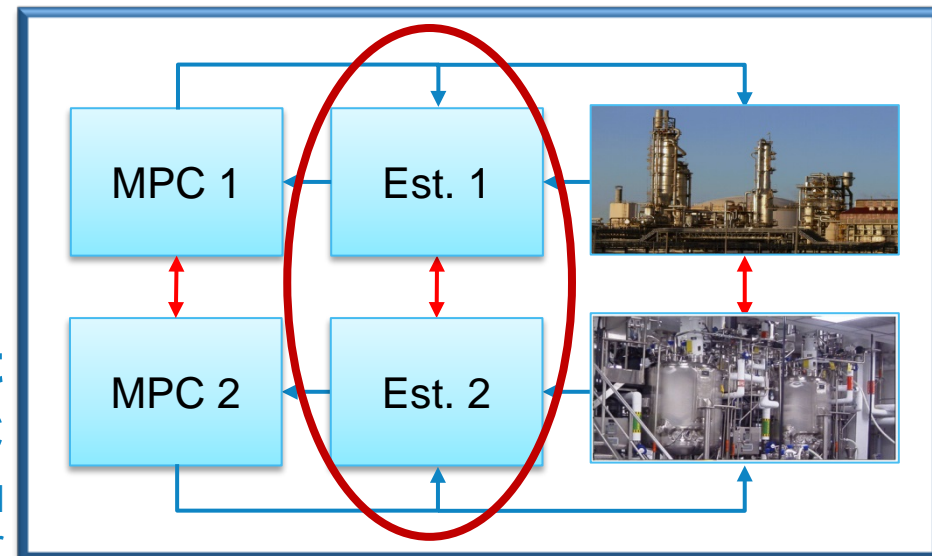
- **DMPC & centralized state estimation** (Zheng et al., 2009, Hu & El-Farra, 2013)
- **DMPC & distributed Luenberger observer** (Venkat et al., 2005, ...)
- **DMPC & distributed Kalman filter** (Venkat 2006 et al., ...)

Novel approach

- **S-DMPC & R-PMHE**
(Schneider, Scheu & M., 2014)
- **Alkylation plant case study:**
130 nonlinear DAEs, 25 states,
5 controls, 6 measurements, linear
S-DMPC & R-PMHE, 1 iteration

Distributed Output Feedback MPC

Distributed MPC & distributed partition-based moving horizon estimator



Distributed Output Feedback MPC

Established approaches

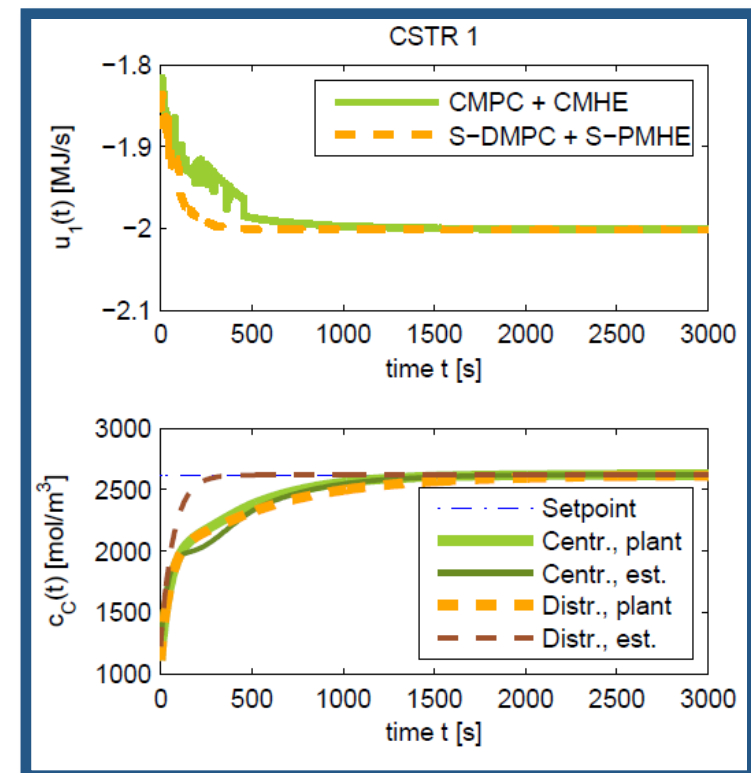
- **DMPC & centralized state estimation** (Zheng et al., 2009, Hu & El-Farra, 2013)
- **DMPC & distributed Luenberger observer** (Venkat et al., 2005, ...)
- **DMPC & distributed Kalman filter** (Venkat 2006 et al., ...)

Novel approach

- **S-DMPC & R-PMHE**
(Schneider, Scheu & M., 2014)
- **Alkylation plant case study:**
130 nonlinear DAEs, 25 states,
5 controls, 6 measurements, linear
S-DMPC & R-PMHE, 1 iteration

Many open issues

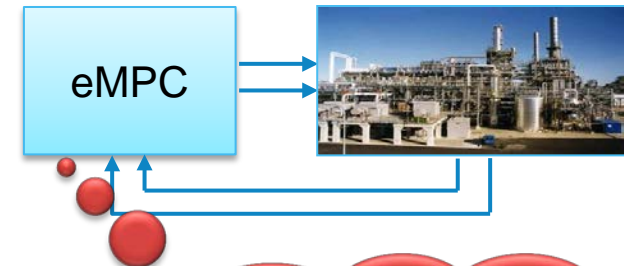
- Formulations, decomposition, and theoretical properties (stability ...)
- Efficient numerical algorithms
- Real-world (nonlinear) applications
- Distributed output feedback eMPC



Economic Model-Predictive Control – Revisited

Continuous-time state feedback on moving horizon

$$\begin{aligned} & \min_{x,u} \Phi(x,u) \quad s.t. \\ & \Phi(x,u) = \|x(t_f)\|_P^2 + \int_{t_0}^{t_f} \|x(t)\|_Q^2 + \|u(t)\|_R^2 dt, \\ & \dot{x}(t) = f[x(t), u(t), d(t)], \quad t \in [t_0, t_f], \\ & x(t_0) = \hat{x}_0, \\ & x(t) \in X, \quad t \in [t_0, t_f], \\ & u(t) \in U, d(t) \in D, \quad t \in [t_0, t_f], \\ & x(t_f) \in X_f \end{aligned}$$



Efficient real-time algorithms, fast updates of pNLP by pQP (Wolf & M., 2016)

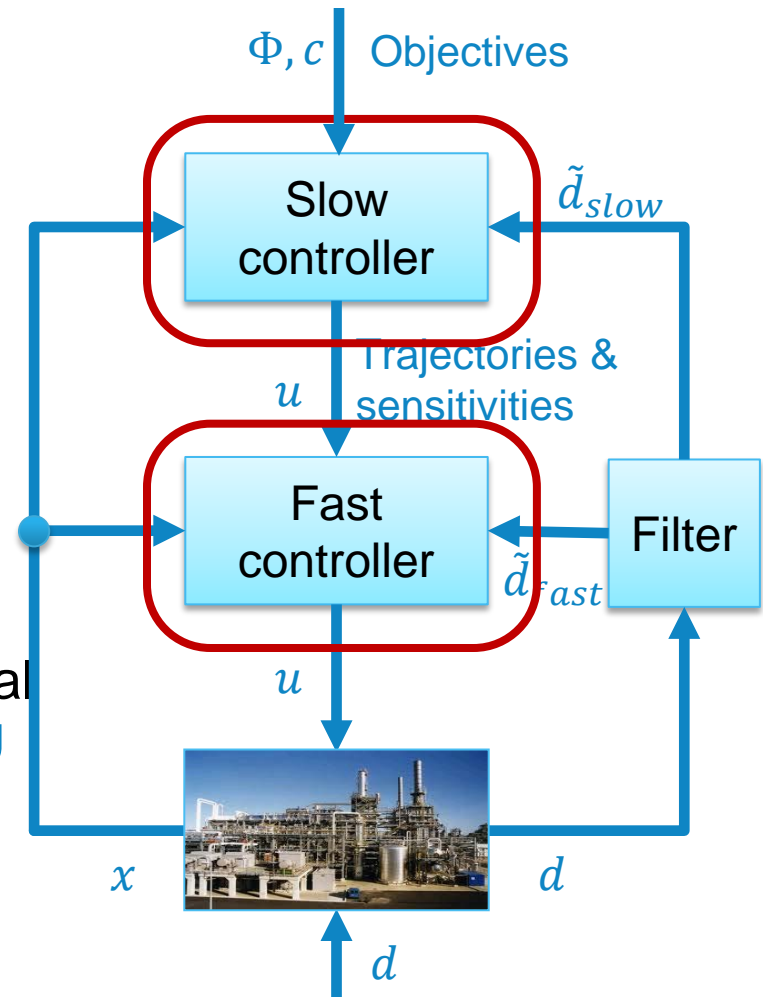
$$\begin{aligned} u_h(t) &= \sum_{\kappa=1}^{K_h} (z_{\kappa})_h \Psi_{\kappa}(t) \longrightarrow z_h = [(z_1)_h^T, \dots]^T \\ d_h(t) &\approx \sum_{\kappa=1}^{K_h} (\bar{d}_{\kappa})_h \Psi_{\kappa}(t) \longrightarrow p_h = [(\bar{d}_1)_h^T, \dots, x_h^{0T}]^T \end{aligned}$$

$$\begin{aligned} & \min_{z_h} \Phi(z_h, p_h) \\ & s.t. \quad c(z_h, p_h) \leq 0 \end{aligned}$$

Parameterization and transcription to pNLP

Hierarchical Two-Layer Architecture for eMPC

- Slow **economic** nonlinear model-predictive control (NMPC) for trajectory generation
 - Low sampling rate
 - Efficient, robust OC algorithm
- Fast **economic** NMPC for tracking control and disturbance rejection
 - High sampling rate
 - Initial value embedding / suboptimal / neighboring extremal update (**NEU algorithm**)



Neighboring Extremal Update (NEU)

- Exploit sensitivity information of previous upper layer NLP solution (*) to generate a fast approximation z_h of the optimal update.

(Kadam & M., 2004, Würth et al., 2009, 2011, Wolf & M., 2016)

- Parametric quadratic programming problem (pQP):

$$\begin{aligned} \min_{\Delta z_h} \quad & J(\Delta z_h) \stackrel{\text{def}}{=} 0.5 \Delta z_h^T L_{zz}^* \Delta z_h + \Delta p_h^T L_{pz}^* \Delta z_h + \Phi_z^* \Delta z_h \\ \text{s.t.} \quad & \mathbf{c}(\Delta z_h) \stackrel{\text{def}}{=} c^* + c_z^* \Delta z_h + c_p^* \Delta p_h \leq 0 \end{aligned}$$

Optimal solution

$$z^*(p^*)$$

$$\begin{aligned} & \Phi_z^*, c_z^*, c_p^* \\ & L_{zz}^*, L_{pz}^* \end{aligned}$$

Feedback

$$\Delta p_h := p_h - p^*$$

NEU

$$\Delta z_h := z_h - z^*$$

Handles changes of active set!

(Ganesh & Biegler, 1987)

L : Lagrange function

c : constraints

p : parameter vector

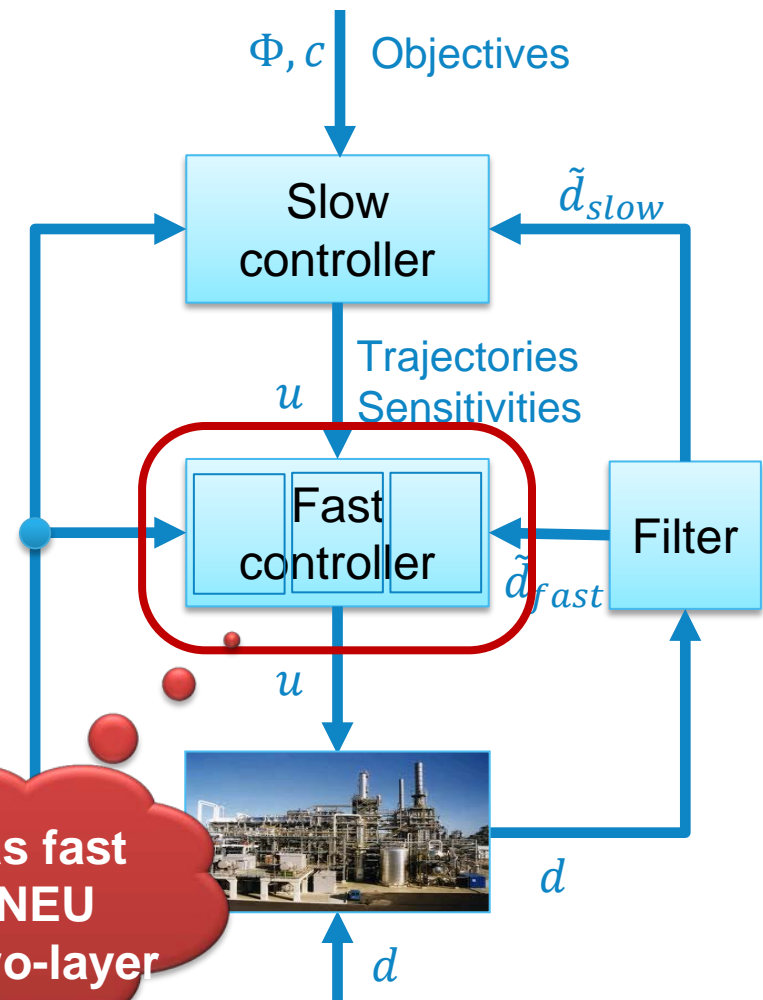
z : control parameter vector

Tracks necessary conditions of optimality rather than outdated reference trajectory and guarantees consistency between layers!

Hierarchical Two-Layer Architecture for eMPC

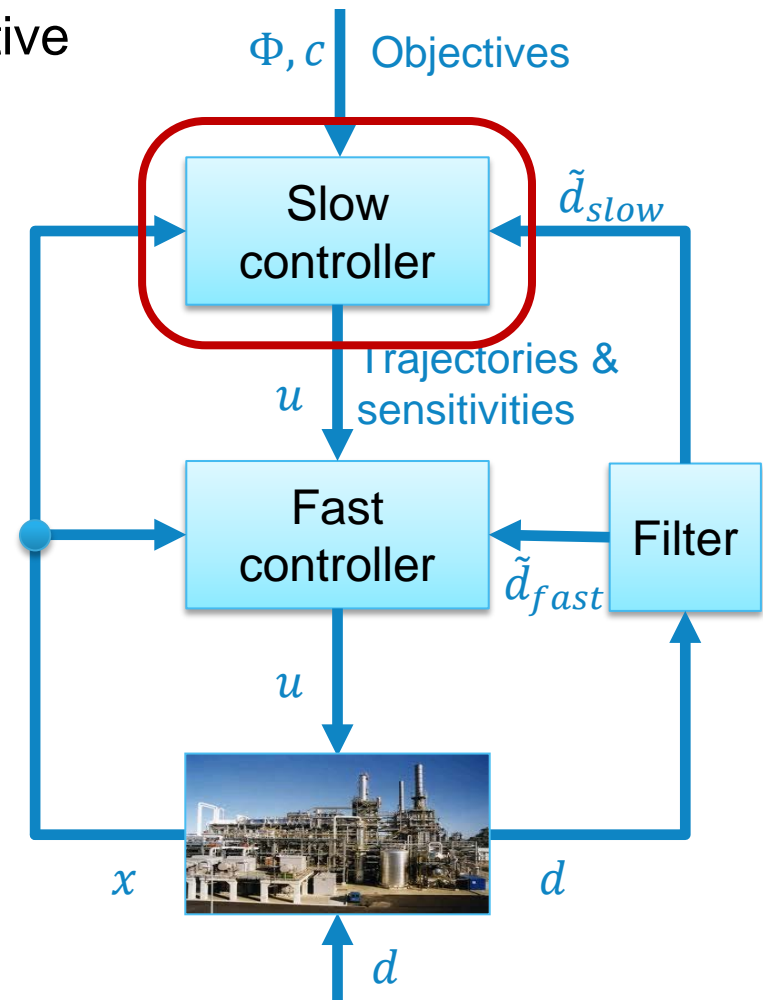
- Slow **economic** nonlinear model-predictive control (NMPC) for trajectory generation
 - Low sample rate
 - Efficient, robust OC algorithm
- Fast **economic** NMPC for tracking control and disturbance rejection
 - High sample rate
 - Initial value embedding / suboptimal / neighboring extremal update (**NEU algorithm**)
- **Distributed** fast MPC for systems
(Wolf et al., 2012)

Use S-DMPC as fast controller in NEU algorithm for two-layer eNMPC



How to Account for Discrete Decisions?

- Slow **economic** nonlinear model-predictive control (NMPC) **for generation of sequence of operational modes and transition optimization**
 - Low sampling rate
 - **Hybrid (switching) controller**
 - Efficient, robust OC algorithm
- Fast **economic** NMPC
 - High sampling rate
 - Initial value embedding / suboptimal / neighboring extremal update (**NEU algorithm**)
- **Distributed** fast MPC for large-scale systems



Scenario-based Decision Making – Situated Action

Adjust operational strategy to context !

Scenario (market, suppliers, demand, state of plant ...)



Strategy 1

Strategy 2

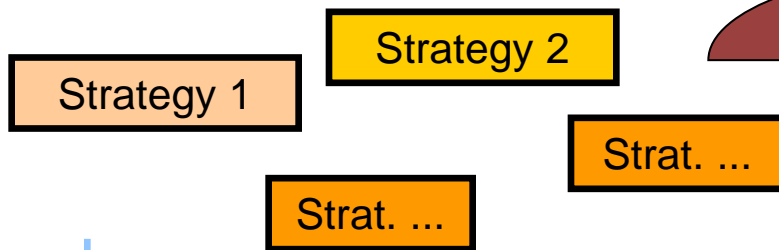
...

Different objectives

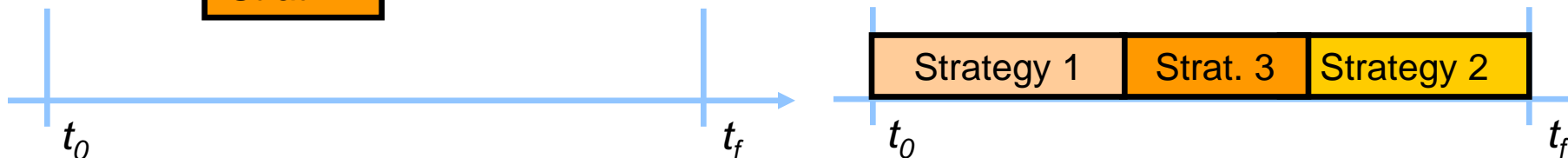
Min cost

Max flexibility

...



Optimal changeover & automatic sequencing



Disjunctive Programming Formulation

- Objective:

$$\min_{z_k, u_k, p, Y} \Phi := \sum_{k=1}^{n_s} \Phi_k(z_k(t_k), p, t_k) + \sum_{i=1}^{n_y} b_i$$

- Dynamic model:

$$s.t. \quad f_k(\dot{z}_k, z_k, u_k, p, t) = 0, t \in [t_{k-1}, t_k], k \in K,$$

- Constraints:

$$g_k(z_k, u_k, p, t) \leq 0, t \in [t_{k-1}, t_k], k \in K,$$

- Initial conditions:

$$l(\dot{z}_0, z_0, p) = 0,$$

- Stage transition conditions:

$$z_{k+1}^d(t_k) - m_k(z_k(t_k), p) = 0, k \in K_m,$$

- Disjunctions:

$$\left[\begin{array}{c} Y_i \\ q_{k,i}(\dot{z}_k, z_k, u_k, p, t) = 0, \\ r_{k,i}(z_k, u_k, p, t) \leq 0, \\ s_i(\dot{z}_0, z_0, p) = 0, \\ z_{k+1}^d(t_k) - v_k^i(z_k(t_k), p) = 0, \\ b_i = \gamma_i, \end{array} \right] \vee \left[\begin{array}{c} \neg Y_i \\ B_{k,i}[u_k^T, p^T, \\ z_k(t_{k-1})]^T = 0, \\ b_i = 0, \end{array} \right]$$

- Propositional logic:

$$\Omega(Y) = True.$$

Take Home Messages

- **The German “Energiewende”**
 - ❖ is an ambitious undertaking which is deemed to succeed;
 - ❖ its success will not only depend on science, though science will be one of the major enablers.
- **Research on new materials, components and devices is going strong (@FZJ on PV, RSOFC, batteries ...)**
- **Systems & control needs much more attention and offers great research opportunities:**
 - ❖ integrated design (e.g., P2X2P, demand-side management),
 - ❖ integration of planning, scheduling & control,
 - ❖ hierarchical and distributed architectures embedding economic model-predictive control and moving horizon estimation,
 - ❖ (big) data analytics & machine learning, and
 - ❖ many more ...



FINDING TOMORROW TODAY

References (1)

- V. Adetola and M. Guay (2010). „Integration of real-time optimization and model predictive control. Journal of Process Control, 20 (2),125 – 133.
- I. Alvarado, D. Limon, D. Munoz de la Pena, J. Maestre, M. Ridao, H. Scheu, W. Marquardt, R. Negenborn, B. De Schutter, F. Valencia, and J. Espinosa (2011). “A comparative analysis of distributed MPC techniques applied to the HD-MPC four-tank benchmark.” Journal of Process Control, vol. 21, no. 5, pp. 800 – 815.
- R. Amrit, J. B. Rawlings and D. Angeli (2011). "Economic optimization using model predictive control with a terminal cost", Annu. Rev. Control, 35(2), 178-186.
- T. Backx, O. Bosgra, and W. Marquardt (2000). “Integration of model predictive control and optimization of processes.” IFAC Symposium Adchem 2000, 249-260.
- J. Busch, M. Santos, J. Oldenburg, A. Cruse and W. Marquardt (2005). „ A framework for the mixed integer dynamic optimisation of waste water treatment plants using scenario-dependent optimal control.” European Symposium on Computer-Aided Process Engineering - 15 Barcelona, Spain.
- J. Busch, J. Oldenburg, M. Santos, A. Cruse and W. Marquardt (2007). “Dynamic predictive scheduling of operational strategies for continuous processes using mixed-logic dynamic optimization.” Comp. Chem. Engg. 31, 574–587.
- M. Diehl, R. Amrit, J.B. Rawlings (2011). „A Lyapunov function for economic optimizing model-predictive control. IEEE Transactions on Automatic Control 56 (3), 703-707
- D. Elixmann, J. Bush, W. Marquardt (2010). “Integration of model-predictive scheduling, dynamic real-time optimization and output tracking for a wastewater treatment process. 11th IFAC Symposium on Computer Applications in Biotechnology, Leuven. IFAC Proceedings Volumes 43 (6), 90-95.
- M. Ellis, H. Durand, P.D. Christofidis (2014). “A tutorial review of economic model predictive control methods.” J. Process Control, 24, 1156-1178.
- S. Engell (2007). „Feedback control for optimal process operation.“ J. Process Control 17, 203-219.
- M. Farina, G. Ferrari-Trecate, and R. Scattolini (2010). “Moving horizon partition-based state estimation of large-scale systems.” Automatica, 46(5):910-918.
- M. Farina and R. Scattolini (2011). “An output feedback distributed predictive control algorithm.” In 50th CDC and ECC 2011, pages 8139-8144.

References (2)

- N. Ganesh, L.T. Biegler (1987). "A reduced hessian strategy for sensitivity analysis of optimal flowsheets." *AIChE J.*, 33, 282–296.
- P. Giselsson (2013). "Output feedback distributed model predictive control with inherent robustness properties." In *ACC*, pages 1694-1699.
- M. T. Gouvea and D. Odloak (1998) "One-layer real time optimization of LPG production in the FCC unit: procedure, advantages and disadvantages." *Comp. Chem. Engng.*, 22(Suppl), S191-S198.
- L. Grüne (2013). „Economic receding horizon control without terminal constraints. *Automatica* 49 (3), 725-734.
- J. W. Grizzle and P.E. Moraal (1990). "On observers for smooth nonlinear digital systems." *American Control Conference*, San Diego, CA.
- M. F. Hassan, G. Salut, G. Singh Madan, and A. Titli(1978). "A decentralized computational algorithm for the global Kalman filter." *IEEE Transactions on Automatic Control*, 23(2):262-268.
- A. Helbig, O. Abel and W. Marquardt (2000). „Structural concepts for optimization based control of transient processes. *In: Nonlinear Model Predictive Control*. F. Allgöwer et a. (Eds.).
- Y. Hu, N.H. El-Farra (2013). "Quasi-decentralized output feedback model predictive control of networked process systems with forecast-triggered communication." *2013 American Control Conference*, 2612-2617
- R. Huang, E. Harinath, L.T. Biegler (2012). „Lyapunov stabilized of economically oriented NMPC for cyclic processes.“ *J. Process Control* 21(4), 501-509.
- R. E: Kalman (1960). "A new approach to linear filtering and prediction problems." *Trans. ASME, Journal of Basic Engineering*, 82 (Series D), 35-45.
- J. Kadam, W. Marquardt, M. Schlegel (2003). "Towards integrated dynamic real-time optimization and control of industrial processes." In: I. E. Grossmann, C. M. McDonald (Eds.): *FOCAPO (Fourth International Conference on Foundations of Computer-Aided Process Operations)*, Coral Springs, Florida, 593-596
- J. V. Kadam and W. Marquardt (2004). "Sensitivity-based solution updates in closed-loop dynamic optimization. *IFAC Symposium DYCOPS-7*.
- L. S. Lasdon (1970). "Optimization Theory for Large Systems." *Macmillan Series for Operations Research*.
- D. G. Luenberger (1964). "Observing the state of a linear system." *IEEE Trans on Mil. Electronics* 8, 290-293.

References (3)

- R. R. Negenborn, B. De Schutter, and J. Hellendoorn (2008). “Multi-agent model predictive control for transportation networks: Serial versus parallel schemes.” *Engineering Applications of Artificial Intelligence* 21(3), 353–366.
- J.M. Maestre, M.A. Ridao, A. Kozma, C. Savorgnan, M. Diehl, M.D. Doan, A. Sadowska, T. Keviczky, B. de Schutter, H. Scheu, W. Marquardt, F. Valencia, J. Espinosa (2015). „A comparison of distributed MPC schemes on a hydro-power plant benchmark.“ *Opt. Control Appl. & Methods* 36(3), 306-332.
- M.D. Mesarovic, D. Macko, Y. Takahara (1970). *Theory of Hierarchical, Multilevel Systems*. Academic Press.
- H. Michalska, D.Q. Mayne, *Moving Horizon Observers*, IFAC Symposium Nonlinear Control Systems Design, Bordeaux, France, 1992.
- J. Oldenburg, W. Marquardt, D. Heinz, D. B. Leineweber (2003). „Mixed logic dynamic optimization applied to batch distillation process design. *AIChE J.*, 49(11), 2900-2917.
- R. Raman and I.E. Grossmann (1994). “Modelling and computational techniques for logic based integer programming.” *Computers and Chemical Engineering*, 18, 563
- S. Roshany-Yamchi, M. Cychowski, R. R. Negenborn, B. De Schutter, K. Delaney, and J. Connell (2013). “Kalman filter-based distributed predictive control of large-scale multi-rate systems: Application to power networks.” *IEEE T. Contr. Syst. T.*, 21(1):27-39.
- R. Scattolini (2009). “Architectures for distributed and hierarchical Model Predictive Control – A review.” *J. Process Control*, 19, 723-731.
- H. Scheu and W. Marquardt (2011). “Sensitivity-based coordination in distributed model predictive control.” *J. Process Control*, 21(5):715-728.
- R. Schneider, H. Scheu, and W. Marquardt (2013). “An iterative partition-based moving horizon estimator for large-scale linear systems.” In 13th ECC, pages 2621 -2626.
- R. Schneider, H. Scheu, and W. Marquardt (2014). “Distributed MPC and partition-based MHE for distributed output feedback.” *IFAC World Congress 2014*, Cape Town, South Africa.
- R. Schneider, R. Hannemann and W. Marquardt (2015). “An iterative partition-based moving horizon estimator with coupled inequality constraints.” *Automatca* 61, 302-307.
- R. Schneider (2016). “On the convergence of sensitivity-driven partition-based moving horizon estimators.”, CDC 2016.

References (4)

- V.S. Vassiliadis, R.W.H. Sargent and C.C. Pantelides (1994). "Solution of a class of multistage dynamic optimization problems. 2. Problems with path constraints." *Ind. Eng. Chem. Res.*, 33, 2123–2133.
- A. N. Venkat, J. B. Rawlings, and S. J. Wright (2005). "Stability and optimality of distributed model predictive control." In 44th CDC and ECC 2005, pages 6680-6685.
- A. N. Venkat, I. A. Hiskens, J. B. Rawlings, and S. J. Wright (2006). „Distributed output feedback MPC for power system control.“ In 45th CDC, pages 4038-4045.
- I. J. Wolf, H. Scheu, and W. Marquardt (2012). "A hierarchical distributed economic NMPC architecture based on neighboring-extremal updates." *Proceedings of the American Control Conference*, Montreal; 4155-4160.
- I.J. Wolf et al. (2014). „Consistent hierarchical economic NMPC for a class of hybrid systems using neighboring-extremal updates.“ *J. Process Control*, 24 (2), 389-398.
- I.J. Wolf and W. Marquardt (2016). "Fast NMPC schemes for regulatory and economic NMPC – A review. *Journal of Process Control* 44, 162-183.
- J.V. Kadam, W. Marquardt (2007). „Integration of economical optimization and control for intentionally transient process operation.“ *Lecture Notes in Control and Information Sciences*, Vol. 438, 419-434.
- L. Würth, R. Hannemann, W. Marquardt (2009). „Neighboring-extremal updates for nonlinear model-predictive control and dynamic real-time optimization.“ *J. Process Control* 19(8), 1277-1288.
- L. Würth, R. Hannemann, and W. Marquardt (2011). "A two-layer architecture for economically optimal process control and operation." *Journal of Process Control*, 21, 311-321.
- Y. Zheng, S. Li, X. Wan (2009). "Distributed model predictive control for plant-wide hot-rolled strip laminar cooling process." *J. Process Control* 19, 1427–1437.