

# Latent Variable Methods in Process Systems Engineering

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#### **OUTLINE**

#### Presentation:

- Will be conceptual in nature
- Will cover many areas of Process Systems Engineering
- Will be illustrated with numerous industrial examples
- But will not cover any topic in much detail

#### Objective:

Provide a feel for Latent Variable (LV) models, why they are used,
 and their great potential in many important problems

## **Process Systems Engineering?**

- Process modeling, simulation, design, optimization, control.
- But it also involves data analysis
  - learning from industrial data
    - An area of PSE that is poorly taught in many engineering programs
- This presentation is focused on this latter topic
  - The nature of industrial data
  - Latent Variable models
  - How to extract information from these messy data bases for:
    - <u>Passive applications</u>: Gaining process understanding, process monitoring, soft sensors
    - Active applications: Optimization, Control, Product development
  - Will illustrate concepts with industrial applications

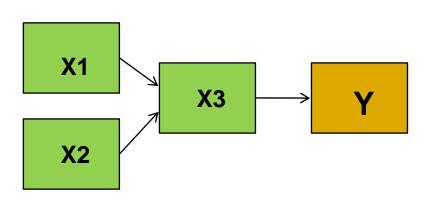


## A. Types of Processes and Data Structures

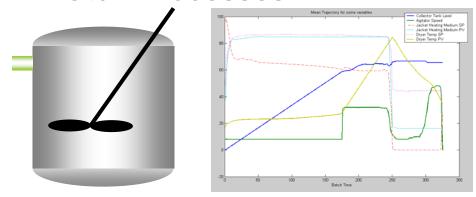
Continuous Processes



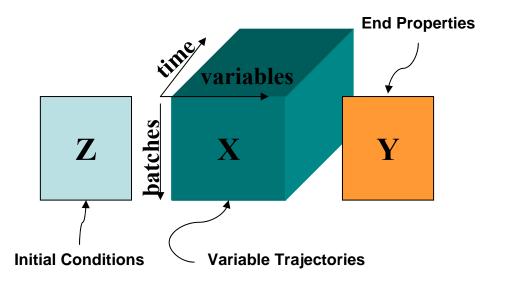
Data structures



Batch Processes



Data structures



## Nature of process data

- High dimensional
  - Many variables measured at many times
- Non-causal in nature
  - No cause and effect information among individual variables
- Non-full rank
  - Process really varies in much lower dimensional space
- Missing data
  - 10 30 % is common (with some columns/rows missing 90%)
- Low signal to noise ratio
  - Little information in any one variable
- Latent variable models are ideal for these problems

## B. Concept of latent variables

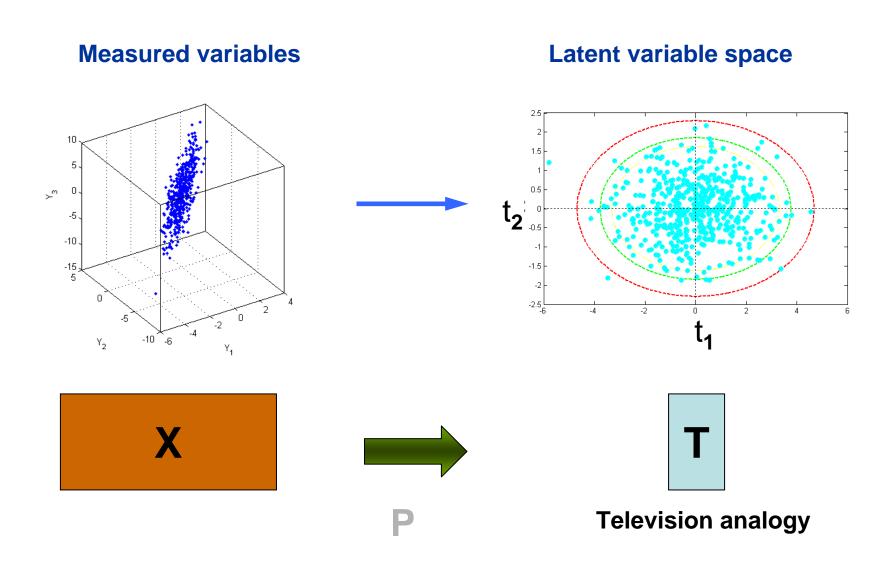
Measurements are available on K physical variables: matrix=X

|   |                        | K columns |          |            |           |         |              |          |           |     |
|---|------------------------|-----------|----------|------------|-----------|---------|--------------|----------|-----------|-----|
| _ | 1                      | 2         | 3        | 4          | 5         | 6       | 7            | 8        | 9         | 1   |
| 1 | Primary ID             | Prim In T | Sec In T | Prim Out T | Feed Flow | Chamb P | Diff P Bag/h | System P | Exhaust P | Sec |
| 2 | 2006-04-05 16:35:00.00 | 119.049   | 116.541  | 41.1646    | 76.5042   | 320.199 | 126.565      | 66.401   | -61.6004  | 41. |
| 3 | 2006-04-05 16:35:05.00 | 119.046   | 116.532  | 41.1979    | 76.4959   | 325.755 | 126.636      | 95.8617  | -43.3963  | 41. |
| 4 | 2006-04-05 16:35:10.00 | 119.044   | 116.523  | 41.1626    | 76.4875   | 321.37  | 126.708      | 82.759   | -52.5372  | 41. |
| 5 | 2006-04-05 16:35:15.00 | 119.041   | 116.514  | 41.1274    | 76.4792   | 327.09  | 126.78       | 80.6494  | -51.5954  | 41. |
| 6 | 2006-04-05 16:35:20.00 | 119.039   | 116.505  | 41.101     | 76.4709   | 326.797 | 126.851      | 94.5307  | -43.7692  | 41. |
| 7 | 2006-04-05 16:35:25.00 | 119.036   | 116.497  | 41.0367    | 76.4625   | 318.052 | 126.923      | 85.1925  | -50.9631  | 41. |
| 8 | 2006-04-05 16:35:30.00 | 119.034   | 116.488  | 41.281     | 76.4542   | 323.099 | 126.995      | 72.5004  | -56.6797  | 41. |

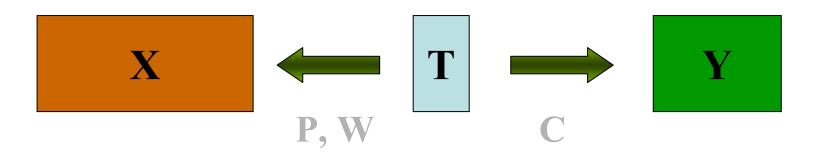
But, the process is actually driven by small set of "A"  $(A \ll K)$  independent latent variables,  $T_{\bullet}$ 

- Raw material variations
- Equipment variations
- Environmental (temp, humidity, etc.) variations

#### Projection of data onto a low dimensional latent variable space (T)



## Latent variable regression models



$$X = TP^T + E$$
  
 $Y = TC^T + F$   
 $T = XW^*$ 

#### Symmetric in X and Y

- Both X and Y are functions of the latent variables, T
- No hypothesized relationship between X and Y
- Choice of X and Y is arbitrary (up to user)
- A model exists for the X space as well as for Y (a key point)

#### **Estimation of LV Model Parameters**

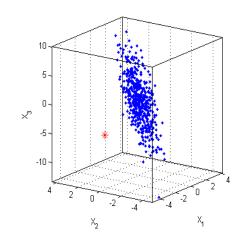
- Parameters: W\*, C, P
- Principal Component Analysis
  - Single matrix X: Maximizes the variance explained
- PLS (Projection to Latent Structures / Partial Least Squares)
  - Maximizes covariance of (X, Y)
- Reduced Rank Regression
  - Maximizes Var(Y) explained by X
- Canonical Variate Analysis (CVA)
  - Maximizes correlation (X, Y)
- Appear to be subtle differences, but method used is often critical to the application

## Subspace Identification Latent variable methods you may be familiar with.

- Subspace identification methods are latent variable methods
  - N4SID Equivalent to Reduced Rank Regression (RRR) (maximizes the variance in Y explained thru correlation with X
  - CVA Canonical Correlation Analysis (maximizes the correlation between X and Y)
  - State variables are the latent variables.

## Important Concepts in Latent Variable Models

- Handle reduced rank nature of the data
  - Work in new low dimensional orthogonal LV space (t1, t2,...)
- Model for X space as well as Y space (PLS)
  - $-X = TP^T + E$ ;  $Y = TC^T + F$ 
    - Unique among regression methods in this respect
  - X space model will be the key to all applications in this talk
    - Essential for uniqueness and for interpretation
    - Essential for checking validity of new data
    - Essential to handle missing data



- Provide causal models in LV space
  - Optimization & control can be done in this space
    - only space where this is justified

#### **Use of LV Models**

- Multivariate latent variable (LV) methods have been widely used in passive chemometric environments
  - A passive environment is one in which the model is only used to interpret data arising from a constant environment
    - Calibration
    - Inferential models (soft sensors)
    - Monitoring of processes
- Used much less frequently in an active environment
  - An active environment is one in which the model will be used to actively adjust the process environment
    - Optimization
    - Control
    - Product Development

## Causality in Latent Variable models

- In the passive application of LV models no causality is required
  - Model use only requires that future data follow the same structure
  - No causality is implied or needed among the variables for use of the model
    - Calibration; soft sensors; process monitoring
- For active use such as in optimization and control one needs causal models
  - For empirical models to be causal in certain x-variables we need to have independent variation (DOE's) in those x's.
  - But much process modeling uses "happenstance data" that arise in the natural operation of the process
    - These models do not yield causal effects of individual x's on the y's
  - But LV models do provide causal models in the low dimensional LV space
    - ie. if we move in LV space (t1, t2, ...) we can predict the causal effects of these moves on X and Y thru the X and Y space models
    - Will use this fact together with the model of the X-space to perform optimization and control in the LV spaces

## C. Industrial applications

- Analysis of historical data
- Process monitoring
- Inferential models / Soft sensors
- Optimization of process operation
- Control
- Scale-up and transfer between plants
- Rapid development of new products

Passive applications

Active applications

## C. Industrial applications

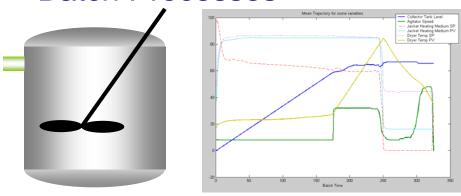
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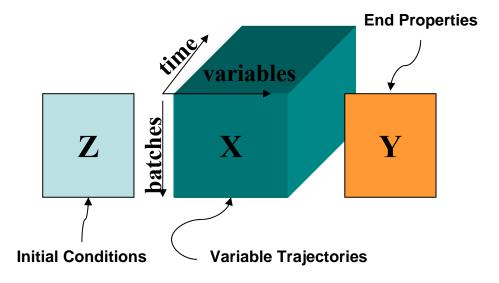
Active applications

## **Analysis of Historical Batch Data**

#### Batch Processes



#### Data structure

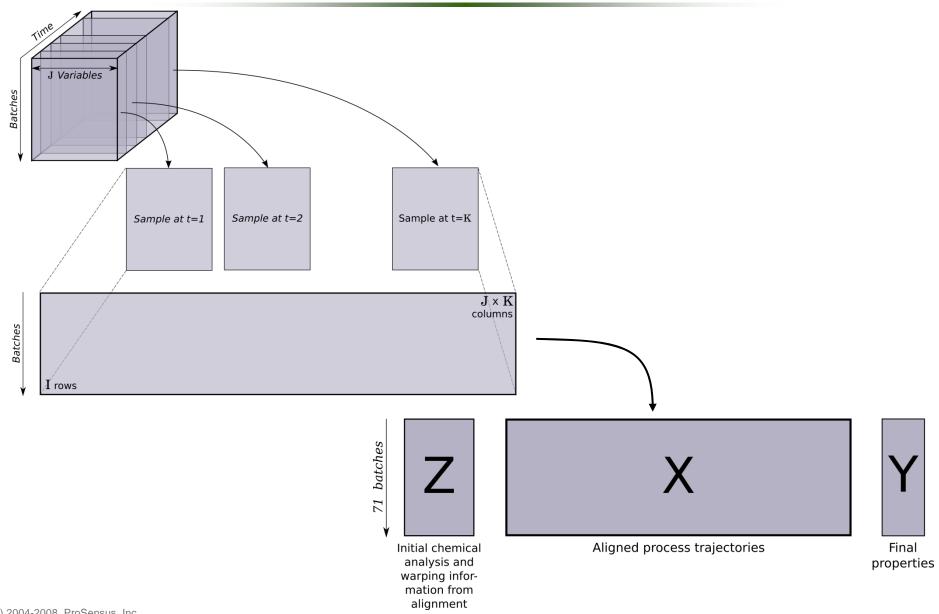


#### **Herbicide Manufacture**

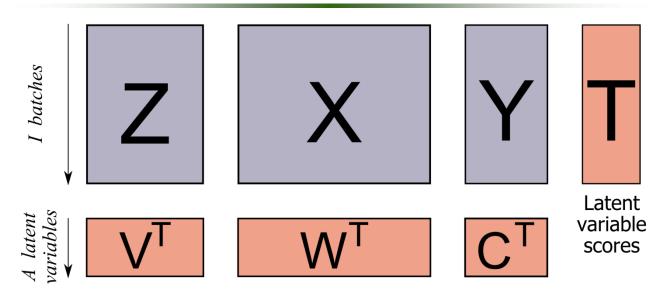
- **Z** Chemistry of materials
  - Discrete process events
- **X** Process variable trajectories
- Y Final quality
  - 71 batches
  - ~ 400,000 data points



## Unfolding and blocking the data



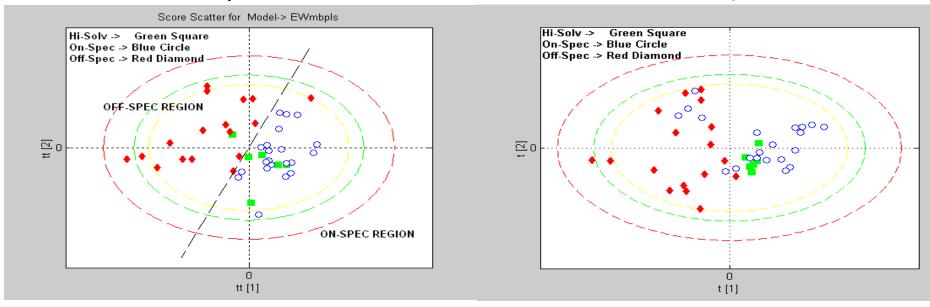
### Multi-way PLS for batch data



- Mean centering removes the average trajectories
- Models the time varying covariance structure among all the process variables over the entire time history of the batch
- Every batch summarized by a few LV scores (t<sub>1</sub>, t<sub>2</sub>, t<sub>3</sub>)
- Relates the IC's (Z) and time varying trajectory information
   (X) to the final product quality (Y)

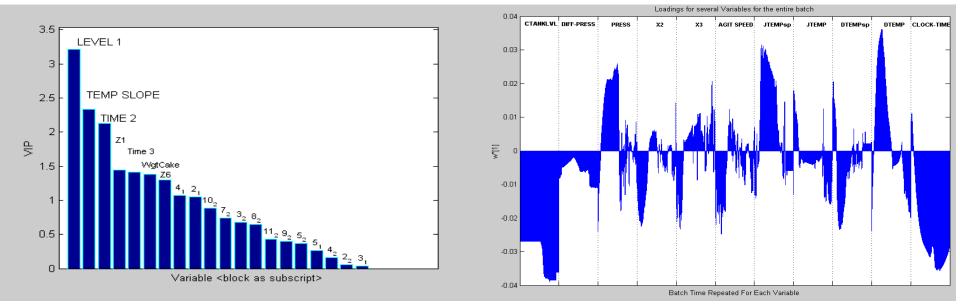
#### LV score plot for Z

#### LV score plot for X



VIP's for Z model

Loading vector  $w_1^*$  for X model



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## **On-line Monitoring of New Batches**

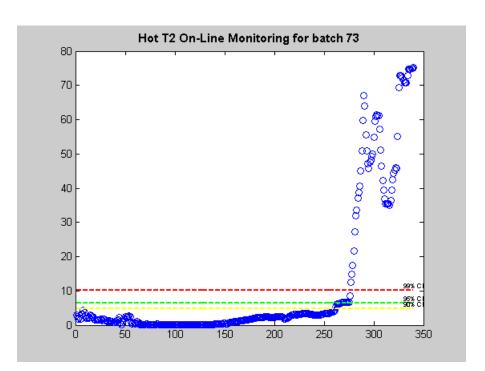
- Multivariate Statistical Process Control
  - Build LV model on all acceptable operational data
  - Statistical tests to see if new batches remain within that model space
    - Hotelling's T<sup>2</sup> shows movement within the LV plane
    - SPE shows movement off the plane



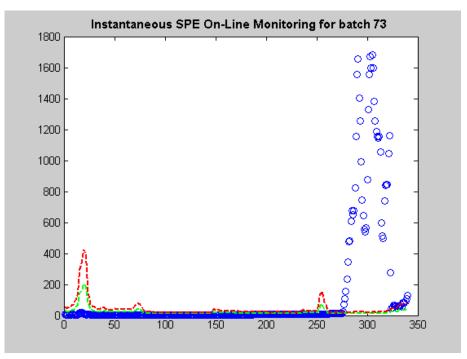
## **Process monitoring: Herbicide process**

## Monitoring of new batch number 73

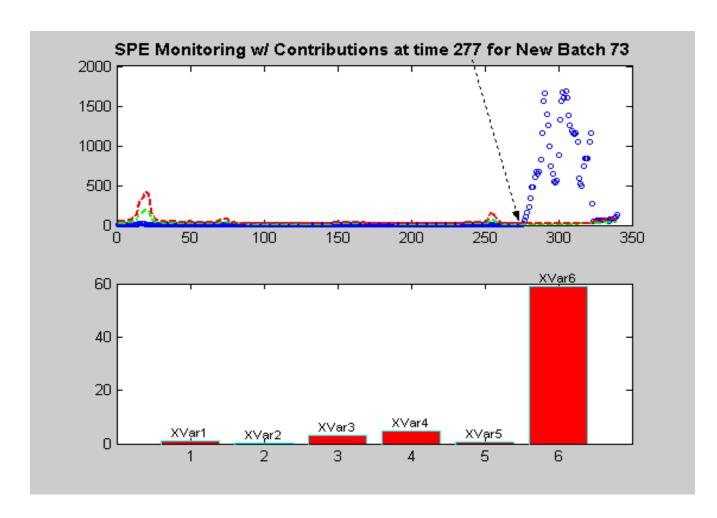
T<sup>2</sup> plot



SPE plot



## Contribution plots to diagnose the problem



Problem: Variable x<sub>6</sub> diverged above its nominal trajectory at time 277

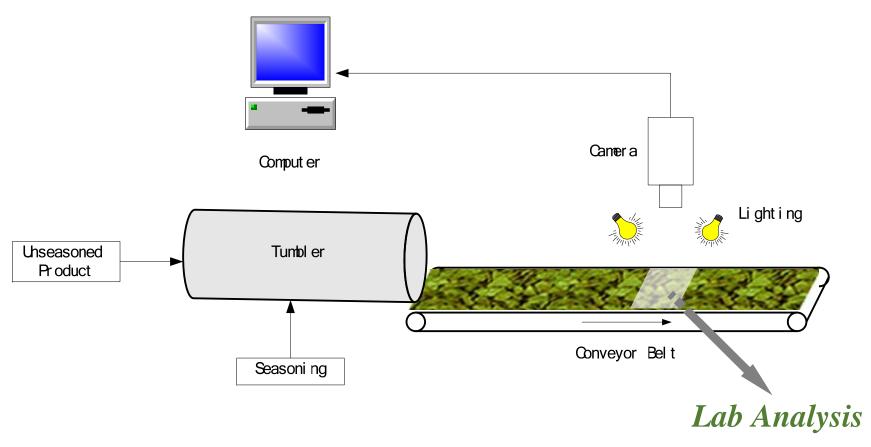
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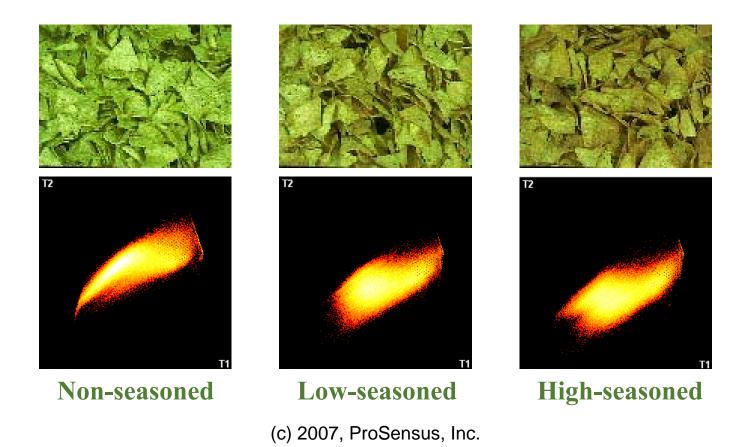
Active applications

## Image-based Soft Sensor for Monitoring and Feedback Control of Snack Food Quality



(c) 2007, ProSensus, Inc.

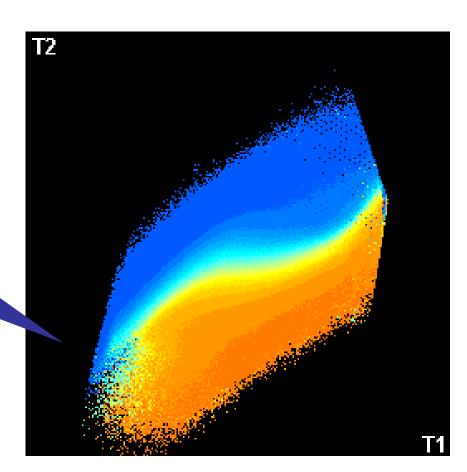
## **PCA Score Plot Histograms**





## Segment Score Space into Multi-mask Region Based on Covariance with Quality

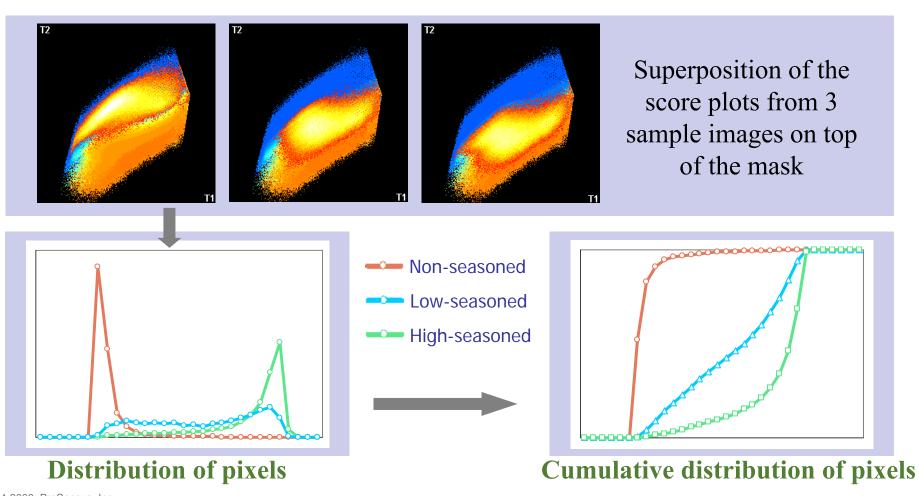
Score space divided up into 32 regions corresponding to various coating levels



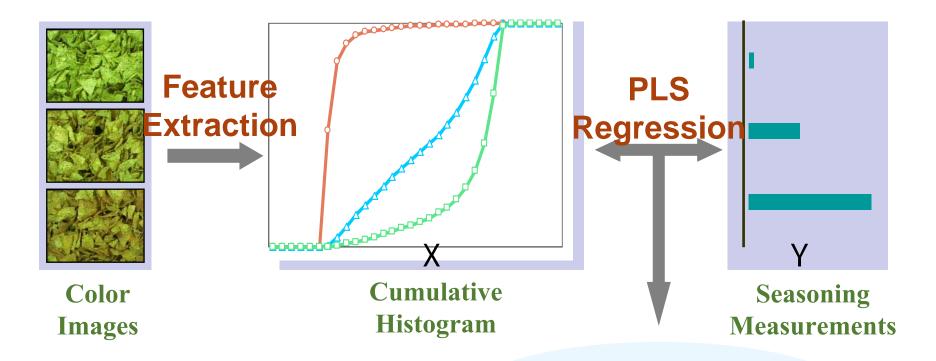
(c) 2007, ProSensus, Inc.



### **Distribution of Pixels**

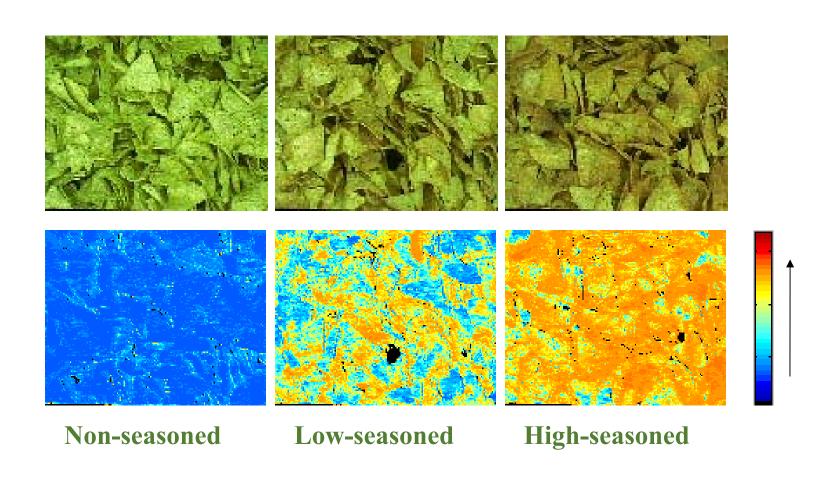


## **Model to Predict Seasoning Concentration**



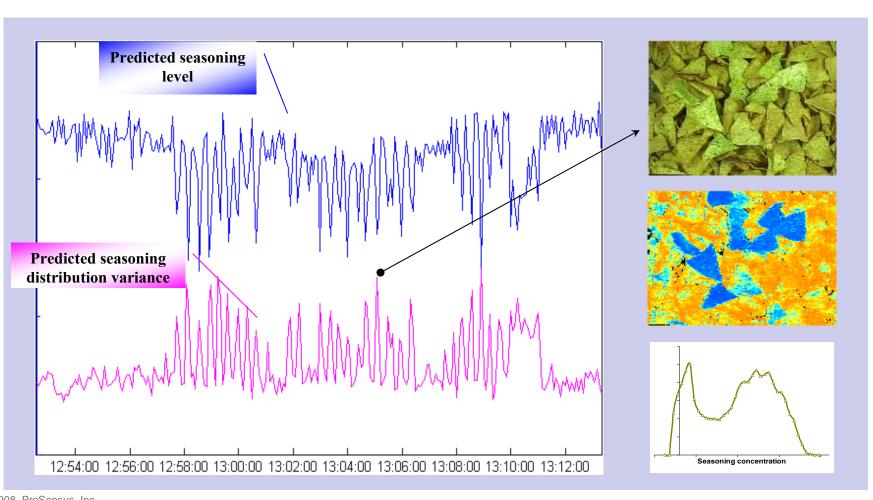
Model for Seasoning Level

## Visualize Images: Pixel by pixel Prediction of Seasoning Concentration

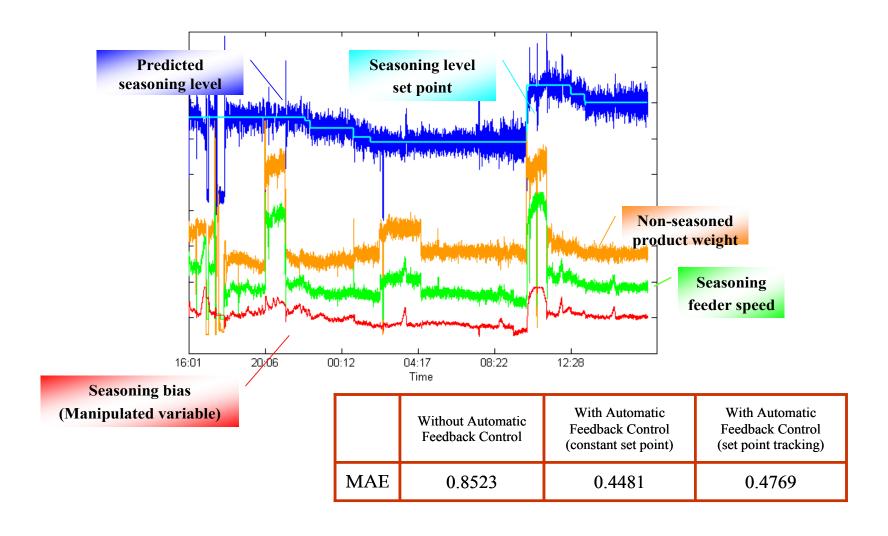




## **Online Results: Mixed Product Experiment**



## **Closed-loop Control of Seasoning Level**



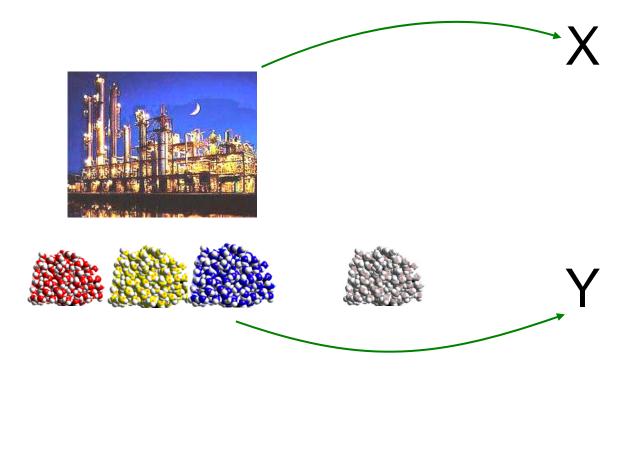
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Passive applications

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## Optimizing operating policies for new products



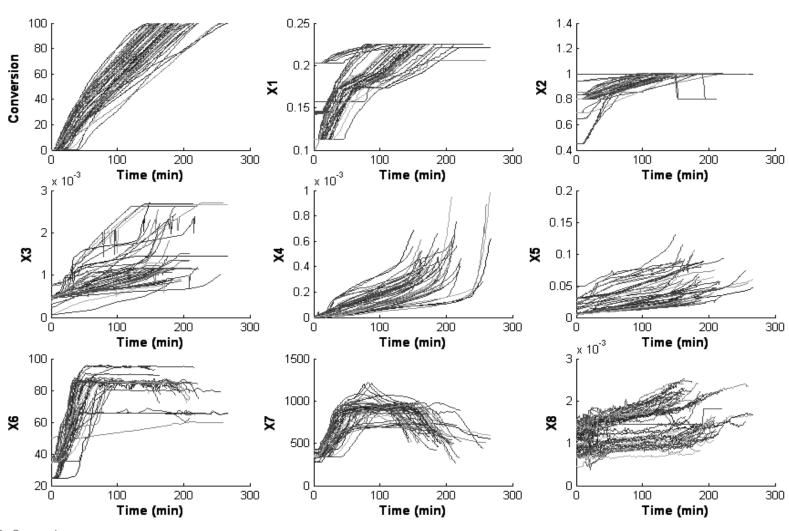
Temperatures
Pressures
Concentrations
Recipes
Flows
Trajectories

Density
Tensile strength
Mw, Mn
Transparency
Biological activity
Toxicity
Hydrophobicity



### **Batch polymerization: Process trajectory data (X)**

#### Batch polymerization – Air Products & Chemicals



## **Batch polymerization data**

#### 13 variables in Y

Desire a new product with the following final quality attributes (Y's):

 $Y_{13} < Y_{13 \text{const}}$ 

Maintain in normal ranges:  $Y_1$   $Y_2$   $Y_3$   $Y_4$   $Y_5$   $Y_6$   $Y_8$ 

Constraints:  $Y_7 = Y_{7des}$   $Y_9 = Y_{9des}$   $Y_{10} < Y_{10const}$   $Y_{11} < Y_{11const}$   $Y_{12} < Y_{12const}$ 

... and with the minimal possible batch time (\*)

#### Solution

- Build batch PLS latent variable model on existing data
- Perform an optimization in LV space to find optimal LV's
- Use LV model of X-space to find the corresponding recipes and process trajectories

### **Unconstrained Solution**

Design via PLS model inversion (no constraints)

PLS Model:  $\hat{\mathbf{Y}} = \mathbf{T}\mathbf{Q}^{\mathsf{T}}$   $\hat{\mathbf{y}}_{\text{des}}^{\mathsf{T}} = \mathbf{Q}\tau_{\text{new}} \qquad \text{Step 1}$   $\hat{\mathbf{X}} = \mathbf{T}\mathbf{P}^{\mathsf{T}} \qquad \tau_{new} = inv\left(Q^{\mathsf{T}}Q\right)Q^{\mathsf{T}}y_{des}$   $\hat{\mathbf{x}}_{\text{new}}^{\mathsf{T}} = \mathbf{P}\tau_{\text{new}} \qquad \text{Step 2}$ 

- If dim(Y) < dim(X) then there is a null space</li>
  - A whole line or plane of equivalent solutions yielding the same y<sub>des</sub>

# Solution with constraints: Formulate inversion as an optimization

• Step 1: Solve for  $\hat{ au}_{new}$  with constraints on T<sup>2</sup> and on y's

$$\min_{\hat{\boldsymbol{\tau}}_{xnew}} \left\{ (\mathbf{y}_{des} - \mathbf{Q} \ \hat{\boldsymbol{\tau}}_{xnew})^{T} \mathbf{G}_{1} (\mathbf{y}_{des} - \mathbf{Q} \ \hat{\boldsymbol{\tau}}_{xnew}) + \rho \left( \sum_{a=1}^{A} \frac{\hat{\boldsymbol{\tau}}_{xnew,a}^{2}}{s_{a}^{2}} \right) \right\}$$

$$s.t$$

$$\mathbf{B} \mathbf{Q} \ \hat{\boldsymbol{\tau}}_{xnew} < \mathbf{b}$$

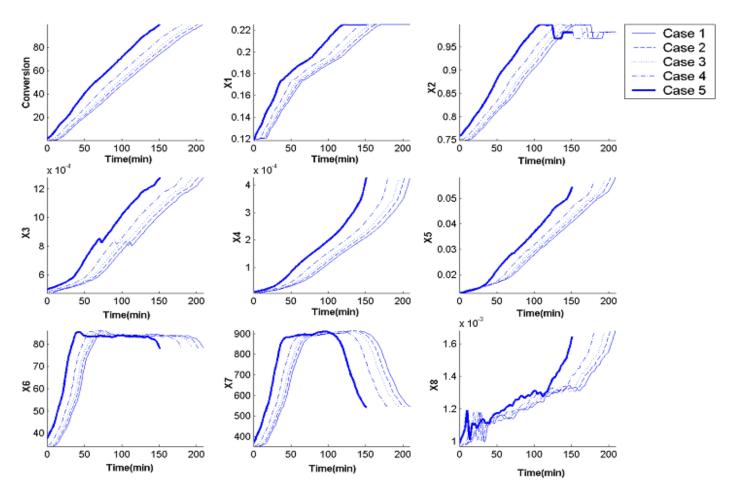
• Step 2: Solve for  $x_{new}$  that yields  $\hat{\tau}_{new}$  subject to certain constraints on SPE and x's.

$$\min_{\mathbf{X}_{\text{new}}} \left\{ \left( \mathbf{W}^* \mathbf{x}_{\text{new}} - \boldsymbol{\tau}_{\text{new}} \right)^{\text{T}} \mathbf{G}_2 \left( \mathbf{W}^* \mathbf{x}_{\text{new}} - \boldsymbol{\tau}_{\text{new}} \right) + \left( \mathbf{x}_{\text{new}} - P \mathbf{W}^* \mathbf{x}_{\text{new}} \right)^{\text{T}} \boldsymbol{\Lambda} \left( \mathbf{x}_{\text{new}} - P \mathbf{W}^* \mathbf{x}_{\text{new}} \right) + \boldsymbol{\eta} \mathbf{x}_{\text{new}} \right\}$$

### Different solutions: change the penalty ( $\eta$ ) on time usage

All solutions satisfy the requirements on y<sub>des</sub>

Case 1 to 5: weight on time-usage is gradually increased



Garcia-Munoz, S., J.F. MacGregor, D. Neogi, B.E. Latshaw and S. Mehta, "Optimization of batch operating policies. Part II: Incorporating process constraints and industrial applications", Ind. & Eng. Chem. Res., 2008

# C. Industrial applications

- Analysis of historical data
- Process monitoring
- Inferential models / Soft sensors
- Optimization of process operation
- Control
- Scale-up and transfer between plants
- Rapid development of new products

Passive applications

Active applications

# Control of batch product quality

- Objective is to control final product quality
  - e.g. control of final particle size distribution (PSD)
- Using all data up to some decision time, predict final quality with latent variable model
  - All prediction done in low dimensional latent variable space (y's then calculated from t's)
- If predicted quality is outside a desired window, then make a mid-course correction to the batch
  - Analogy to NASA mid-course rocket trajectory adjustment in moon missions
- Data requirement: Historical batches + few with DOE on corrective variables

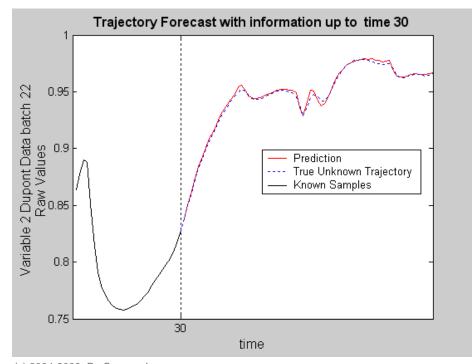


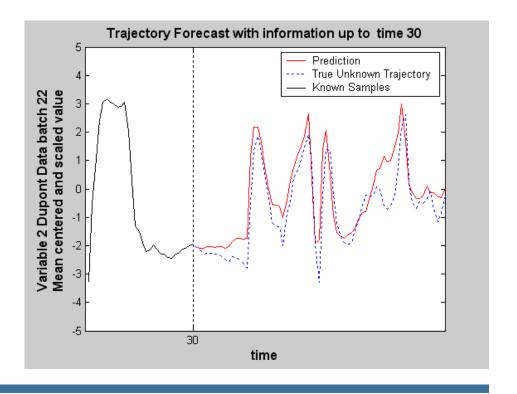
### LV models provide accurate adaptive trajectory predictions

- Use various missing data imputation methods
  - Equivalent of Kalman Filter

Prediction of a variable trajectory using information up to time 30 (DuPont)

Deviations from the mean trajectory – Prediction vs actual

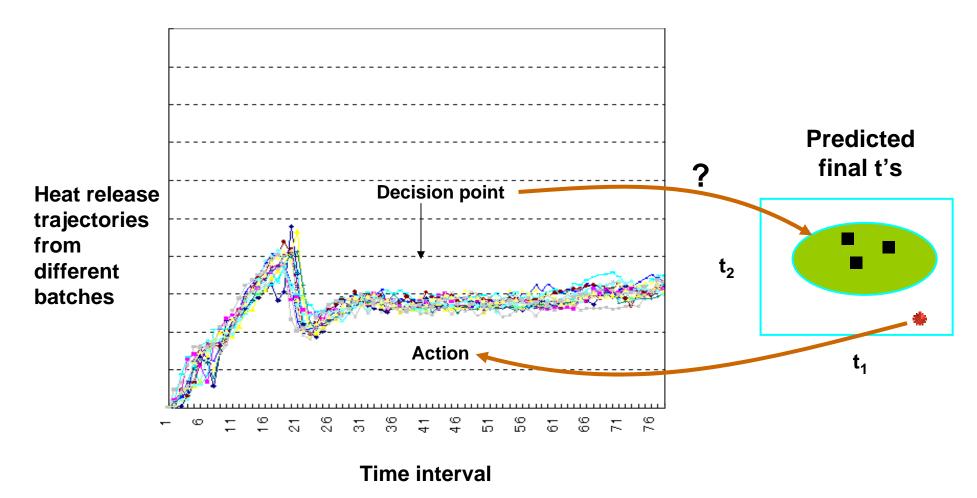




(c) 2004-2008, ProSensus, Inc.

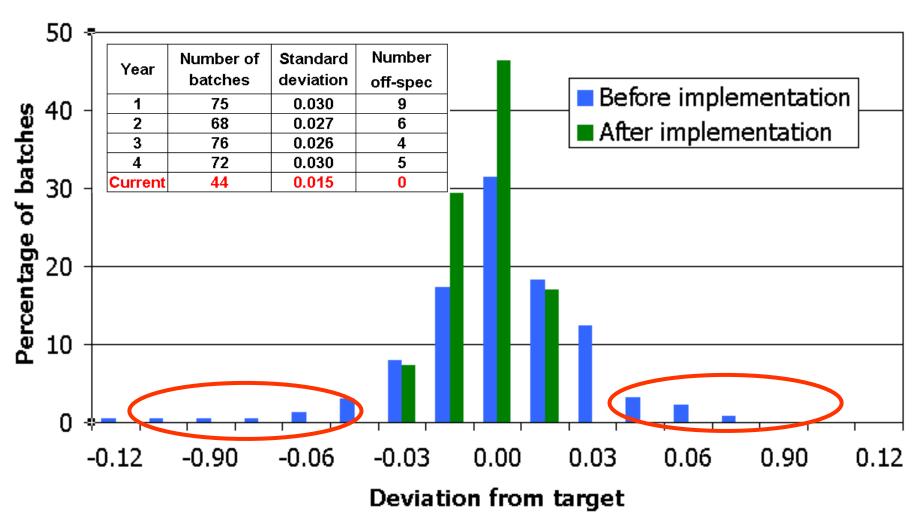
### Control of PSD via mid-course correction

 At decision point – predict t's (Y's) – if outside target region – take action



# Industrial results (Mitsubishi Chemicals)

Mid-course control: before and after implementation



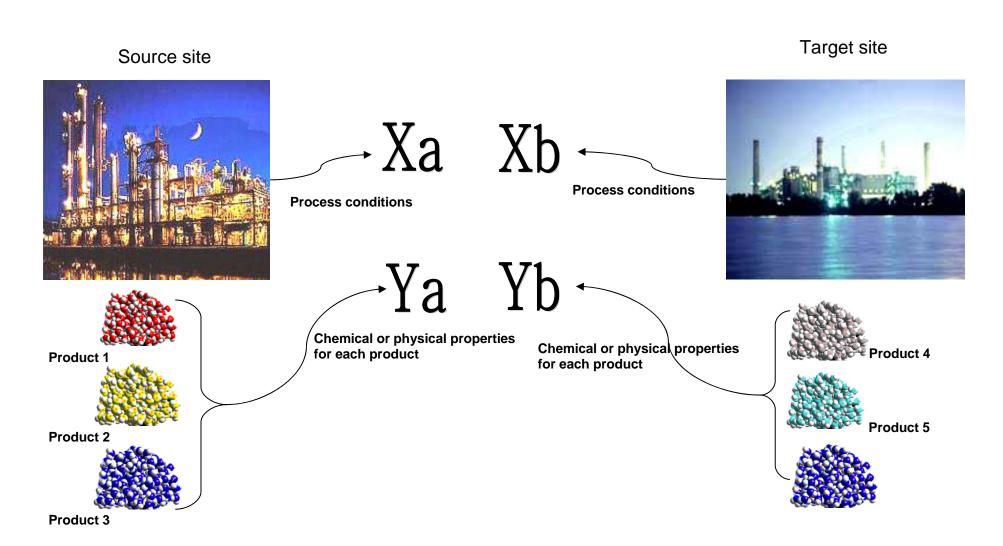
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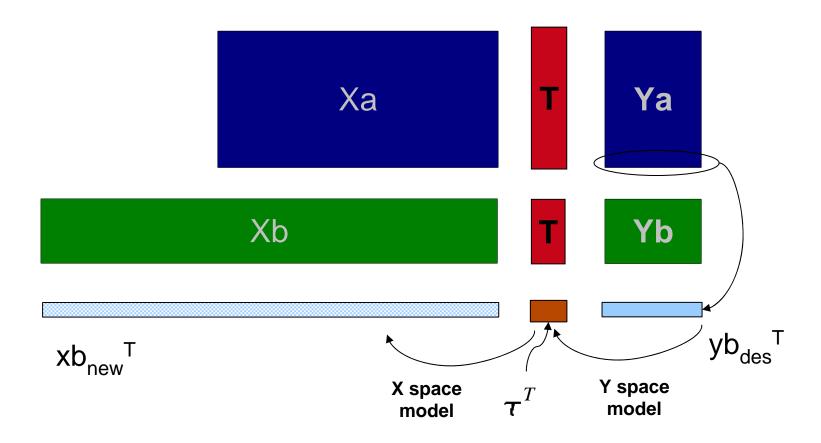
Active applications

# Product transfer between plants and scale-up



# Product transfer and scale-up

### Historical data from the 2 plants. Build JYPLS model



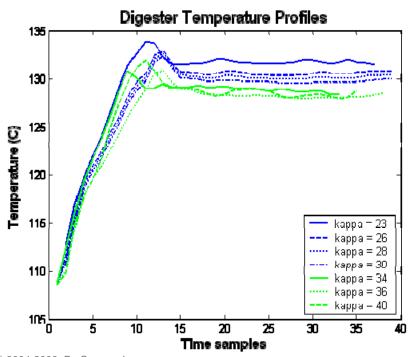
Garcia-Munoz, S., T.Kourti and J.F. MacGregor, "Product Transfer Between Sites using Joint-Y PLS", Chemometrics & Intell. Lab. Systems, 79, 101-114, 2005.

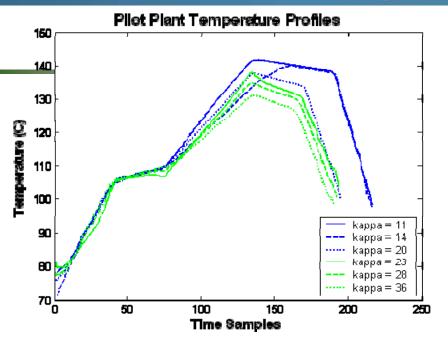


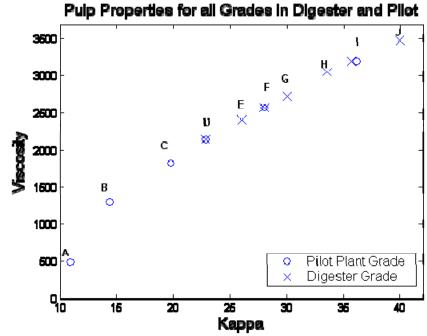
### **Industrial Scale-up Example**

Tembec - Cdn. pulp & paper company:

Pilot plant and full scale digesters





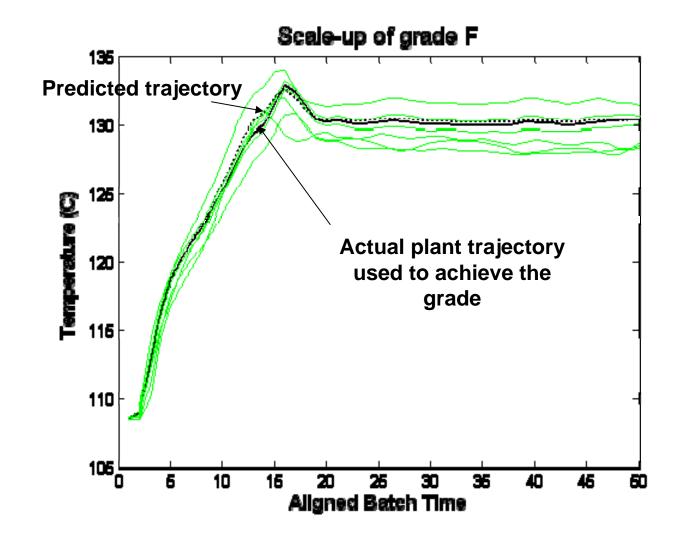


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# Scale up for grade F – pulp digester

Build models on all pilot plant data and all plant data (ex F)

Design operating profiles to achieve grade F in plant.



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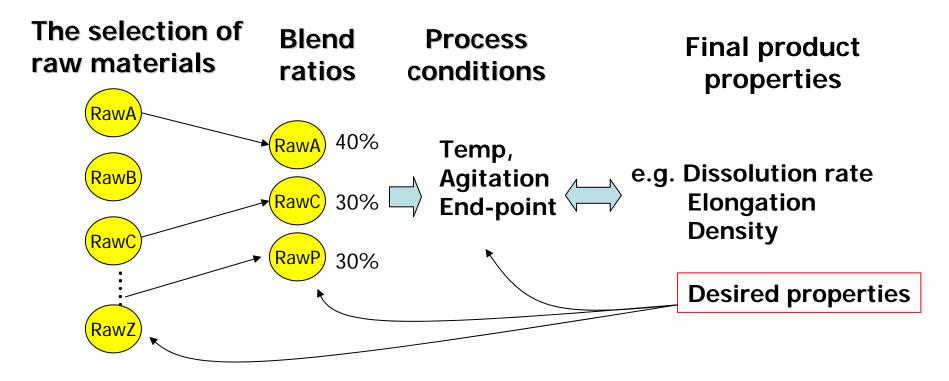
Passive applications

Active applications

# **Data Mining for Product Engineering**

- Companies accumulate lot of data on their products and processes
- Can we use it to rapidly develop new products?
- Three general degrees of freedom for developing new products:
  - Raw material selection
  - Ratios in which to use raw materials (formulation)
  - Process conditions for manufacturing
    - Relative importance of these three depends on the industry and the product
    - Huge synergisms among these

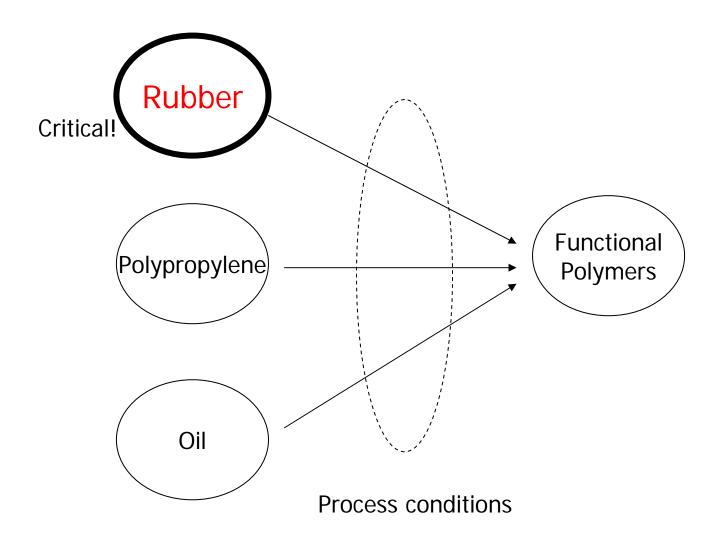
# What is the problem?



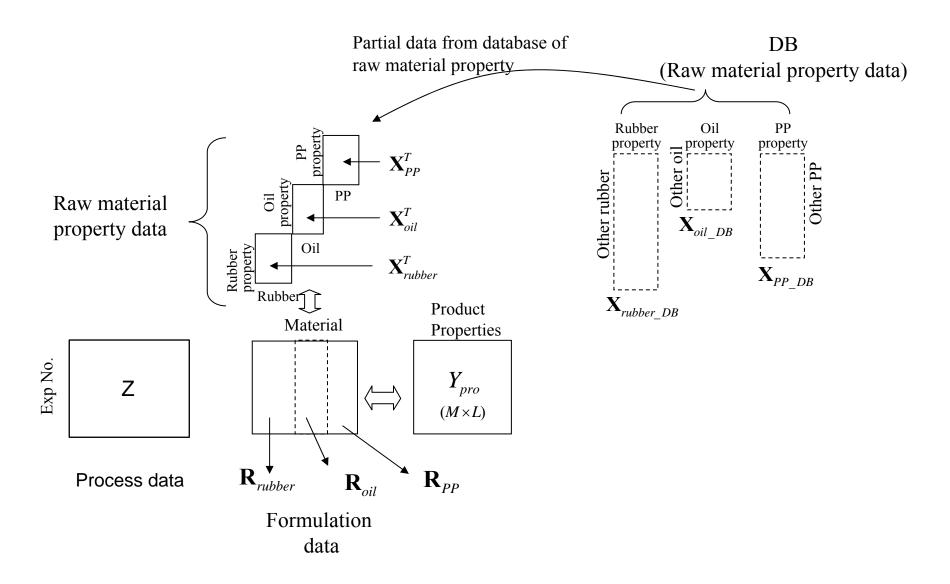
Traditional approaches tend to treat each step separately→ inefficient as they miss synergism among these degrees of freedom

# **Example: Functional Polymer Development**

### Mitsubishi Chemicals



### Data structure





# Methodology

Build a multi-block PLS model that relates all the databases together and predicts the final quality attributes

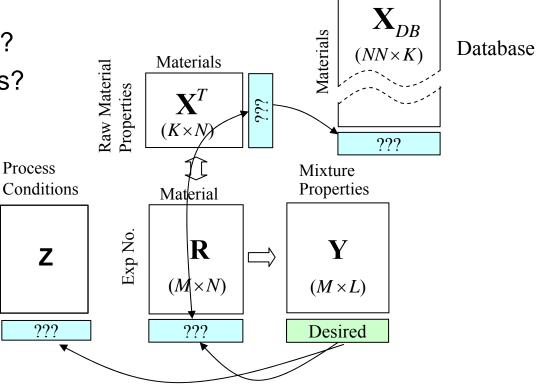
Perform an optimization in the latent variable space of the

Raw material multi-block PLS model properties – Which materials?

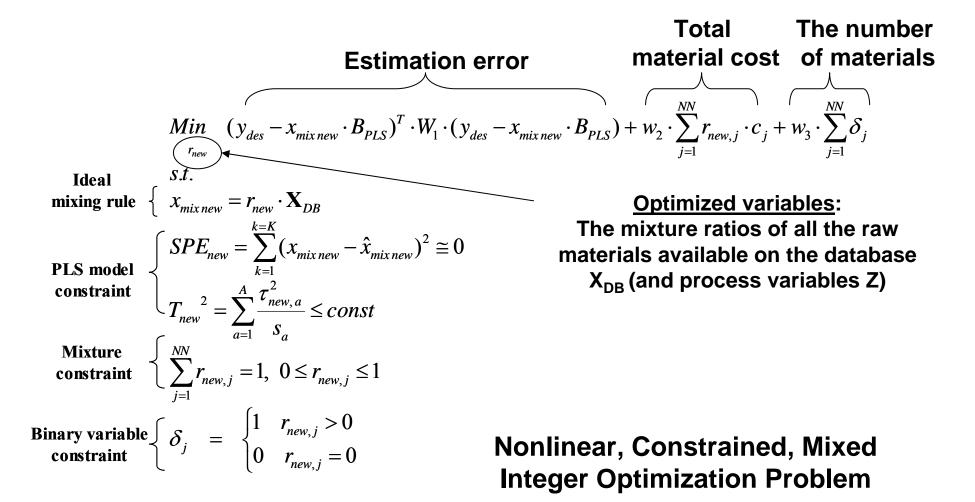
– Formulation ratios?

– Process conditions?

Minimum cost



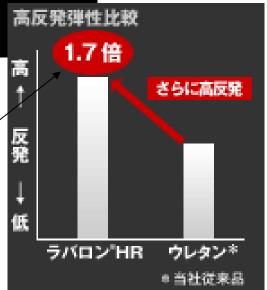
# Formulation of the Optimization



# One Example: Golf ball development



Approach to golf ball core design increased the resilience 1.7 times compared to previous products

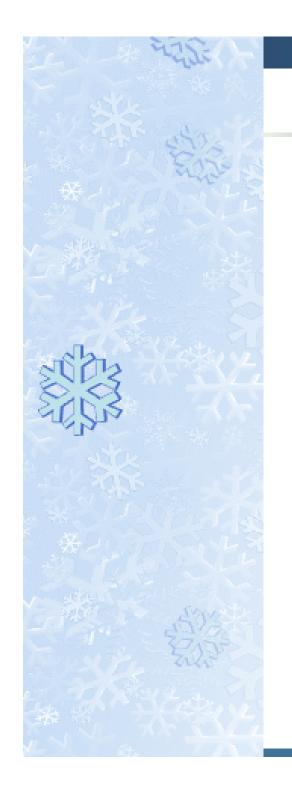


# **Summary**

- Latent variable models:
  - Important concepts:
    - Low dimensional Latent Variable spaces
    - Models for both X and Y
    - Causality only in LV space
- Passive applications
  - Analysis, soft sensors, monitoring
- Active applications
  - Optimization, control, product development
- All work done in LV space (t1,t2, ..)
- Models for X and Y used to get back to these variables.

### **Conclusions**

- If you use historical process data, then Latent Variable approaches are essential
  - Allow one to uniquely interpret and use the data in both passive and active applications





# Some References on topics in the presentation

### Latent variable methods (general)

- Eriksson L., Johansson, E., Kettaneh-Wold, N. and Wold, S., 1999. "Introduction to Multi- and Megavariate Data Analysis using Projection Methods (PCA & PLS), Umetrics AB, Umea, Sweden
- Kourti, T. (2002). Process Analysis and Abnormal Situation Detection: From Theory to Practice. <u>IEEE Control Systems</u>, 22(5), 10-25.

#### Software

SIMCA\_P (Umetrics); Unscrambler (Camo); Matlab toolbox (Eigenvector Technologies), ProMV (ProSensus)

#### Analysis of historical data

 Garcia-Munoz, S., T. Kourti and J.F. MacGregor, A.G.. Mateos and G. Murphy, "Trouble-shooting of an industrial batch process using multivariate methods", <u>Ind. & Eng. Chem. Res.</u>, <u>42</u>, 3592-3601, 2003

#### Monitoring

T. Kourti and J.F. MacGregor, 1995. "Process Analysis, Monitoring and Diagnosis Using Multivariate Projection Methods", <u>J.</u>
 Chemometrics and Intell. Lab. Systems, 28, 3-21.

#### Control

 Flores-Cerillo, J. and J. F. MacGregor, "Within-batch and batch-to-batch inferential adaptive control of semi-batch reactors: A Partial Least Squares approach", <u>Ind. & Eng. Chem. Res.</u>, <u>42</u>, 3334-3345, 2003.

#### Image-based soft sensors

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#### Optimization

- Jaeckle, J.M., and MacGregor, J.F. (1998). Product Design Through Multivariate Statistical Analysis of Process Data. AIChE Journal, 44, 1105-1118.
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   Chemometrics & Intell. Lab. Syst., 70, 63-74, 2004.
- Garcia-Munoz, S., J.F. MacGregor, D. Neogi, B.E. Latshaw and S. Mehta, "Optimization of batch operating policies. Part II: Incorporating process constraints and industrial applications", <u>Ind. & Eng. Chem. Res.</u>, Published on-line, May, 2008

### Product development

- Muteki, K., J.F. MacGregor and T. Ueda, "On the Rapid development of New Polymer Blends: The optimal selection of materials and blend ratios", Ind. & Eng. Chem. Res., 45, 4653-4660, 2006.
- Muteki, K. and J.F. MacGregor, "Multi-block PLS Modeling for L-shaped Data Structures, with Applications to Mixture Modeling", Chemometrics & Intell. Lab. Systems, 85, 186-194, 2006

#### Design of Experiments

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- Muteki, K. and J.F. MacGregor, "Sequential design of mixture experiments for the development of new products", Chemometrics & Intell. Lab Sys., 2007.